

April 8, 2015

NEOMED RESEARCH AND GRADUATE EDUCATION + COMPARATIVE MEDICAL UNIT FINAL REPORT

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NEOMED Research and Graduate Education Building + Comparable Medical Unit Expansion

General Info

Location: The Northeast Ohio Medical University Campus
 4209 Ohio 44, Rootstown Ohio
Function: Research/Education
Size: 83,000 GSF
Height: Four Stories above Grade
Cost: \$38.8 Million
Delivery: Design-Bid-Build with Multiple Prime Contract
Construction Timeline: May 2011-August 2013



Project Team

Architecture: Ellenzweig, TC Architects
Interior Design: TC Architects, Schumacher Design
Testing: PSI, Inc.
MEP: BR+A, Scheeser Buckley Mayfield
Civil/Structural: The GPD Group
CM: The Ruhlin Company
Owner: Northeast Ohio Medical University

Architecture

Façade: Modular face brick with aluminum paneling and glass
Roof: 12"x12" concrete pavers
Interiors: Gypsum wall board on steel studs, grouted cmu's, interior glazing
Zoning: RGE- offices and conference rooms at east end, labs and support rooms west. Top floor shelled out. CMU- specimen holding areas, cage washes, future expansion Building D- several existing labs and offices renovated



Structural

Foundation: Concrete Footings
Superstructure: Steel Framing
Floors: Steel Deck with concrete

Electrical

Site Service: Existing high-voltage campus system stepped down via pad-mounted 1500 kVA transformer
Main Distribution: 480V via 3000A single-end switchboard, with stepdown transformers to convert to 208/120V. Outdoor diesel emergency/standby generator rated at 500 kVA, 480/277V

Mechanical

Heating: 4 3MMBTU boilers in RGE Basement
Cooling: 2 300 ton electric centrifugal chillers in RGE basement, 2 induced draft cooling towers
Ventilation: 2 custom-built AHU's for lab spaces at 37,500 CFM each, 100% OA; smaller office AHU sized at 25,000 CFM and 30% OA. CMU has one 85,000 CFM custom AHU with 100% OA.
Energy Recovery: Heat pipes with sealed refrigerant run from exhaust to supply ducts.
Controls: Independent DDC system interfaced with existing campus front ends

Sam Bridwell

Option-Mechanical

Advisor-Dr. Freihaut

<https://www.engr.psu.edu/ae/thesis/portfolios/2015/stb5114/index.html>

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Executive Summary

This report is the culmination of a comprehensive analysis of the Research and Graduate Education building and Comparative Medical Unit expansion project. The goal of this analysis was to evaluate the merits and goals of the existing project and its systems, and then execute a proposal of alternatives intended to provide tangible benefits to the operators and occupants.

As a high-technology, medical research project the RGE and CMU proved to be a very interesting and technically challenging project to analyze. A high degree of system complexity resulted from the wide range of services needed and strict environmental requirements. The existing system showed itself to be well-designed with regard to programming requirements and in many ways the most appropriate solutions to the design challenges at hand. The goal of the project was very clear: provide the highest quality research and education facility possible to foster the growth and development of health care education within the university and the surrounding community.

Keeping in mind the project goals of quality, availability, independence, and flexibility, a modification to the existing building utilities was proposed in the form of a cogeneration plant to go alongside the existing plant in the RGE basement. Adding on-site generation capability would make the project completely independent of outside utility structures, and the myriad of thermal loads for both space conditioning and lab processes were potential uses for excess generation heat. A configuration was chosen that provided the ability to handle the full campus electrical load, with reasonable turndown for part load operation due to its modular nature. Excess heat was taken advantage of to cover both the low-pressure and high-pressure steam loads present throughout the year. Due to the low cost of electricity at the project location, electric on-site generation did not prove as big of a savings generator as is usually expected from cogeneration projects. However, the cogeneration plant still had a reasonable payback of roughly a decade due to very low gas prices and high equipment efficiencies. A number of the non-quantifiable benefits of cogeneration are directly applicable to this facility, including power reliability, conduciveness to facility expansion, and off-hour operation. In addition, the plant will decrease the campus energy use and environmental impact.

In conjunction with the proposed cogeneration or CHP plant, an interconnection scheme was devised so that the plant could operate in parallel with the electric grid safely and effectively. The ability to start up from a dead state without outside assistance, known as black start capability, was also designed into the cogeneration plant.

Another auxiliary component of the proposal was the implementation of a Design-Build project delivery method in place of the then-mandatory Multiple-Prime contract structure. Based on outside research findings and documented project management challenges, it is quite plausible that an alternative delivery method could have made project administration significantly smoother and quite possibly have saved schedule time and change order money.

Project Overview

The NEOMED Research and Graduate Education building and Comparative Medical Unit expansion project is the first phase of a multi-phase campus expansion plan at the Northeast Ohio Medical University. The project consists of the RGE, a four-story 63,000 SF biomedical research building. The first three floors are fully built out with laboratory and support spaces, offices, and small group instruction rooms. The fourth floor is shelled in and will be built out in the future as the research program grows. There is a half-basement of roughly 6,000 SF housing a stand-alone utility plant.

The CMU expansion (noted as V on the map below) consists of a 14,500 SF addition to an existing facility housing a multispecies vivarium and research spaces for animal models of human disease. This facility provides all animal care services for research and instruction at the university. Areas for behavioral analysis, cage washes, multispecies holding and processing, and storage for feed and bedding are all contained in the new addition.

As a minor component of the project, several existing wet laboratories in the existing Building D were renovated. These labs now constitute the REDI-Zone, an area dedicated to public-private partnership research and development with early-stage biomedical companies.

Several other projects have been constructed within the last five years at the NEOMED campus. NEOMED's first on-campus housing, named The Village, opened August 2013 along with the Phase 1 addition studied in this report. Phase 2 of expansion consisted of the NEOMED Education and Wellness Center, or NEW Building. Constructed in conjunction with Signet Development, this multi-use facility opened September 2014 and contains an auditorium, event spaces, a high school Bio-Med science academy, a wellness center, the Signet executive boardroom, and several amenities. Phase 3 was planned as a new office and teaching building; this project was dropped earlier during campus planning, but is now under development again.

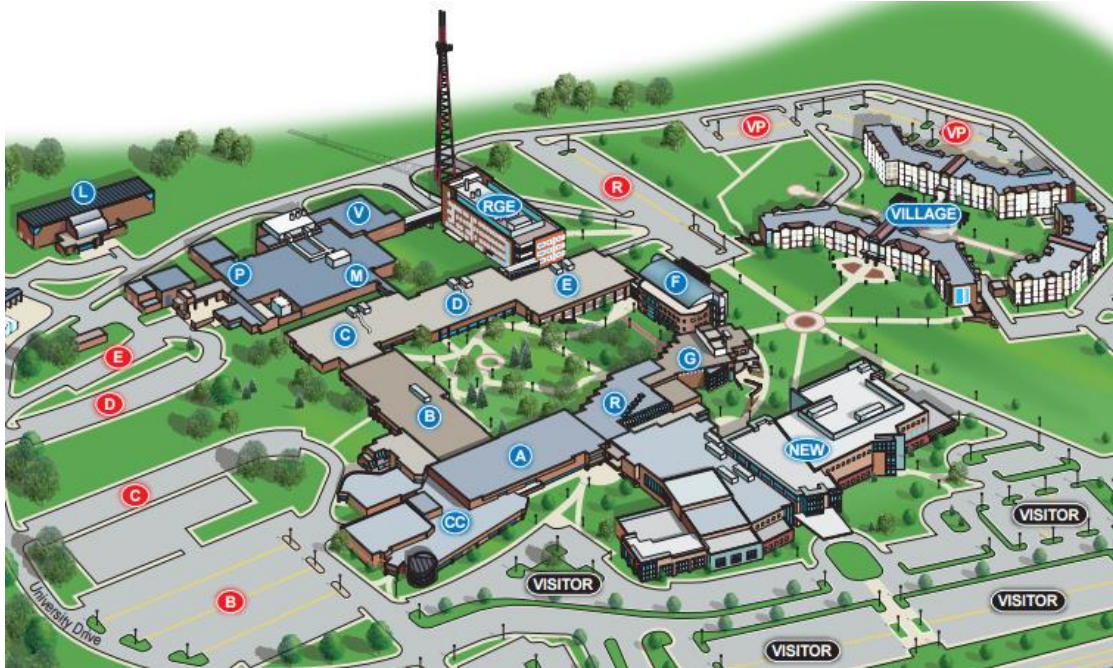


Figure 1: NEOMED Campus Map (Source: www.neomed.edu/map)

Existing Mechanical System

Design Criteria

Objectives and Requirements

The new Research and Graduate Education Building was built to help the university address the biomedical research and education needs of the region. It provides a working space for 30+ scientists focused on research involving better diagnosis and treatment of arthritis, cardiovascular disease, Alzheimer's disease, and innovative ways to design and deliver new medicines. The facility provides full support for teams with offices for faculty, write-up areas for researchers, small group teaching rooms, and open lab and support spaces. The top floor is shelled out for future program expansion.

The existing Comparative Medical Unit provides animal care services for research and teaching programs at the university. It is staffed by 8 personnel under a qualified vet specializing in lab animal medicine. The addition to the existing building was meant to expand animal care capabilities by adding to the vivarium and providing additional mechanical space.

Due to the sensitive nature of the activities in the lab and vivarium spaces, 100% outdoor air is required for these areas. As a result of this requirement, serious thought was given to the different energy recovery measures that could be taken to minimize the energy use of airside systems. HVAC System design was intended to have following characteristics: modular approach, energy responsiveness, flexibility for future changes, durability and ease of maintenance, reliability, and redundancy of critical components.

Code requirements that were followed include:

- Ohio State Building and Mechanical Codes.
- NEOUCOM Design and Engineering Guidelines
- Recommendations of the National Fire Protection Association (NFPA), in general, and, in particular:
 - HVAC: NFPA 90A, 90B, 96
 - HVAC: NFPA 45
- Recommendations of ASHRAE including ASHRAE 62-1999, Indoor Air Quality and ASHRAE/ANSI 15, Chiller Mechanical Rooms.
- National Electrical Code (NEC)
- Energy Conservation Act 222
- ANSI Z 9.5
- USGBC LEED Criteria
- NIH Design Requirements Manual
- Recommendations of AAALAC (animal areas)

Design Influences

Available utilities greatly affect building systems design. Existing campus utilities include electric, natural gas, cold water and sanitary/storm sewer. Electrical service consists of a high voltage loop

stepped down to 480/277 and 208/120 at each building. Site natural gas piping is a mix of low pressure and medium pressure.

With regards to heating, roughly 6 or 8 boiler plants are located at various points on the existing campus. Typically one “heating” location is present for a heating water loop for each building project. The largest of these is the existing boiler and chiller plant in the M building, just to the east of existing CMU. This main plant feeds all of the original 1974 part of campus. The chillers at M Building feed nearly all of the entire campus as well. There are some smaller DX cooling units scattered throughout the campus, but they are not a significant percentage of the campus cooling capacity.

In addition to chillers and boilers, Building M also contains a high pressure steam boiler plant that makes 80 psig steam. Originally a coal fired plant in 1974 with two large coal boilers, it was switched to four natural-gas fired Ohio-Special steam boilers in 1991. The steam plant once served heat exchangers in the M building boiler room, AHU heating coils throughout campus, the DHW tank in the M building, numerous humidifiers throughout campus, and many lab steam outlets, plus steam sterilizers. The NEOMED campus has since downsized their use of steam, and now only hi-pressure steam is distributed to the CMU vivarium equipment, humidifiers in the CMU, and steam sterilizers.

Operability was a major influence in initial design, and is one of the factors that drove the decision to provide stand-alone utilities for the RGE Building. The RGE is intended to be available 24/7 to the scientists and their teams, and also the CMU must be able to provide 24/7 HVAC for the animals in the vivarium.

Distance to existing utilities also drove the decision to include stand-alone utilities. Originally, the design team considered extending the hi-pressure steam from the existing M building boiler room to the new RGE building, but that was cut due to budgetary concerns. Space was reserved in the RGE lab AHUs for humidifiers to be installed later, along with space for a medium pressure steam boiler in RGE basement. Also, the design team looked at extending piping from the central M building boiler and chiller plant; however, there was still going to be a need for additional chilled water and heating capacity so the cost to just include a new plant was very similar. Direct burial was considered as well as an indoor route, but that was complicated by the fact that the bridge connectors were alternate bids. The CMU addition is however connected to the M building boiler and chiller plant as well as the steam plant, seeing as the existing utilities were already located in the original building.

A variable air volume was deemed the safest and most obvious choice for airside systems. Due to the very stringent air change per hour requirements and variety of unique spaces, plus the need for 100% outdoor air, custom air handling units were created for the RGE labs and Vivarium expansion. The office side of the RGE does include a custom 30% outdoor air unit with a mixing plenum and economizer for some energy recovery.

Heat and energy recovery was a critical design point due to the large air turnover rate; a number of options were weighed. Desiccant dehumidification was ruled out, primarily due to the chemicals and contaminants that would be present. The design team did not know how those would have reacted with the desiccants, so they erred on the safer side. Also, the additional efficiency would primarily occur during cooling season and in a cool wet climate it was not “where the money was” with savings. Air-to-air, wheel, and heat-pipe systems were all eliminated as energy recovery systems due to their potential cross-over for contamination. A heat-pipe recovery was briefly considered, but would have needed to be

a two coil design which is a more complex and expensive variety. The only options left were either simple run-around glycol coils or a heat pump between the outside air and exhaust air streams. The design team elected to use glycol coils in the end.

With concern to controls, the team did not consider CO2 monitoring since most spaces were going to have occupancy sensors; some of the sensors unfortunately did get value-engineered out. The new addition has an automatic temperature control system consisting of an independent direct digital control circuit. This circuit is connected and interfaced with the existing campus front ends to allow the campus-wide system to trend recording of the major equipment operation and alarms. This data is used to develop a point schedule for the RGE, as well as to trend recording of environmental conditions and lighting in the CMU to maintain AAALAC accreditation.

A RO/DI water system was provided for the labs and vivarium spaces, sized to supply the feed for the animal watering equipment. A separate laboratory waste collection system was provided to drain all laboratory fixtures. The waste is piped through a duplex limestone chip tank neutralization system.

With regards to fire protection, the new RGE includes a combination wet sprinkler and standpipe system with sprinkler drain risers extended to spill to the exterior. It was important to specify non-ferrous piping and components to be used in areas subject to magnetic fields or equipment. In addition, a new fire pump room was provided in the RGE basement. The existing CMU building was non fire suppressed, so the new addition was designed to remain non fire suppressed with the inclusion of fire separation walls between the existing building and new addition.

Design Conditions

The RGE Building has a variety of laboratory and office spaces, many of which had stringent space thermostat set points. All Occupied spaces were set according to the temperature and humidity settings in Figure 2, taken from Division 23 Section 3 of the BR+A Schematic Narrative.

	<u>Winter °F</u>	<u>Summer °F (±2°F)</u>
<u>Exterior Design Temp.</u>	0	89°db /73°wb
<u>Interior Design Temp.</u>		
Laboratories / support spaces	72	72
Mechanical/Electrical Rooms	65	Vent Only
<u>Supply Air Temperature (at discharge of chilled water coil)</u>	52°F db	51°F db /51.5° wb
<u>Humidity</u>		
Lab / Support spaces	35%±5	50% (±5%)

The project mechanical system was designed with a winter exterior design temperature of 0 degrees F and a summer exterior design temperature of 89 degrees dry bulb/73 degrees wet bulb +/- 2 degrees. Indoor design temperature and humidity varies based on space type. Labs and support spaces are set to 72 degrees F year-

round. Mechanical and electrical rooms are conditioned to 65 degrees during the winter and ventilated with no conditioning in the summer. Animal holding rooms in the CMU have a selectable range from 68-85 degrees to provide species-appropriate conditioning, with the exception of rabbit holding areas set to exactly 65 degrees.

Humidity in the lab and associated support spaces is set to 35%(±5) in the winter and 50% (±5%) in the summer. Vivarium spaces in the CMU are set to 30-40%(±5) during winter and 50% (±5%) during summer.

The majority of the RGE building is configured on a 100% OA system to control contaminants; labs, tissue culture rooms, operating rooms, etc. These rooms, however, have very stringent air circulation requirements. These requirements, given in minimum air changes per hour, ensure that enough uncontaminated fresh air is utilized and that delicate pressure relationships are maintained between rooms so as to avoid contaminant travel. These requirements are outlined below in Figure 3, from Division 23 Section 4a of the Schematic Narrative.

Very specific lighting and power loads are given by Figure 3 in addition to ventilation requirements. Additional values for electric loads are given in Division 26 Section 4a, listed below in Figure 4.

- 1) Laboratories and support spaces
 - Exhaust: 100% Exhaust.
 - Air Circulation: As required by air conditioning load or equipment ventilation load. Min. 6 ACH/HR.
 - Pressure: Negative in relation to corridors and office spaces
 - Electrical Loads: 10 w/sf power, 2 w/sf lighting
- 2) Toilets/Janitors Closets
 - Exhaust: 100% Exhaust
 - Air Circulation: 10 ACH exhaust (min.), constant volume
 - Pressure: Negative to adjacent spaces
 - Electrical Loads: 1.5 w/sf lighting, convenience outlets
- 3) Procedure Rooms
 - Exhaust: 100% Exhaust
 - Air Circulation: 15 ACH minimum, as required for equipment makeup ventilation Load, constant volume
 - Pressure: Negative to adjacent spaces
 - Electrical Loads: 15 w/sf power, 2 w/sf lighting
- 4) Tissue Culture Rooms
 - Exhaust: 100% Exhaust
 - Air Circulation: 15 ACH minimum, as required for cooling
 - Pressure: Positive
 - Electrical Load: 15 w/sf power; 2 w/sf lighting
- 5) Corridors
 - Exhaust: 100% Exhaust
 - Air Circulation: Minimum 6 ACH or requirement for make-up due to labs being at negative pressure.
 - Pressure: Positive to Laboratories
 - Electrical Loads: 1.5 w/sf lighting
- 6) Environmental Rooms
 - Exhaust: 100% Exhaust
 - Air Circulation: 20 CFM ventilation only
 - Pressure: Neutral

Figure 3: Airflow requirements (Source: BR+A Schematic Design Narrative)

4. Normal Power
 - a. The electrical system loads will be designed as follows:
 - 1) 1.5 watts/sq.ft. for lighting.
 - 2) 8 to 10 watts/sq.ft. for Laboratories
 - 3) 10 to 30 watts/sq. ft for Lab Support Spaces
 - 4) 2.0 watts/sq.ft. for power-All Other Areas.
 - 5) 10 to 15 watts/sq.ft. for Plumbing and HVAC air handling equipment.



Figure 4: Light and Power Design Loads (Source: BR+A Schematic Design Narrative)

System Breakdown

The project has utilities independent of the campus infrastructure. Contained within the RGE basement are four 3MMBTU natural gas-powered condensing boilers for heating, two 300-ton electric centrifugal chillers for cooling, and three 1000lb/hr. medium pressure vertical steam boilers for humidifiers and laboratory process equipment.

Most air handling units on the project were custom made by Air Enterprises. Two 100% Outdoor Air AHU's, sized at 37,500 CFM each, serve the lab areas to the west in the RGE. Serving the offices on the east is a smaller AHU at 25,000 CFM and 30% outdoor air. A small constant-volume 4,500 CFM air handler is located in the RGE basement to provide ventilation and space conditioning. The CMU expansion has a new 85,000 unit with 100% outdoor air similar to the two serving the RGE labs.

Running water for the project is provided by a new 6-inch water service. Domestic hot water is provided via duplex 250-gallon gas-fired condensing water heaters located in the RGE basement. The building is designed as a single zone with full recirculation back to the water heaters. A separate supply and return branch provides hot water for the lab equipment and is outfitted with local backflow preventers. The plumbing system is equipped with a duplex water booster to assist in serving the upper floors.

The RGE has a new main electrical service with a single-ended normal power switchboard rated at 480V 3000A. A pad-mounted distribution stepdown transformer takes the 480V down to 208/120V. This transformer is rated at 1500 kVA and is three-phase, four-wire. Power is then circuited throughout the building via double-throw branch automatic transfer switches. A 400kW/500kVA diesel emergency generator sits outside to provide power to the 225A emergency branch serving emergency light and power fixtures. The generator also is connected to a 300A circuit legally required for the fire pump, and an optional 800A standby circuit for HVAC components and select lab equipment.

Lighting in the RGE is mostly fluorescent. All lighting fixtures are suspended from the building structure rather than the ceiling system. Sensors and controls are provided to perform daylight dimming in perimeter areas and zero-occupancy shutoff. Existing Telecommunications system in the Comparative Medical Unit are extended to the expansion and the new RGE Building. 120V power sources, obtained from the emergency/standby system, provide power for alarms and access control system.

Airside

To achieve proper ventilation and space conditioning, there are five total air handling units for the project, broken down in the table below. AHU-1 and AHU-2 are located on the rooftop of the RGE and serve the Lab and Support areas, while AHU-3 is located on the roof as well and serves the RGE offices. AHU-4 is located in the Basement of the RGE and serves to simply provide constant volume ventilation and space conditioning to the mechanical plant. AHU-5 is located on the roof of the CMU addition.

Air Handling Units																
NO.	Type	Area	Min. OA. CFM	Supply			Fans			Exhaust			Coils			
				NO.	CFM/fan	ESP	NO.	CFM/fan	ESP	NO.	CFM/fan	ESP	Heating		Cooling	
													GPM	Tot. MBH	GPM	Tot. MBH
AHU-1	Custom VAV	RGE Labs	50,000	4	12,500	4.0"	-	-	-	2	50,000	4.75"	140	2085	470	3584
AHU-2	Custom VAV	RGE Labs	50,000	4	12,500	4.0"	-	-	-	2	50,000	4.75"	140	2085	470	3584
AHU-3	Custom VAV	RGE Offices	8,400	2	14,000	3.0"	1	28,000	2.0"	-	-	-	51	820	150	1294
AHU-4	Constant	RGE Basem.	450	1	4,500	1.0"	-	-	-	-	-	-	13	194.4	47	187
AHU-5	Custom VAV	CMU exp.	85,000	4	21,250	4.0"	-	-	-	3	42,500	4.0"	270	3420	625	6135

Figure 5: AHU Schedule

Hot Water and Steam

Located in the RGE Basement plant are three 3MMBTU gas-powered condensing boilers providing preheat and reheat water for the airside equipment. A firetube steam boiler was added to the pre-existing CMU steam plant to handle the steam loads of the project. In addition,

Boilers							
NO.	Type	Medium	MBH In	MBH out	GPM	Steam PSIG	Min. Gas input pressure
B-1	Condensing	HW	3,000	2,883	225	-	3.5"
B-2	Condensing	HW	3,000	2,883	225	-	3.5"
B-3	Condensing	HW	3,000	2,883	225	-	3.5"
B-5	Firetube	Steam	1,969	1,697	-	80	9.5"
B-6	Modulating, Condensing	HW	3,000	2,664	133	-	3.5"
B-7	Modulating, Condensing	HW	3,000	2,664	133	-	3.5"

Figure 6: Boiler Schedule

Hydronic Pumps						
	NO.	Type	Service	GPM	Head Pressure (FT H2O)	MHP
RGE	HWP-1	End Suction	Primary Heating Water	450	72	15
	HWP-2	End Suction	Primary Heating Water	450	72	15
	CWP-1	End Suction	Chilled Water Pump	680	65	20
	CWP-2	End Suction	Chilled Water Pump	680	65	20
	TWP-1	Horiz. Split Case	Tower Water Pump	1275	65	30
	TWP-2	Horiz. Split Case	Tower Water Pump	1275	65	30
	HGRP-1	End Suction	AHU-1 Heat Recovery Coil	480	65	15
	HGRP-2	End Suction	AHU-2 Heat Recovery Coil	480	65	15
	HCP-1	In-line	AHU-1 Heating Coil	140	15	1
	HCP-2	In-line	AHU-2 Heating Coil	140	15	1
	HCP-3	In-line	AHU-3 Heating Coil	50	12	0.5
	HCP-4	In-line	AHU-4 Heating Coil	12	12	0.125
	CWP-3	In-line	AHU-4 Cooling Coil	47	25	0.75
	CMU	HWP-1	End Suction	Heating Water	500	50
HWP-2		End Suction	Heating Water	500	50	15
HCP-1		In-line	AHU-5 Heating Coil	270	12	1.5
HGRP-1		End Suction	Heat Recovery	540	65	15

Figure 7: Pump Schedule

Chilled Water

Two 425-ton electric centrifugal chillers are located in the basement plant to provide chilled water for the HVAC equipment. Each Chiller is connected to a cooling tower on the roof of the RGE.

Chillers					
NO.	Type	Tons Output	Min. Turndown Tons	Evap. GPM	Cond. GPM
CH-1	Centrifugal	425	45	680	1275
CH-2	Centrifugal	425	45	680	1275

Figure 8: Chiller Schedule

Cooling Towers						
NO.	Type	Tons	No. Cells	Total GPM	Motors	
					HP	RPM
CT-1	Crossflow	425	1	1275	25	1800
CT-2	Crossflow	425	1	1275	25	1800

Figure 9: Cooling Tower Schedule

Energy Recovery

Within each of the three 100% outdoor air units is a run-around glycol loop for heat recovery.

Loads and Energy Use

During initial building analysis, an energy model/load calculation was constructed in Trane Trace 700 to compare to actual design documents. However, existing design documentation was limited. An Elite load calculation was utilized to quantify the envelope loads of the project, but no other documentation was available for load sizing. No yearly energy analysis had been performed for the project. The combination of existing calculation reports and specified design conditions were used to construct the Trace model, but some inputs were unspecified or unclear so assumptions needed to be made.

Assumptions

Documents provided did not specify any particular occupation densities. Therefore, when calculating internal loads and ventilation requirements, ASHRAE standard values for occupancy per 1000 square foot were internally referenced by the Trace model.

Given the research and laboratory programming of the building, the research function areas are required to maintain delicate pressure relationships. While perhaps not entirely realistic, all areas were modeled in the Trace file as having pressurized tight construction with 0 cooling and heating infiltration.

In the Trace model average values were used for the construction data for building elements. A library entry for the RGE wall was created, based off of section provided in construction drawings. The "RGE Wall" template consists of 5/8" gypsum board, followed by 6" insulation between metal studs, 2.73" high-density stiff insulation, air space, and 4" face brick. Floor slabs were all entered as 4" heavyweight concrete and roof was calculated as 4" lightweight concrete. Interior partitions were all taken as .75" gypsum frame from the preloaded library. All glass was entered as a percentage of wall area, in most areas 38%. The default single clear ¼" window type was utilized.

Trane Trace has a preloaded library of several hundred American cities across the country. Weather data for Akron, Ohio was specified as this was the closest city to the project's Rootstown, Ohio location.

At the time of model construction, no data for typical occupancy schedule was available. While not the most realistic measure, all schedules were specified as 100% available and will need to be modified as more information is obtained.

Heating and Cooling Loads

The first observation taken when the Trace model finished generating reports was that the calculated airflows for most of the air handlers were significantly larger than the design CFM respective to each AHU. The only value that was realistic was the 26,000 CFM cooling airflow calculated for AHU-3, which serves the office spaces. Each of the lab AHU's were designed at 50,000 CFM; AHU-1 was twice that at

98,000 cooling CFM and AHU-2 was a whopping six times design value at 300,000 cooling CFM. The constant volume AHU-4 for the basement was twice design value at 19,000 cooling CFM.

The calculated plant capacities had corresponding overly-large loads. The total system cooling capacity of the RGE came out at 1958 tons, over twice the size of the existing chilled water plant. The system heating capacity came in at roughly 27MMBTU, three times the size of the existing hot water boiler arrangement. Further refinement of the Trace model modified schedule and material assumptions and put out closer, but still unrealistic values.

Trace outputs are summarized in Appendix A. Designer reports from the Elite model are located in Appendix B.

Energy Use

According to the Trace 700 model, yearly electric consumption is on the order of 4,200,000 kWh. Yearly gas consumption is on the order of 200,000 therms and yearly water consumption is 7 million gallons. Building energy consumption comes in at roughly 350 kBtu/SF-year. Source energy consumption comes in at about 655 kBtu/SF-year. Based on Trace default financial values, total annual utility cost is \$221,799 per year. Based on Trane Trace calculations, 7.7 million lbm/year of CO₂ is emitted. 53,200 gm/year of SO₂ is emitted and 13,300 gm/year of NO_x is emitted. Given the error in heating and cooling loads, these numbers are not to be trusted; accurate utility data from the NEOMED campus plant was later gathered during proposal execution and provides a much better assessment of energy use.

ASHRAE Standard Evaluations

ASHRAE 62.1.5-2013: Systems and Equipment

5.1 Ventilation Air Distribution

The RGE, CMU and Building D are all in compliance with Section 5.1. The laboratories, support rooms, vivarium, and other such rooms are supplied with 100% outdoor air, therefore the airflow needed for proper conditioning easily exceeds ventilation requirements. The design documents all have appropriate information for balancing and minimum airflow allowed.

5.2 Exhaust Duct Location

Documents indicate that all exhaust duct runs are negatively pressurized relative to the supply duct runs in each room. The lab exhaust runs through two custom air handling units each at 50,000 CFM. Smaller exhaust fans are located above the office wings, and space is allotted for exhaust fans to be placed for future expansion.

5.3 Ventilation System Controls

The RGE building and the CMU addition each have an independent direct digital control systems interfaced with existing campus network. The system accomplishes all sensing and controlling via electronic actuation of all valves and dampers.

5.4 Air Stream Surfaces

All airstream surfaces are comprised of sheet metal ductwork with metal fasteners to comply with requirements for resistance to mold growth and erosion.

5.5 Outdoor Air Intakes

Outdoor air intake for office end of the RGE building is located on the east face of AHU-3. The outdoor air intake of the laboratory air handlers is located on the north face of the supply air tunnel. All outdoor air intakes are well outside of the required distances; the exhaust stacks for the lab exhaust are 25 feet high per 62.1 Table 5.5.1, giving plenty of distance for the class 4 air to discharge. In addition, each inlet is protected by a mesh screen and louvers to protect from rain, snow, and birds. All AHU’s on the project are equipped with access doors for maintenance purposes.

TABLE 5.5.1 Air Intake Minimum Separation Distance

Object	Minimum Distance, ft (m)
Class 2 air exhaust/relief outlet (Note 1)	10 (3)
Class 3 air exhaust/relief outlet (Note 1)	15 (5)
Class 4 air exhaust/relief outlet (Note 2)	30 (10)
Plumbing vents terminating less than 3 ft (1 m) above the level of the outdoor air intake	10 (3)
Plumbing vents terminating at least 3 ft (1 m) above the level of the outdoor air intake	3 (1)
Vents, chimneys, and flues from combustion appliances and equipment (Note 3)	15 (5)
Garage entry, automobile loading area, or drive-in queue (Note 4)	15 (5)
Truck loading area or dock, bus parking/idling area (Note 4)	25 (7.5)
Driveway, street, or parking place (Note 4)	5 (1.5)
Thoroughfare with high traffic volume	25 (7.5)
Roof, landscaped grade, or other surface directly below intake (Notes 5 and 6)	1 (0.30)
Garbage storage/pick-up area, dumpsters	15 (5)
Cooling tower intake or basin	15 (5)
Cooling tower exhaust	25 (7.5)

Note 1: This requirement applies to the distance from the outdoor air intakes for one ventilation system to the exhaust/relief outlets for any other ventilation system.
 Note 2: Minimum distance listed does not apply to laboratory fume hood exhaust air outlets. Separation criteria for fume hood exhaust shall be in compliance with NFPA 45⁵ and ANSI/AIHA Z9.5.⁶ Information on separation criteria for industrial environments can be found in the *ACGIH Industrial Ventilation Manual*⁷ and in *ASHRAE Handbook—HVAC Applications*.⁸
 Note 3: Shorter separation distances shall be permitted when determined in accordance with (a) ANSI Z223.1/NFPA 54⁹ for fuel gas burning appliances and equipment, (b) NFPA 31¹⁰ for oil burning appliances and equipment, or (c) NFPA 211¹¹ for other combustion appliances and equipment.
 Note 4: Distance measured to closest place that vehicle exhaust is likely to be located
 Note 5: Shorter separation distance shall be permitted where outdoor surfaces are sloped more than 45 degrees from horizontal or that are less than 1 in. (30 mm) wide.
 Note 6: Where snow accumulation is expected, the surface of the snow at the expected average snow depth constitutes the “other surface directly below intake.”

Figure 10: ASHRAE Std. 62.1 Table 5.5.1

5.6 Local Capture of Contaminants

All areas with equipment that generate contaminants, such as labs and restrooms, have exhaust to capture contaminants and direct outdoors away from any intake openings.

5.7 Combustion Air

All laboratory spaces are equipped with fume hoods for removal of any potential combustion products.

5.8 Particulate Matter Removal

Supply air tunnels have a MERV-9 pre-filter and a MERV-14 after-filter within each air handler. Heat recovery coils within exhaust tunnels have MERV-9 pre-filters. Also, room-side replaceable “filter grilles” are used for exhaust of the animal holding room in the CMU. All of these meet the minimum ASHRAE standard of MERV-8 filtration.

5.9 Dehumidification Systems

Lab and support spaces are designed at 35% humidity in winter and 50% humidity in summer. The vivarium is designed at 30-40% winter humidity and 50% summer humidity. These are all less than the required 65% maximum. Regarding section 5.9.2, the RGE has two custom air handling units, with both supply and exhaust at 37,500 CFM for 100% outdoor air intake. The CMU addition has an 85,000 CFM supply and exhaust in a similar fashion.

5.10 Drain Pans

No mention of drain pans is given in the specifications

5.11 Finned-Tube Coils and Heat Exchangers

Plate and frame heat exchangers are utilized on this project rather than finned-tube heat exchangers

5.12 Humidifiers and Water-Spray Systems

The project utilizes Nortec NH series electrode steam humidifiers which are specified to use potable water and drain pans per ASHRAE standard.

5.13 Access for Inspection, Cleaning, and Maintenance

Sufficient access to HVAC equipment has been designed.

5.14 Building Envelope and Interior Surfaces

Architectural wall sections such as Figure 6 indicate a building envelope with rigid insulation, moisture barriers, and batt insulation between studs.

5.15 Buildings with Attached Parking Garages

Building has no attached parking garages, therefore section 5.15 does not apply.

5.16 Air Classification and Recirculation

The laboratories, animal operating rooms, and various technical support spaces are all Class 2 air per Table 6.2.2.1. However, it is important to note that the airstreams from any of the fume hoods is Class 4 as stated by Table 5.16.1. All other areas such as conference rooms and offices are Class 1 air. As stated before, the laboratory and animal care areas are operating on 100% outdoor air with no recirculation. The Class 1 rooms all recirculate air via return ducts. It is also important to note that the biosafety cabinet fume hoods shall recirculate 100% back into the procedure rooms.

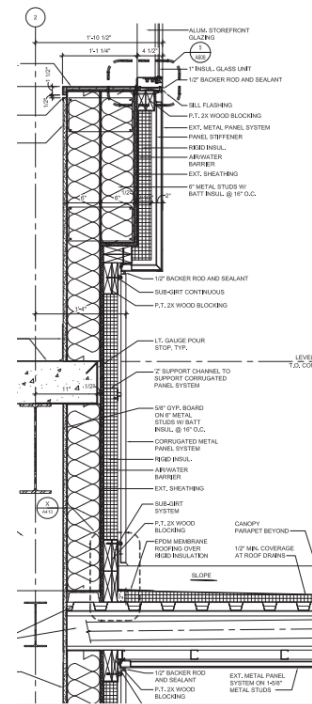


Figure 11: Typ. Architectural Wall Section (Source: TC Architects Construction Documents)

5.17 ETS Air

Smoking is not allowed in any part of the building; 5.17 does not apply.

ASHRAE 62.1.6-2013: Procedures

6.1 General

The site’s outdoor air has no contamination issues and is deemed acceptable for ventilation purposes. Proper ventilation rates are hereby calculated via the prescriptive Ventilation Rate Procedure and the Exhaust Rate Procedure and compared to the existing design specifications. No natural ventilation strategies are used in the design.

6.2 Ventilation Rate Procedure

A preconfigured excel spreadsheet was used to calculate ventilation needed for the offices and conference rooms to the east end of the RGE building, covered by AHU-3. In this project, this was the only air handler configuration that was not configured for 100% outdoor air intake. The breakdown from the spreadsheet calculations is located in Appendix A.

First, breathing zone outdoor air flow rates are calculated with Equation 6-1 from ASHRA 62.1-2013 for each room

$$V_{bz} = R_p * P_z + R_a * A_z$$

Where R_p is outdoor airflow rate per person, P_z is zone population by occupancy class, R_a is outdoor airflow rater per area, and A_z is the area covered by the zone. Table 6-1 of ASHRAE Standard 62.1-2013 contains values for both R_p and R_a , and is referenced by the spreadsheet.

The next step is to find and factor in the zone air distribution effectiveness E_z , found in Table 6-2. In all instances examined, supply air was delivered via ceiling diffusers at cooling temperature, so E_z was 1.0 all around. These values are also referenced in the spreadsheet in Appendix A.

After entering area and airflow data from the drawings, the total supply airflow amounted to roughly 19,600 CFM. This is slightly less than the design value for AHU-3 of 28,000 CFM. Figure 7 below gives a breakdown of total system ventilation.

Results			
Ventilation System Efficiency	Ev		0.80
Outdoor air intake required for system	Vot	cfm	1609
Outdoor air per unit floor area	Vot/As	cfm/sf	0.17
Outdoor air per person served by system (including diversity)	Vot/Ps	cfm/p	12.1
Outdoor air as a % of design primary supply air	Ypd	cfm	8%

Figure 12: AHU-3 Ventilation Breakdown

Also, tallying up the individual zones indicates a surplus of 1294 CFM of unneeded outdoor air and a maximum Z_p value of .26. This could present an opportunity for energy savings.

ASHRAE 90.1.5-2013: Building Envelope

5.1 General

As shown by Figure B1-1 in ASHRAE Standard 90.1-2013 Section 5.1.4, the project’s location in Rootstown, Ohio places it in the 5A Climate Zone, a relatively cool, moist region.

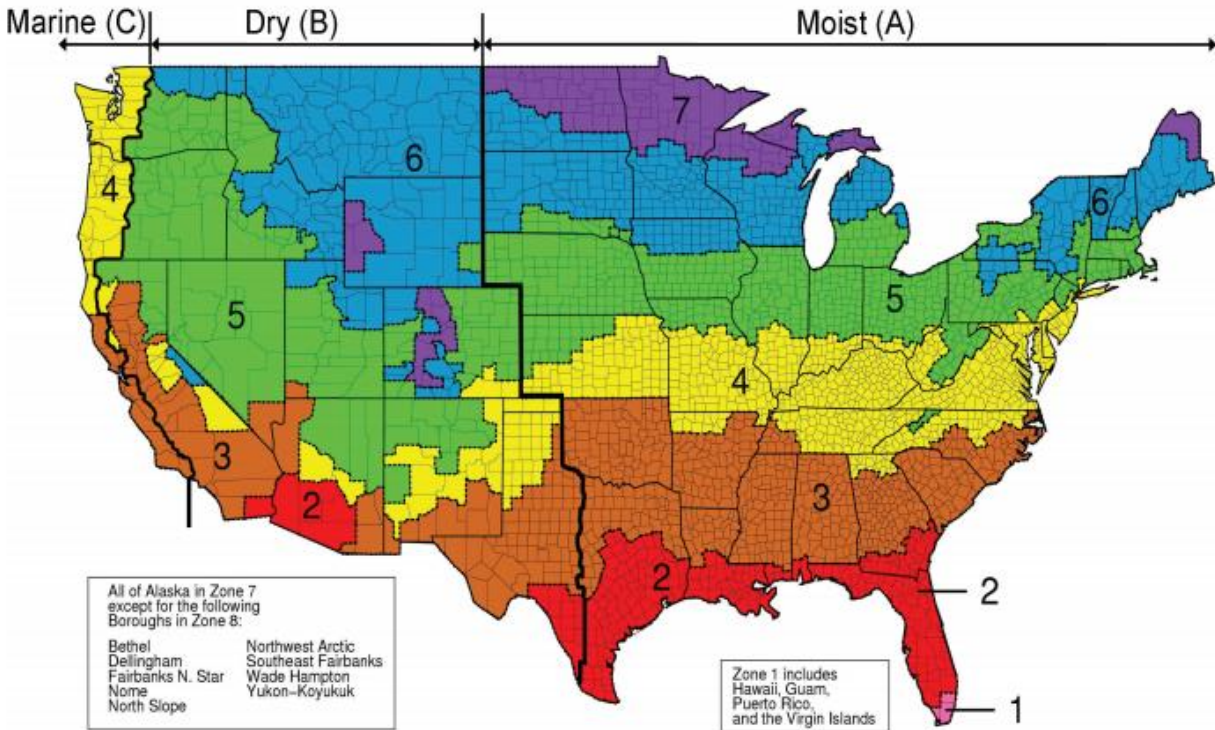


Figure B1-1 U.S. climate zone map (ASHRAE Transactions, Briggs et al., 2003).

Figure 13: ASHRAE Std. 90.1.5.1.4 Figure B1-1

5.2 Compliance Paths

Here we will elect to use the prescriptive evaluation for the building envelope outline in Section 5.5 of the code.

5.4 Mandatory Provisions

The building is constructed with a continuous air and water membrane throughout the entirety of the envelope. In addition, the entrances to the RGE and CMU have vestibules per section 5.4.3.4 of the code.

5.5 Prescriptive Building Envelope Option

Insulation values for the envelope are not available, making the envelope difficult to access. More information finding will be required.

ASHRAE 90.1.6-2013: Heating, Ventilation, and Air Conditioning

6.4 Mandatory Provisions

The prescriptive path outlined in Section 6.4 of Standard 90.1-2013 shall be followed as the building project does not meet the size criteria for the simplified approach outlined in Section 6.3. All equipment meets efficiency standards outlined in the tables of Section 6.8 and load calculations were conducted in the program Chvac 7 in accordance with ASHRAE Standards. The DDC system mentioned in the Standard 62.1.5.3-2013 controls all equipment in accordance with Standard 6.4.3.

6.5 Prescriptive Path

AHU-3 is outfitted with an economizer in accordance with code Section 6.5.1. The automatic temperature control system governs the zone controls via digital sensors and actuators. Also, given the data presented in the analysis of Standard 62.1.6.2 the amount of outdoor air utilized by the office air handler is less than the amount needed to require energy recovery equipment. However, the two AHU's feeding the labs of the RGE and the AHU feeding the CMU expansion use heat pipes with refrigerant to transfer heat from the exhaust stream to the supply stream during heating season, and vice versa during the cooling season.

ASHRAE 90.1.7-2013: Service Water Heating

Domestic water service is piped through water softeners with a duplex water system to provide adequate pressure for lab fixtures. Hot water will be provided via duplex 250 gallon condensing water heaters. This equipment is of proper efficiency per standard 7.8.

ASHRAE 90.1.8-2013: Building Power

This project has a new main electrical service made up of a single ended normal power switchboard, diesel emergency generator, branch automatic transfers and an optional standby distribution system. Feeders are sized within the required voltage drop of 2% and branch circuits are sized to no more than 3% voltage drop.

ASHRAE 90.1.9-2013: Building Lighting

All lighting on the project is automatically switched off via low voltage relays or occupancy sensors. Multi-level switch control is provided in perimeter areas to reduce intensity of light during daylight hours.

ASHRAE 90.1.10-2013: Other Equipment

None of the equipment mentioned in Section 10 applies to the project.

LEED Analysis

The project schematic design outline states that the team sought for a basic LEED Certification level. What follows is a quick breakdown of the RGE and CMU's adherence to the Energy and Atmosphere and Indoor Environmental Air Quality sections of the USGBC LEED 2013 Standard for New Construction.

Energy and Atmosphere Credits

EA Prerequisite 1: Fundamental Commissioning and verification- pass

Commissioning performed by PSI, INC

EA Prerequisite 2: Minimum Energy Performance- pass

Option 2- follows ASHRAE Standard 90.1

EA PREREQUISITE: BUILDING-LEVEL ENERGY METERING-pass

New meters installed for natural gas, HW, DCW, CW, Electric at CMU; meters for NG, Electric, and DCW at RGE

EA PREREQUISITE: FUNDAMENTAL REFRIGERANT MANAGEMENT-pass

No CFC's in any of new construction

EA CREDIT: ENHANCED COMMISSIONING-0 pts

No follow-up commissioning after building opened

EA CREDIT: OPTIMIZE ENERGY PERFORMANCE-0 pts

No energy modeling/simulation performed

EA CREDIT: ADVANCED ENERGY METERING-1 pt

Meters are interfaced with campus network. ATC stores data and trends and develops point schedule

EA CREDIT: DEMAND RESPONSE-0 pts

No demand response program used

EA CREDIT: RENEWABLE ENERGY PRODUCTION-0 pts

No renewable energy sources on campus utilized

EA CREDIT: ENHANCED REFRIGERANT MANAGEMENT- 0 pts

No analysis performed on refrigerants used

EA CREDIT: GREEN POWER AND CARBON OFFSETS-0 pts

No contract engaged

Indoor Environmental Quality Credits

EQ PREREQUISITE: MINIMUM INDOOR AIR QUALITY PERFORMANCE-pass

Project meets ASHRAE STD 62.1

EQ PREREQUISITE: ENVIRONMENTAL TOBACCO SMOKE CONTROL-pass

Due to the nature of the activities inside of both the RGE and CMU, smoking is prohibited in or around

EQ CREDIT: ENHANCED INDOOR AIR QUALITY STRATEGIES- 1 pt

Pressurized Vestibules are used at all entryways, areas with potentially hazardous chemicals are kept at negative pressure and sufficiently exhausted, and all AHU's have MERV-14 after filters

EQ CREDIT: LOW-EMITTING MATERIALS- 0pts

EQ CREDIT: CONSTRUCTION INDOOR AIR QUALITY MANAGEMENT PLAN- 0 pts

EQ CREDIT: INDOOR AIR QUALITY ASSESSMENT- 0 pts

EQ CREDIT: THERMAL COMFORT- 0 pts

All temperature and humidity controlled by ddc system to exact design specifications

EQ CREDIT: INTERIOR LIGHTING- 0 pts

Mostly fluorescents used, mostly automatic controls

EQ CREDIT: DAYLIGHT- 0 pts

No daylighting analyses performed

EQ CREDIT: QUALITY VIEWS- 1 pt

Layout and glazing is such that at least 75% of all regularly occupied spaces in RGE have unobstructed outdoor visibility.

EQ CREDIT: ACOUSTIC PERFORMANCE- 0 pts

No acoustical analysis performed

As evidenced by this analysis, the design did not truly aim for any sort of serious LEED certification, despite what the schematic outline states or what the original intent may have been.

Overall System Evaluation

Overall, the system functions very well towards meeting the priorities of the owner, which are running an excellent facility conducive to top-notch biomedical research, while maintaining some level of efficiency and affordability. Given the stringent design conditions, viable system options, and existing conditions, the mechanical design is very reasonable and functions well.

Proposed Redesign

Considerations

When evaluating potential alternatives to the systems already in place on the RGE + CMU project, there were a number of considerations to be made. During conversation with facility administration, it was made very clear that the top priorities of this project during its design and construction were:

- 1) Quality of facility
- 2) 24/7 availability for researchers and staff
- 3) Independence and reliability of systems
- 4) Flexibility for future changes

Cost and energy savings were absolutely important, but the established programming took precedence. Alternate systems and methods were evaluated in the context of these priorities.

Due to the required high air changeovers in many areas, energy recovery was a major consideration during design. While evaluating the existing energy recovery methods, no real practical alternative for air-side energy recovery presented itself. The idea of using active chilled beams in place of VAV was considered as a way of reducing the amount of wasted energy in the HVAC system. While they have been successfully utilized in lab applications, there are a litany of precautions to be taken. Normally chilled beams are only beneficial in labs where the HVAC system is sized largely based on equipment loads and less making up exhaust from fume hoods. The use of chilled beams in a vivarium may not even be allowed via code. While there is some potential for the implementation of chilled beams to result in less energy waste and smaller airside equipment, there is too much risk associated on this particular project due to stringent ACH, humidity, and pressure relationships required.

One major area with potential for alternate methods was within the construction management and delivery of the project. As a very technically challenging project, the RGE + CMU had a high expense relative to size and scope, and a premium on quality. The project was also on a very strict schedule; the new facilities were to be ready for use in time for the start of the 2013 fall semester. However, due to NEOMED being a public university and therefore a public, state-funded building project, the owner was legally required to use a competitively bid multiple-prime contract structure. The project experienced notable schedule over-runs due to weather and delays, and conflicts occurred as a result.

Proposed Alternatives

In light of the stated design priorities and importance of energy conservation, the implementation of cogeneration presented itself as a viable and attractive alternative to the existing system. On-site electricity generation would allow more independence for the facility as well as another layer of reliability. In addition, the excess heat generated is excellent for steam processes, and the project has a sizable, consistent steam requirement. Provisions could be made to accommodate the planned expansion of the shelled-out areas and future humidifiers in the RGE building, or even the other campus projects.

One breadth study consists of electrical work coinciding with CHP application. Interconnection with the existing utility and the implementation of black start capability will both be addressed. The ability to still utilize the electric grid in addition to on-site generation will be very important, but precautions must be

taken with interconnection design to prevent accidents and malfunctions. Being able to restart on-site generation in case of a blackout, without outside assistance, is also another crucial consideration.

The other breadth study consists of the evaluation of the multiple-prime project delivery structure implemented on the project. A comparison to other alternate systems, such as single-prime, design-build, and CM-at-risk will be made by use of real research on different projects. The research will be used to support potential benefits from an alternate delivery system within the context of this particular project.

Proposed Redesign Analysis

Mechanical Depth: CHP Implementation

Research

Research was conducted to learn about the different cogeneration strategies and their benefits and drawbacks. There are currently three main methods used for electrical generation in a CHP system. These are known as prime movers, and can be steam or gas turbines, reciprocating engines, or fuel cells. Fuel cells are a relatively new and underdeveloped technology, and were deemed impractical and inefficient for this project so they were never considered.

Reciprocating engines used for cogeneration are essentially like larger versions of an automobile engine. They tend to have smaller electrical capacities, and so are more suited for smaller plants. They tend to have a higher electrical efficiency than turbines, which results in less heat available for recovery. This heat is usually lower grade, and in the form of hot water. This means that when configured to provide absorption cooling, only a single-effect chiller can be used.

In comparison to turbines, engines have much quicker start times- a typical internal combustion engine can start up within five to ten minutes, whereas steam turbines often need a half hour and assistance from another power source to start up. Engines are much less sensitive to partial loads, and can even be configured in blocks to allow for a wider range in load turndown and better part-load power efficiency.

Turbines used for cogeneration are similar in operation to the turbines used for aircraft. They tend to run larger than reciprocating engines, and due to their lower efficiency they give off more heat for recovery. This heat is of higher-quality steam, which is much more conducive for process steam generation. Also, this high quality heat allows for double effect absorption cooling, which has a higher coefficient of performance than single effect. Steam and gas turbines do not typically respond well to fluctuations in load, and are better used in constant operation applications.

There are advantages and disadvantages to each prime mover available for cogeneration. The most suitable prime mover will depend on factors such as plant size, Thermal-to-Electric Ratio, and the fraction of time the plant is operating known as the Load Factor.

Utility Data Collection and Analysis

The first step toward designing a cogeneration plant for the project was to gather real utility data. Early in the proposal execution, utility data was gathered covering years 2003 through 2014. Each month, Kilowatt-hours, MCF's of gas, average temperature, and dollars spent on electric and gas were tabulated. This raw data is formatted in spreadsheets located in Appendix C.

In another spreadsheet, several calculations were performed to derive utility trends. First, the monthly electric prices were calculated by dividing dollars spent by Kilowatt-hours of consumption. Natural gas prices were calculated in the same manner. Then, using a conversion factor of 293 kWh per MMBTU, the unit prices were converted to identical units and the difference between them was calculated. This difference in price between electric and natural gas is known as the Spark Gap or Spark Spread; it is a good metric for gauging the payback period of on-site generation. Then, in separate cells, Kilowatt-hours values were converted to Kilowatts and MMBTU's converted to MBH. Using the same conversion factor as before, these units were made identical and the Thermal-to-Electric Ratio (λ D) was calculated.

The full spreadsheet is located in Appendix C; the ten-year average of all of these calculations is shown below:

\$/kwh	\$0.077
\$/MMBTU	\$7.85
Spark Gap	\$14.60
kW	1084
MBH	6010
λD	1.63

From this data, we can see that we have an average spark gap of \$14.60, which is not a bad number but not as great as it could be. The average Thermal-to-Electric ratio is 1.63, which is close to the “sweet spot” for CHP of 1.5.

Graphs were constructed with the calculation spreadsheet to identify consistent trends. Plots of electric demand, thermal demand, and Thermal-to-Electric Demand Ratio were created to illustrate monthly trends:

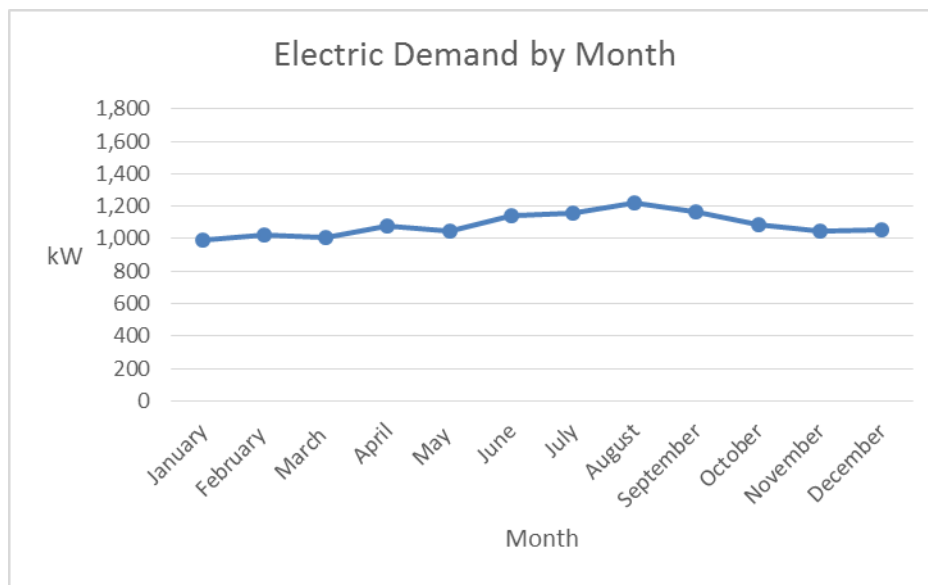


Figure 14: 10-Year Average Electric Load Profile

The electric load profile is relatively stable, with a slight peak during the summer months. This is due to electric chillers on campus operating during the cooling season. Discounting the power used by chillers, the campus has a fairly stable month-to-month demand of around 1000kW.

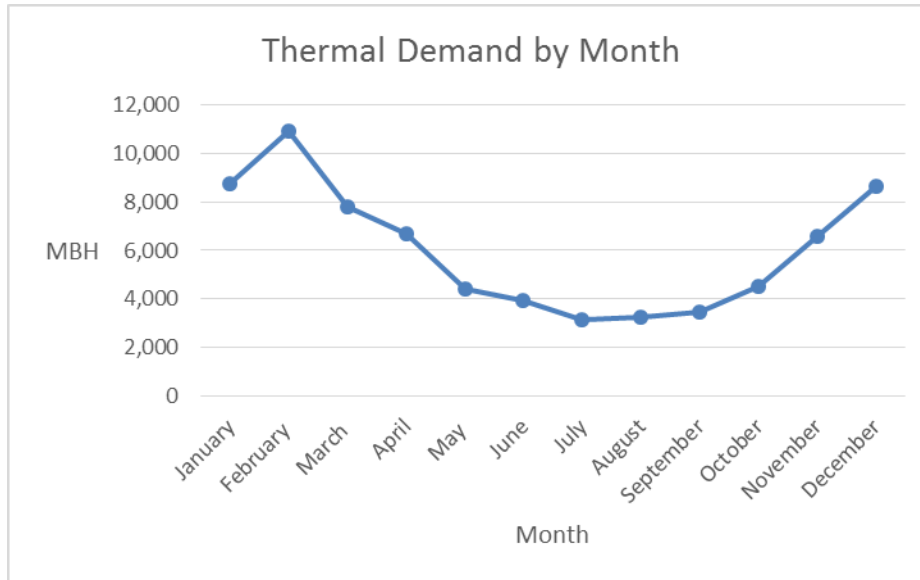


Figure 15: 10-Year Average Thermal Load Profile

Thermal demand varies much more by season than electric, as expected in a temperate area such as northeast Ohio. A peak of about 1100 MBH occurs in February, and a low of around 3500 MBH occurs in the middle of the summer. Given that there are no heating operations during the summer months, we can deduce that this low is the base steam load for the process and humidification needs of the campus.

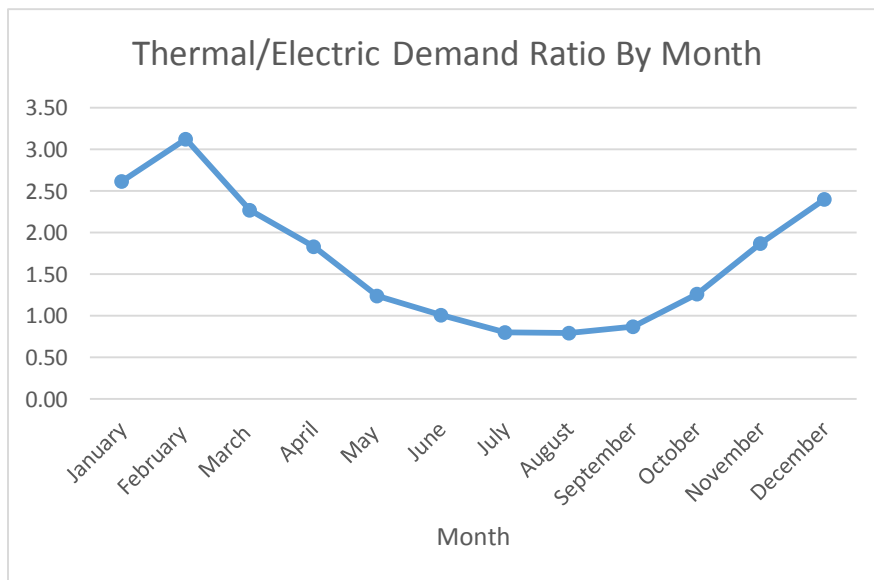


Figure 16: 10-Year Average Thermal-to-Electric Ratio

System Selection Process

A number of existing conditions were evaluated for their conduciveness to cogeneration. One consideration discussed early on was whether to use the cogeneration plant to provide for the RGE and CMU project alone, or to provide for the whole campus. A district system was deemed much more practical, as it would provide much more leeway than a stand-alone system for just one building. A district system could also provide utilities for the later campus expansions, such as the year-round heating required for the lap pool and hydrotherapy pool located in the NEW building. The heating and chilled water plant in the M building adjacent to the project already provides for most of the campus, so it is not unrealistic to expect a cogeneration plant located in the RGE to serve as a district system.

Out of all of the potential uses for recovered heat, the summer steam load identified in early utility analysis seemed like the most logical choice. As a steady load with good relative size to electric demand, this load is conducive to the proposed plant. Other uses for recovered engine heat will still be considered, namely space heating and cooling via absorption chillers.

Other considerations included the need for a dual-fuel prime mover. The natural gas available on site is an excellent fuel with good thermal properties and low emissions, but can become hard to transport in bitter cold weather. A cogeneration system capable of running on other fuels will be very important on this project. In addition, the current RGE basement would not have any room for the new plant; the area would need to be expanded from a half basement to the full building footprint. There is no reason why this could not have been done if it was requested during design; however it must be kept in mind that this would add some cost to the project.

Most of the project conditions and priorities pointed to reciprocating engines as the best prime mover for a CHP plant. However, it is important to have some type of objective analysis to confirm or refute this opinion. An initial screening was performed using a DOE CHP Qualification Tool spreadsheet, with utility data taken from the 10-year average values previously calculated and equipment data taken from design documents and product literature. The full calculation is located in Appendix D.

<u>Site Data Collection</u>															
1. How many hours per year does the facility operate? (hours) Or, ask about operating schedule - day/week, hours/day													8,760		
2. What is your average power demand during operation? (kW), or													1,084		
3. How much electricity do you use in a year, kWh?													9,369,859		
4. What is your facility's primary thermal load (i.e., DHW, steam/HW space heating, process steam, cooling, etc.)													Space Heating		
5. What is your average thermal demand? (MMBtu/hr), or													6.01		
6. How much fuel (gas/oil/etc) do you use in a year? (MMBtu/yr, Therms/yr, etc.)													51,922		
7. What is your current fuel price? (\$/MMBtu)													\$7.850		
8. How much do you pay for fuel annually? (Dollars/yr)													\$405,770		
9. What are the CHP Fuel Costs? (\$/MMBtu)													\$7.850		
10. What is your average electricity price? (\$/kWh)													\$0.077		
11. How much do you pay for electricity annually? (Dollars/yr)													\$712,509		
12. What is the efficiency of your existing boiler(s)/thermal equipment? (decimal)													0.90	RGE HW Boiler	
13. What is the efficiency of your existing chillers? (kWh/ton)													0.60	RGE Chiller	

Figure 17: Initial System Screening Site Data Input

Based on the site data, the spreadsheet logic selected Example System C as the ideal configuration for this project. This configuration consists of a 1000 kW reciprocating engine as the prime mover, with a generating efficiency of 36.8 percent, 3.8 percent higher than typical grid efficiency. This engine gives off roughly 3800 MBH in waste heat, perfect for the base steam load calculated previously.

CHP System					
Net CHP Power, kW	1,084	CHP System Specs	C	Based on thermal match but capped at av	
CHP Electric Efficiency, % (HHV)	36.8%	CHP system specs	C		
CHP Thermal Output, Btu/kWh	3,854	CHP system specs	C		
CHP Thermal Output, MMBtu/hr	4.2	CHP system specs	C		
CHP Power to Heat Ratio	0.89	Calculated based on CHP power output and thermal output			
CHP Availability, %	98%	90 to 98%			
Incremental O&M Costs, \$/kWh	\$0.019	CHP system specs	C		
Thermal Utilization, %	90%	Amount of available thermal captured and used - typically 80 to 100%			
Total Installed Costs, \$/kW	\$2,335	CHP system specs	C		

Figure 18: Screening System Selection

Prime Mover Driven CHP Performance Assumptions	0							
	98.2	772.3	1129.5	3127.2	7170.9	15423.0	22397.9	41420.9
	Based on Recip Engines				Based on Gas Turbines			
Thermal Output, MMBtu/hr	0.34	2.64	3.85	10.67	24.47	52.62	76.42	141.33
Net Capacity, kW	50	600	1,000	3,300	5,000	10,000	20,000	45,000
System	A	B	C	D	E	F	G	H
Heat Rate, Btu/kWh	12,637	9,896	9,264	8,454	11,807	12,482	10,265	9,488
Net Electrical Efficiency, %	27.0%	34.5%	36.8%	40.4%	28.9%	27.3%	33.2%	36.0%
Thermal Output, Btu/kWh	6,700	4,392	3,854	3,233	4,893	5,262	3,821	3,141
Thermal Output, MMBtu/hr	0.34	2.64	3.85	10.67	24.47	52.62	76.42	141.33
Thermal Output for Cooling (single effect)	80%	85%	85%	85%	100%	100%	100%	100%
Thermal Output for Cooling (double effect)	50%	50%	50%	50%	90%	90%	90%	90%
Total Efficiency, %	80%	78%	79%	79%	70%	69%	70%	69%
Incremental O&M, \$/kWh	\$0.0240	\$0.0210	\$0.0190	\$0.0126	\$0.0123	\$0.0120	\$0.0093	\$0.0092
Total Installed Costs, \$/kW	\$2,900	\$2,737	\$2,335	\$1,917	\$2,080	\$1,976	\$1,518	\$1,248

Figure 19: Screening Tool Configuration Specs

This initial screening confirmed that a mid-sized reciprocating engine would be the ideal prime mover for the cogeneration plant. For the next step in analysis, several sizes of GE Jenbacher Model 3 and Model 4 Series engines were used. The Jenbacher is specifically designed for CHP use; it has features including lean burn controls, multiple fuels, and high generating efficiencies.

Configuration Feasibility analysis

In order to properly size the CHP system, it was necessary to use utility data gathered after completion of the project. Using the same method that was used to plot 10-year average trends, plots were made of 2014 (data taken after project completion). On these same plots, 2013 data was plotted as a comparison and to determine if the 2014 data was valid or too different for use.

Based on the plots, it would be reasonable to use the 2014 data as the basis for sizing the CHP plant. The 2014 electrical load profile follows roughly the same pattern as the previous year; it is simply increased in accordance with the RGE and CMU electrical loads. The 2014 thermal profile essentially follows the same pattern as the previous year, with any variability likely due to temperature differences between years. The 2014 profile shows a base thermal load of roughly 4800 MBH, up from a 2900 MBH base load from 2013; the difference is roughly equivalent to the capacity of the steam boiler installed in the project.

From these plots, a thermal load of 4.82 MMBTU will be used for configurations designed to handle the process steam load and the average thermal load of 8.42 MMBtu was used in configurations designed for trigeneration. The average 2014 electric load of 1565 kW was used in all configurations. 2014 prices were also used to best reflect current conditions.

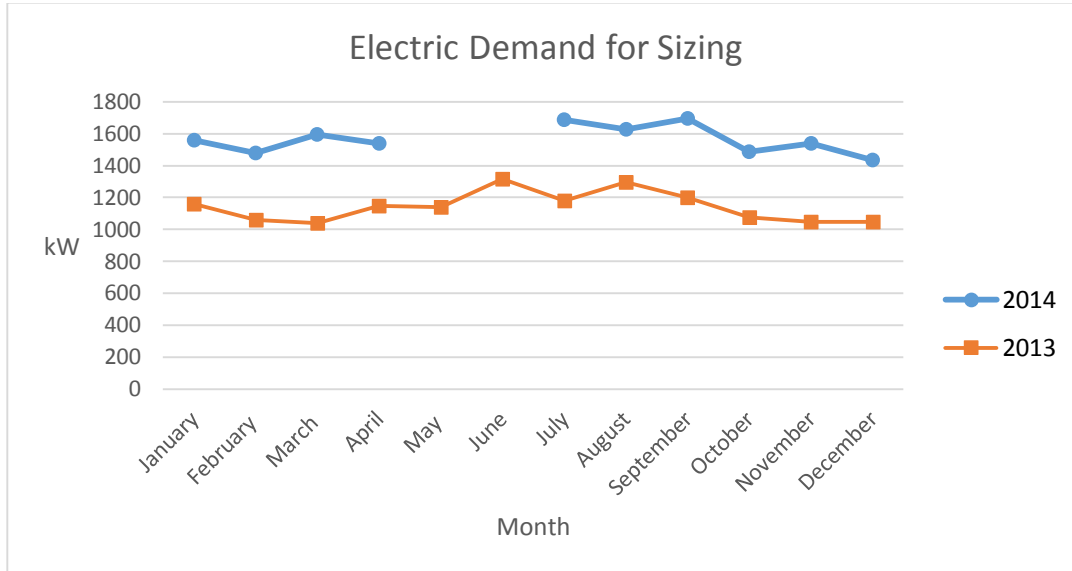


Figure 20: 2013/2014 Electric Load Profile

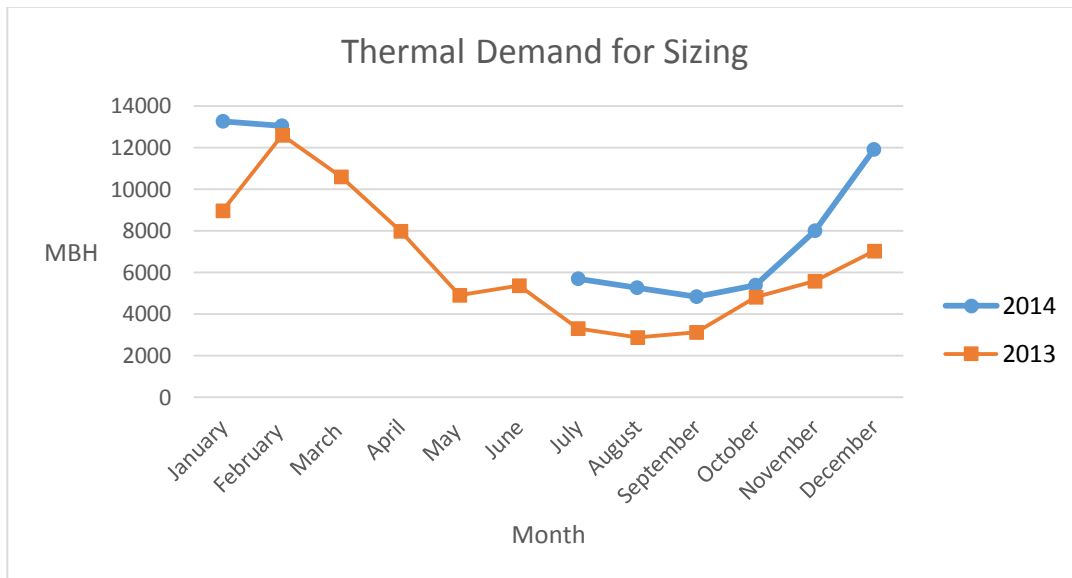


Figure 21: 2013/2014 Thermal Load Profile

Nine configuration were chosen for analysis, based on two variables each with three options:

Generator Configuration: Single vs. Two-Gen. Block vs. Three-Gen. Block (3)
 Waste Heat Application: Steam vs. Heating/Cooling sized to waste heat vs.
 Heating/Cooling sized to cooling load w/ boiler makeup X (3)
 = 9 configs

Each option is listed with corresponding payback period and emissions. Full calculation spreadsheets for payback and emissions are detailed in Appendix E.

Configuration	Equipment Setup	Payback Period	Emissions	
			Vehicles	Houses
A	1 GE Jenbacher J420 with process steam load	8.4	2,201	1,439
B	2 GE Jenbacher J316 with process steam load	10.5	2,630	1,720
C	3 GE Jenbacher J312 with process steam load	14.4	2,945	1,926
D	1 GE Jenbacher J420 with trigeneration, absorption cooling sized to thermal output	11.1	2,076	1,358
E	2 GE Jenbacher J316 with trigeneration, absorption cooling sized to thermal output	11.4	2,461	1,610
F	3 GE Jenbacher J312 with trigeneration, absorption cooling sized to thermal output	14.5	2,756	1,802
G	1 GE Jenbacher J420 with trigeneration, full load absorption cooling with boiler makeup	11.4	2,076	1,358
H	2 GE Jenbacher J316 with trigeneration, full load absorption cooling with boiler makeup	11.5	2,461	1,610
I	3 GE Jenbacher J312 with trigeneration, full load absorption cooling with boiler makeup	14.5	2,756	1,802

Figure 22: Potential Cogeneration Configurations

Based on these results and good engineering judgement, configurations A and B appear to be the most worthy options. A has a single generator sized to the base electric load of 1435 kW, and has just enough waste heat to handle the full process steam load. B has two generators that together can handle the peak 1697 kW electric load, and gives off more than enough heat to feed process steam loads. Out of all the iterations, the ones with steam loads had better emissions scores than ones configured for trigeneration. In addition, options A and B had the best payback periods of 8.4 and 10.5 years, respectively.

Sensitivity Study

A sensitivity analysis was conducted on the top two configurations to gauge the effect of fluctuations in utility rates. While the most current utility rates were used in the configuration screenings, in reality these rates will change over the course of the plant’s life. In all likelihood, electricity will increase in cost due to construction and development, and natural gas will continue to drop due to the growing production of the Utica shale region encompassing northeast Ohio. Reduced gas rates, increased electric rates, and a combination of both were plugged into the screening tool spreadsheets of A and B to predict the effect on payback period.

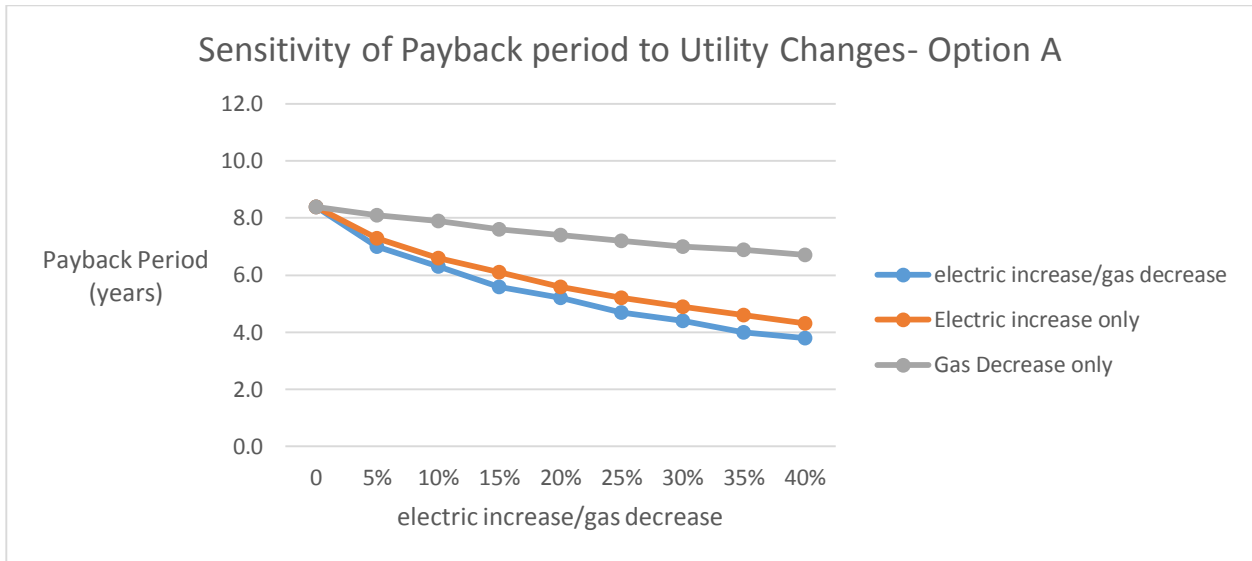


Figure 23: Utility sensitivity-Option A

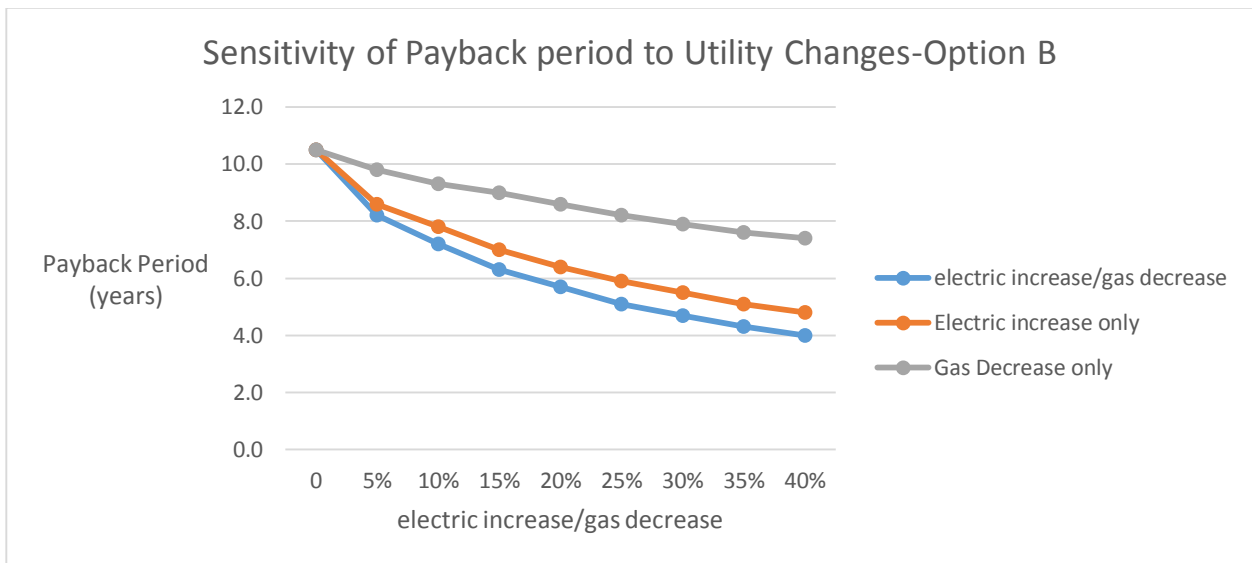


Figure 24: Utility Sensitivity-Option B

The sensitivity analysis shows that while a decrease in gas price will have some positive effect on payback period, increase in electricity cost will have the greatest financial effect. Just a five or ten percent increase in electric rates can shave several years off of payback.

System Configuration and Operation

While the chosen configurations appear conducive to handling steam loads, there is one caveat. In a reciprocating engine cogeneration setup, waste heat is derived from two separate sources: exhaust gas and engine jacket water. The coolant water can be used to produce low-pressure steam via forced circulation; however, only the engine exhaust can be used to generate high-pressure steam. Roughly

half of the Jenbacher engine's waste heat is dissipated in exhaust gas, so there is a limit on how much high pressure steam the cogeneration plant can produce.

The diagram on the following page illustrates the setup of a combination system with two Jenbacher 316 engines producing both high and low pressure steam. Circulation pumps force jacket water to a steam separator, where some of the water flashes to steam at about 10 psig. The remaining water is recirculated to the engine. Attached to each exhaust outlet is a once-through heat recovery steam generator for production of high pressure steam at 60 psig. An OTSG is different from a regular HRSG in that it consists of a simple tube circuit in place of the typical economizer, boiler, superheater arrangement. This eliminates the need for steam drums, blowdown systems, and recirculation systems, making the OTSG much more straightforward and smaller than typical HRSG arrangements. An additional benefit is that an OTSG can run dry, meaning that the engine can still run even when steam is not needed. This arrangement can effectively utilize heat recovery to generate both high pressure steam for process and low pressure steam for humidification in the RGE and CMU

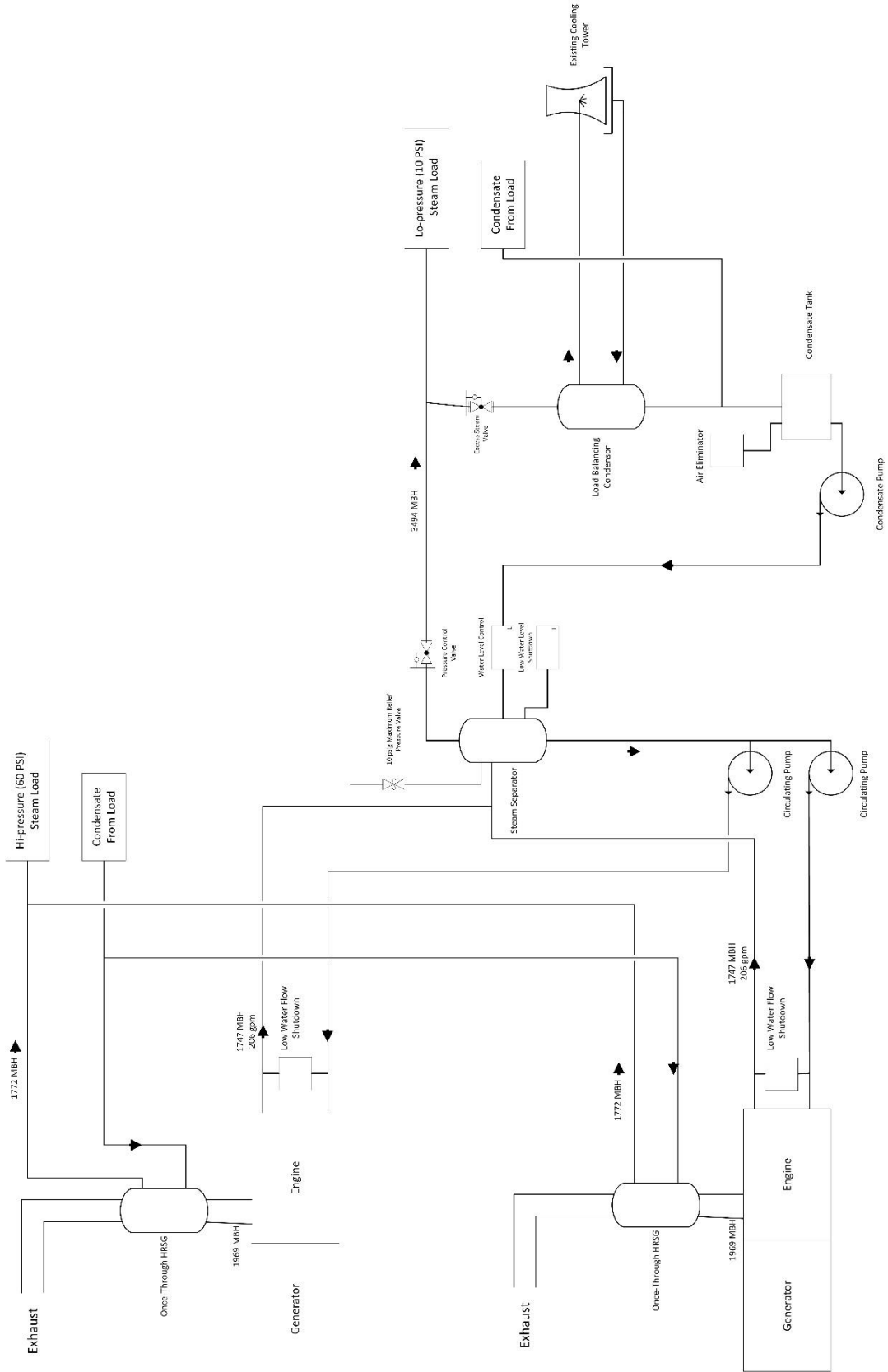


Figure 25: Cogeneration Plant Configuration

Recommendations and Further Expansion

Based upon the analyses conducted, Option B is recommended for implementation. This Cogeneration system consists of two Jenbacher 316 engines each with a generating capacity of 848 kW, combined for almost 1700 kW of generating power for the entire campus. The engine block produces roughly 6700 MBH of useful heat in both liquid and gaseous form. This heat will be used to take care of the campus steam loads.

The configuration was chosen because it is capable of meeting campus peak loads with no outside assistance. As a reciprocating engine block, there is also good turndown capability for meeting part loads during off-hours and base electrical loads during non-cooling periods. In addition, an engine block adds a layer of redundancy; it is unlikely that both engines will go out at the same time. In addition, the extra heat adds a safety factor and also makes further steam load expansion permissible, such as the eventual fitout of the RGE top floor and humidifiers for the RGE rooftop units.

Despite not having the lowest payback period, option B is still reasonable at ten years. Expected fluctuations in utility rates could result in an even shorter period. Bearing in mind, however, this analysis does not factor in other required work such as the need for a full basement and utility tie-in.

Further expansion of the cogeneration system coinciding with later phases of campus expansion could be placed in the full RGE basement; however, it is best practice to place the equipment as close to thermal loads as possible. Therefore, the best option for such expansion would be to locate new equipment somewhere near or inside the NEW Center building.

Electrical Breadth: Power Interconnect and Black Start Capability

Interconnection Laws and Standards

Safe interconnection is a major consideration for any cogeneration system that wants to operate in parallel with the electric grid. Many state authorities have laws and standards governing interconnection to ensure safety and help expedite the application process. However, not all states have these policies, and policy can vary wildly state to state.

The EPA's documentation on state interconnection standards shows that Ohio does in fact have a set of interconnection standards, and that these standards are considered more "district-generation friendly" than those of many other states. For one, Ohio is one of only three states that have no system size limit for interconnection; other policies have limits ranging from 25 MW to 10 kW. Ohio also leaves the decision to provide a disconnect switch at the utility's discretion. In addition, Ohio mandates the practice of net metering for all investor-owned utilities (i.e. on-site generation) regardless of size. Net metering is a practice in which excess electricity generated on-site and distributed elsewhere is used to offset electricity provided by the grid. Several expedited permitting methods exist, depending on system size and type.

Research has shown that Ohio has fairly relaxed rules for grid interconnection, and that there will be no issue with interconnecting the proposed cogeneration system.

Utility Interconnect Design

The best option for a facility that wants both on-site generation and grid connectivity is a parallel operation where the electric loads of a campus or facility are actively tracked, then adjust the generator output to match the load with any excess load coming from the grid. Another option would be to operate generators at full load and sell excess electricity back to the utility or receive net metering credits. While Ohio does have a net metering policy, it was deemed wiser to operate with the first option. The proposed cogeneration setup can be operated at part-load when needed, which use less gas than constant full load operation, plus it is unknown if the local grid is adequately sized to handle extra load.

Interconnection is often a difficult issue. Utilities and/or state regulations often require considerable protective relays and special fuses or breakers. The standard approach taken by a utility is usually to drop a generator off-line anytime a fault occurs anywhere in the system, which is less than ideal for the facility operator. In fact, due to all the protective measures required, it is not uncommon for facility breakers to trip and kick a generator off-line for unwarranted reasons such as a voltage surge on the utility line. And above all, safety is paramount in design to ensure the protection of facility staff and maintenance personnel.

While voltage regulation is the responsibility of the electric utility, control of current and power factor is the domain of the facility. Generator excitation must be controlled via a power factor controller; over-excitation produces excessive reactive power which reduces the reactive power drawn from the grid and adversely affects current. Communication must be established with the utility to vary excitation with respect to utility network load fluctuations. The practice of controlling power factor acts to incentivize the utility to cooperate with onsite generators.

Another important aspect of interconnection is phase synchronization. A generator that is out-of-synch with the utility can cause large transient faults within the system. During a utility blackout event, it is important to make sure the generator remains isolated when utility service is restored, as it may or may not be in phase with the grid. In addition, problems can occur when a breaker opens on a generator. If the generator is undersized compared to the load present in the system, the generator overloads and begins to drop voltage and frequency. If oversized, the generator may be subject to overspeeding.

Several pieces of equipment are very important for grid interconnect design. Reclosing breakers are a popular alternative to regular circuit breakers; they may be set to interrupt a circuit and then re-energize a line after a certain time. Sectionalizers are more permanent breakers used in conjunction with reclosing breakers to isolate a fault and allow normal power to be restored elsewhere. This system is helpful for mitigating the adverse effects that can result from robust protection relaying, because the generator can quickly be put back online and a circuit breaker doesn't need to be reset every time some small fault occurs. Automatic synchronizers are also frequently employed to ensure that a generator is not brought back online without first being in phase with the utility. A variety of relays are employed for measurement of current, voltage, frequency, and excitation. Another important consideration is the utility transformer; depending on the primary-secondary connection scheme, it may be necessary to replace or modify the transformer to include a grounded leg on the facility side.

The figure on the following pages illustrates a proposed interconnection scheme for the 1696 kW cogeneration plant. It includes a number of the items mentioned in a configuration meant to ensure safe and effective plant operation in parallel with the existing local utility grid.

Black Start Capability

Most reciprocating engines either are self-starting or need the assistance of a battery pack. As a smaller, inverter-based engine, the Jenbacher 316 is capable of self-starting in the event of an outage.

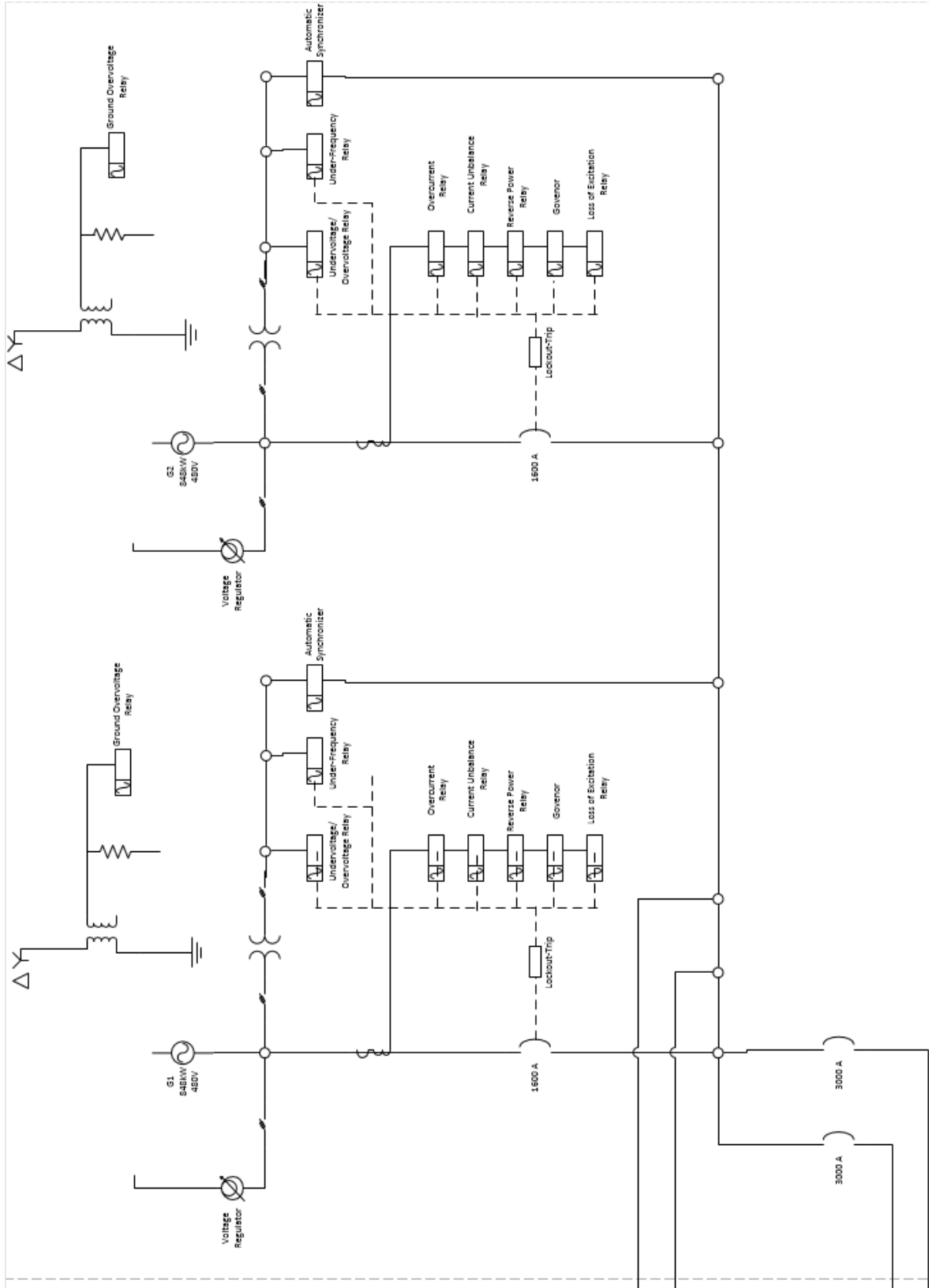


Figure 26: Electric Grid Interconnect Diagram-Part 1

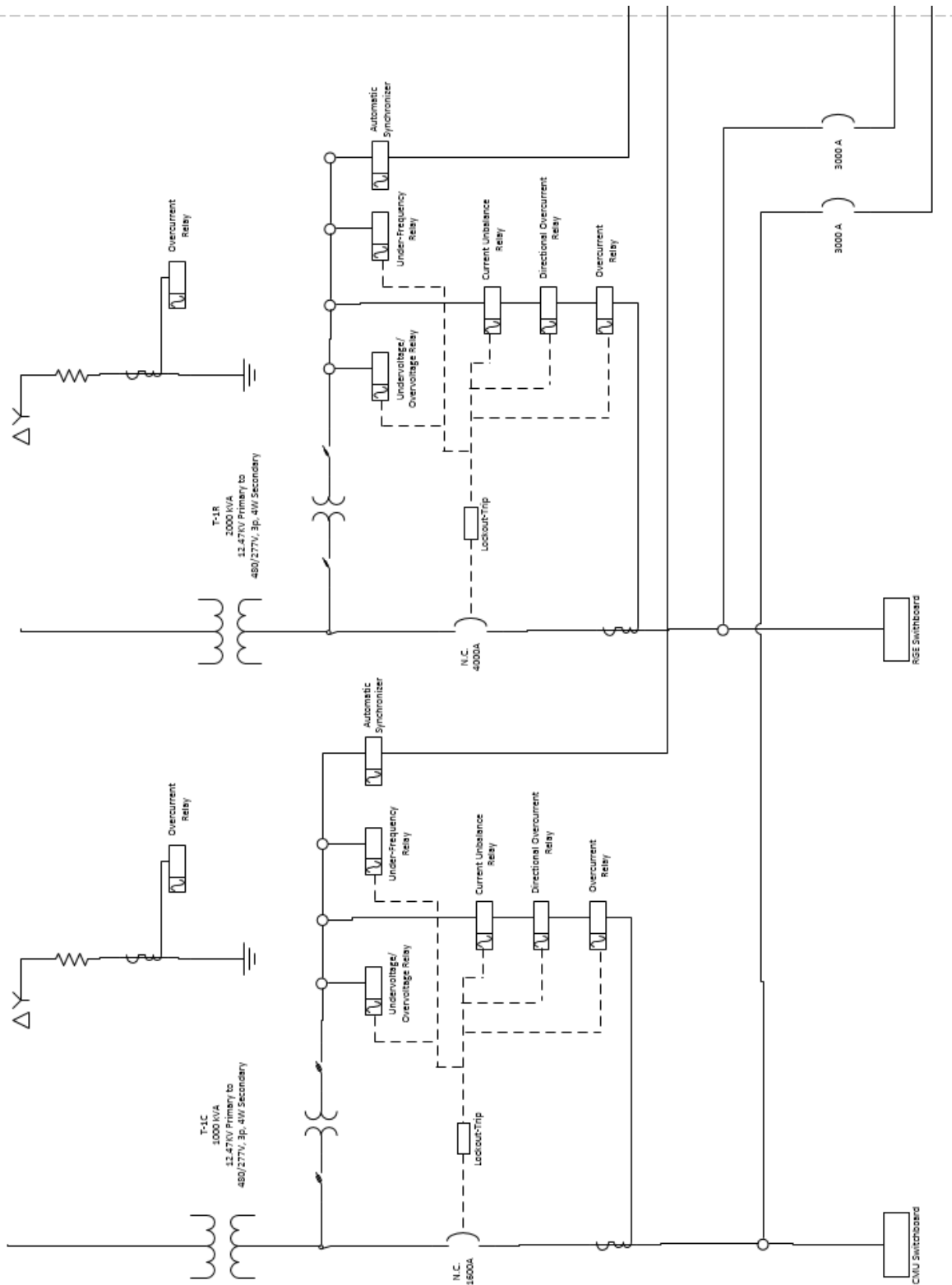


Figure 27: Electric Grid Interconnect Diagram-Part 2

Construction Management Breadth: Alternative Project Delivery

Background

At the time of bidding in 2011, the state of Ohio mandated that all building projects funded with state money were to be awarded as competitive multiple-prime contracts. As a project on a public university, the NEOMED RGE + CMU fell under this ruling and was multiple prime. Early in 2012 the Ohio AIA changed its stance and now allows other delivery methods for state funded building.

While the owner did hire a construction management firm to help manage the project, the firm was only an agent of the owner within the project structure. The CM did not hold any of the contracts for work; as a result the contractors were not beholden to the CM and their advice. The project experienced notable over-runs due to weather and contractor delays, and there were several instances during and after project delivery when conflict arose among the different parties involved on the project. It is quite plausible that had an alternative delivery method been an option at the time, the project could have avoided several obstacles on the way to completion.

Research

To better gain an understanding of real implications of different project delivery methods, established research on the subject was studied. The main source of this data was a study published in a 1998 issue of the Journal of Construction Engineering and Management titled “Comparison of U.S. Project Delivery Systems”. This paper presents data collected from 351 U.S. building projects regarding cost, schedule, and quality in relation to project delivery method. Three methods were chosen for analysis: Design-Bid-Build, Design-Build, and Construction Management at Risk.

The paper used several data sets to further categorize projects. Six different facility types were identified: the RGE + CMU would fall into the “high technology” category, which made up 17% of project surveyed or roughly 60 different projects. The project belongs to the 5,000-15,000 m² range, which encompassed one-third of projects in the study and constituted a small-mid size project bracket. RGE unit cost was calculated with project statistics, and numbers for location index and inflation taken from the RS Means Building Construction 2013 edition:

$$(\$38 \text{ million}/80,000 \text{ SF}) * (100/96 \text{ location index}) * (.558 \text{ inflation } 1998\text{-}2013) = \$274/\text{SF or } \$2950/\text{m}^2$$

This places the RGE in the top unit cost bracket of projects over \$1800/m². It is noted that the majority of these projects also fell into the high technology facility type.

Univariate results showed that ½ of CM-at-Risk and Design-Build projects studied were delivered on time or ahead of schedule. By contrast, ½ of the Design-Bid-Build projects were more than 4% late. In addition, a moderate improvement in quality in both CM-at-Risk and Design-Build was observed relative to Design-Bid-Build quality.

Facility Type	Metric	Unit Cost	Cost Growth	Schedule Growth	Construction Speed	Delivery Speed	Intensity	Turnover Quality	System Quality	Equipment Quality
Light industrial	DB, CMR < DBB	●	○	CMR < DB, DBB	DB, CMR > DBB	DB, CMR > DBB	○	○	DB > DBB	○
Multi-story dwelling	○	○	○	○	○	○	DB > DBB	○	○	○
Simple office	○	○	○	CMR < DBB	○	CMR > DBB	DB > CMR, DBB	CMR > DB, DBB	○	○
Complex office	○	○	○	DB < DBB	○	○	DB > DBB	DB > CMR, DBB	○	DB > CMR
Heavy manufacturing	○	○	○	○	○	○	○	○	○	○
High technology	○	DB < DBB	○	○	○	○	DB > CMR	DB, CMR > DBB	DB > DBB	○

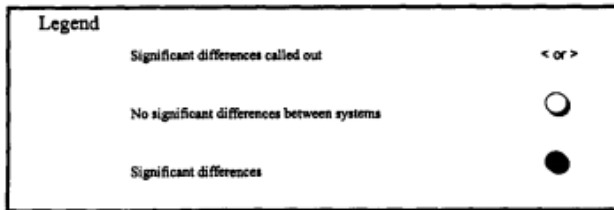


FIG. 2. Matrix of Significance by Facility Type and Owner Type Unadjusted for Other Explanatory Variables

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Figure 28: Univariate Results by Facility Type (Source: J. Constr. Eng. Manage. 1998.124:435-444.)

Univariate results were further broken down by facility type, detailed in the figure above taken from the research paper. High technology projects in the study showed several areas where a Design-Build delivery performed significantly better than Design-Bid-Build, namely cost growth (defined as a percent difference between final cost and contract cost) and system quality. Design-Build showed a significant advantage over CM-at-Risk in intensity, which the report defined as unit cost divided by total project time. Both DB and CM-at-Risk showed significant advantage over DBB in turnover quality, which was measured in three areas: difficulty of facility start-up, number and magnitude of call-backs, and operation and maintenance cost.

When the results were segregated by public vs. private ownership, DB was shown to significantly outperform DBB in all nine categories measured. Publicly-owned CM-at-Risk projects significantly outperformed DBB in schedule growth (percent difference between real time and planned time) and turnover quality specifically. There were no appreciable differences between DB and CMR found for the public projects studied.

In addition to the univariate analysis, a multivariate analysis was conducted in an attempt to explain the variability in unit cost and delivery speed. Overall, a trend was established for both metrics across all projects that had DB performing best, CMR in the middle, and DBB least favorable. Several interesting findings were discussed that pertain to the RGE + CMU project. First, the unit cost of a high technology project was largely determined by physical building size. Interestingly enough, DBB projects were shown to have on average a slight decrease in construction speed with increasing size, which runs opposite of the overall positive correlation found when looking at all studied projects.

The multivariate analysis demonstrated that project delivery played a major role in the success of a project. Delivery method was found to have a significant influence on construction speed specifically, but less so on total delivery speed. Delivery was also the single biggest influence on schedule growth. In fact, it was concluded that project delivery method was the biggest influence across every metric, matched only by facility type.

While many industry professionals hold their own views on different project delivery methods and anecdotes abound, this research provides objective evidence that delivery methods such as Design-Build and CM-at-Risk provide advantages over more traditional methods that would have benefitted this particular project.

Potential Project Benefits

In light of the research conducted an alternate Design-Build delivery system will be proposed for the RGE + CMU project. There are several areas in which this project could have potentially benefitted from a DB approach.

After months of design work, the project began bidding in the fall of 2011. The project was split into three phases of bidding, spaced out over the course of about a year. The project broke ground December 2011 and construction began; owner move-in was originally scheduled for the end of May 2013. Construction had no major delay issues during the early phases of the project. However, around February-March 2013 the schedule started slipping. Following through that spring and summer the project experienced an exponentially-growing schedule slippage. Disputes ensued among the contractors and with the project team on who was to blame. Project completion got pushed back to July and then to August. The owner stated that move-in of faculty and researchers could start no later than July 15 in order to be ready for the coming semester; if move-in was not complete by fall, they would lose hundreds of thousands of dollars in grant money.

Much deliberation ensued and a schedule was eventually devised that summer with sequencing that allowed the owner to move in during July and August while some construction activities were still happening. The RGE and CMU expansion were finally completed late August 2013 and the building was opened for use in time for the fall semester. For more detail, several real project schedules prepared by the construction manager can be found in Appendix H.

However, the electrical contractor made a claim in May 2013 for \$777,000 due to loss of productivity, extension of supervision and general conditions, and other factors resulting from delays as well as a request for more time. This claim was followed by several notices during the summer and fall, and a damage report compiled by an independent consultant submitted November 2013. Following the report, the Architect denied the claim and that winter the parties made several attempts to resolve the dispute at the project level. After these efforts failed, the State Architect's Office threatened to get involved and in response an official mediation was held May 2014 in an attempt to formally settle the dispute.

Based on mediation statements, the contractor's damages report, and correspondence, an idea of how the ordeal ended up could be deduced. The electrical contractor's delay and damages claims were eventually rejected by the state, but it acted as a bargaining chip to gain \$300,000 of smaller claims they wanted and receive their last contract payment of \$279,095. This dispute was simply the largest of a small number of conflicts that arose on the project as a result of project delivery structure.

In conclusion, the project could have benefitted greatly from the implementation of a Design-Build delivery system. The CM agency has experience working on design-build teams, and essentially could have done the same job except with contractual authority to back it up. The management and timely execution of the project could have occurred much more smoothly had an alternative delivery method been available at the time of bidding.

Summary of Work and Conclusions

Based upon the analyses contained within this report, it is plausible that the proposed alternates could have had a positive effect on the design, construction and operation of the Research and Graduate Education and Comparative Medical Unit project. Option B evaluated in the mechanical depth appears to be the most attractive alternate when weighing the different needs and desires of the project according to their priority. Generating on-site electricity to campus full load with waste heat used for steam needs is considerably more feasible than aiming for space heating or trigeneration, or running a generation scheme for a base load or grid buyback.

Research on grid connection requirements and responsibilities for this particular project show that it is quite feasible to implement a parallel operation of on-site generation and local electric grid. In addition, had an alternative project delivery method been possible it could have had a positive effect on project management.

The existing project and the work performed was of excellent quality; the conclusions of this report are in no way meant to imply any flaws. This analysis was conducted in an academic context in which there was much more freedom and flexibility for exploration than in the real world. The opinions expressed within this report are the sole interpretation of the author and reflect the results of a comprehensive educational exercise.

Acknowledgements

I would like to thank a number of people for their help and support over the course of this project. Without their knowledge, expertise and willingness to help I would not have been able to complete this process.

Chris Schoonover	<i>Principal - Scheeser Buckley Mayfield, LLC</i>
Brian Ault	<i>Mechanical Engineer - Scheeser Buckley Mayfield, LLC</i>
Blaine Wyckoff	<i>Director of Campus Operations- Northeast Ohio Medical University</i>
Jim Rankin	<i>Asst. Dir. of Campus Operations- Northeast Ohio Medical University</i>
Jim Freihaut	<i>Professor of Architectural Engineering – Penn State</i>
Rob Leicht	<i>Asst. Professor of Architectural Engineering – Penn State</i>
Tim Warren	<i>President - JDB Engineering, Inc.</i>
Tom Leary	<i>Executive VP/DOP - JDB Engineering, Inc.</i>
Ari Tinkoff	<i>Managing Director/Principal - BR+A Consulting Engineers</i>
Scott Walthour	<i>Managing Principal – Arium AE</i>
Chris Elgin	<i>Structural Engineer - GPD Group</i>
Diet Mt. Dew	<i>Carbonated Soft Drink – PepsiCo Inc.</i>
Steam	<i>Internet-based gaming platform – Valve Corporation</i>

And of course...I would like to thank my friends and family for their love and support

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Appendices

Appendix A: Trane TRACE 700 Reports

SYSTEM SUMMARY
DESIGN AIRFLOW QUANTITIES
By ACADEMIC

System Description	System Type	MAIN SYSTEM					Auxiliary System Supply Airflow cfm	Room Exhaust Airflow cfm
		Outside Airflow cfm	Cooling Airflow cfm	Heating Airflow cfm	Return Airflow cfm	Exhaust Airflow cfm		
Alternative 1								
RGE AHU-1	Variable Volume Reheat (30% Min Flow Default)	68,749	98,914	29,914	98,914	68,749	0	96,704
RGE AHU-2	Variable Volume Reheat (30% Min Flow Default)	297,689	299,521	91,650	299,521	297,689	0	311,391
RGE AHU-3	Variable Volume Reheat (30% Min Flow Default)	3,245	26,354	8,001	26,354	3,245	0	10,572
RGE AHU-4	Bypass Multizone	450	18,956	18,956	18,956	450	0	18,753
Totals		370,133	444,145	148,521	444,145	370,133	0	437,420

Note: Airflows on this report are not additive because they are each taken at the time of their respective peaks. To view the balanced system design airflows, see the appropriate Checksums report (Airflows section).

USE

ONLY

Project Name: Neomed Research and Graduate Education
Dataset Name: TECH 2.trc

TRACE® 700 v6.3 calculated at 03:46 AM on 10/06/2014
Design Airflow Quantities Report Page 1 of 1

SYSTEM SUMMARY
DESIGN COOLING CAPACITIES
 By ACADEMIC

Alternative 1

Building Airside Systems and Plant Capacities

Plant	System	Peak Plant Loads							Block Plant Loads										
		Main Coil	Aux Coil	Opt Vent Coil	Misc Load	Stg 1 Desic Cond	Stg 2 Desic Cond	Base Utility	Peak Total	Time Of	Peak	Main Coil	Aux Coil	Opt Vent Coil	Misc Load	Stg 1 Desic Cond	Stg 2 Desic Cond	Base Utility	Block Total
Cooling plant - 001		1,958.9	0.0	0.0	0.0	0.0	0.0	0.0	1,958.9	7/16	1,749.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	1,749.0
RGE AHU-1		386.6	0.0	0.0	0.0	0.0	0.0	0.0	386.6	7/16	353.8	0.0	0.0	0.0	0.0	0.0	0.0	0.0	353.8
RGE AHU-2		1,486.9	0.0	0.0	0.0	0.0	0.0	0.0	1,486.9	7/16	1,312.4	0.0	0.0	0.0	0.0	0.0	0.0	0.0	1,312.4
RGE AHU-3		54.5	0.0	0.0	0.0	0.0	0.0	0.0	54.5	7/16	53.1	0.0	0.0	0.0	0.0	0.0	0.0	0.0	53.1
RGE AHU-4		30.9	0.0	0.0	0.0	0.0	0.0	0.0	30.9	7/16	29.7	0.0	0.0	0.0	0.0	0.0	0.0	0.0	29.7
Building totals		1,958.9	0.0	0.0	0.0	0.0	0.0	0.0	1,958.9		1,749.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	1,749.0

Building peak load is 1,958.9 tons.

Building maximum block load of 1,749.0 tons occurs in July at hour 16 based on system simulation.

Project Name: Neomed Research and Graduate Education
 Dataset Name: TECH 2.trc

TRACE® 700 v6.3 calculated at 03:46 AM on 10/06/2014
 Design Capacity Quantities report Page 1 of 1

SYSTEM SUMMARY
DESIGN HEATING CAPACITIES
 By ACADEMIC

Alternative 1

System Coil Capacities

System Description	System Type	Main System Btu/h	Aux System Btu/h	Preheat Btu/h	Reheat Btu/h	Humid. Btu/h	Optional Vent Btu/h	Stg 1	Stg 2	Stg 1	Stg 2	Heating Totals Btu/h
								Desic Regen Btu/h	Desic Regen Btu/h	Frost Prevention Btu/h	Frost Prevention Btu/h	
RGE AHU-1	Variable Volume Reheat (30% Min Flow Default)	-3,275,402	0	-3,504,387	-576,530	0	0	0	0	0	0	-6,783,789
RGE AHU-2	Variable Volume Reheat (30% Min Flow Default)	-4,792,309	0	-14,572,320	-1,951,715	0	0	0	0	0	0	-19,364,528
RGE AHU-3	Variable Volume Reheat (30% Min Flow Default)	-1,271,535	0	-170,008	-141,833	0	0	0	0	0	0	-1,441,542
RGE AHU-4	Bypass Multizone	-66,281	0	0	0	0	0	0	0	0	0	-66,281
Totals		-9,409,526	0	-18,246,715	-2,670,078	0	0	0	0	0	0	-27,656,240

Building Plant Capacities

Plant	System	Peak Loads												
		Main Coil MBh	Preheat Coil MBh	Reheat Coil MBh	Humid. Coil MBh	Aux Coil MBh	Opt Vent Coil MBh	Misc Load MBh	Stg 1 Desic. Regen. MBh	Stg 2 Desic. Regen. MBh	Stg 1 Frost Prev. MBh	Stg 2 Frost Prev. MBh	Base Utility MBh	Absorption Load MBh
Heating plant - 002		9,410	18,247	0	0	0	0	0	0	0	0	0	0	0
	RGE AHU-1	3,279	3,504	0	0	0	0	0	0	0	0	0	0	0
	RGE AHU-2	4,792	14,572	0	0	0	0	0	0	0	0	0	0	0
	RGE AHU-3	1,272	170	0	0	0	0	0	0	0	0	0	0	0
	RGE AHU-4	66	0	0	0	0	0	0	0	0	0	0	0	0

Building peak load is 27,656.2 MBh.

Project Name: Neomed Research and Graduate Education
 Dataset Name: TECH 2.trc

TRACE® 700 v6.3 calculated at 03:46 AM on 10/06/2014
 Design Capacity Quantities report Page 1 of 1

Economic Summary

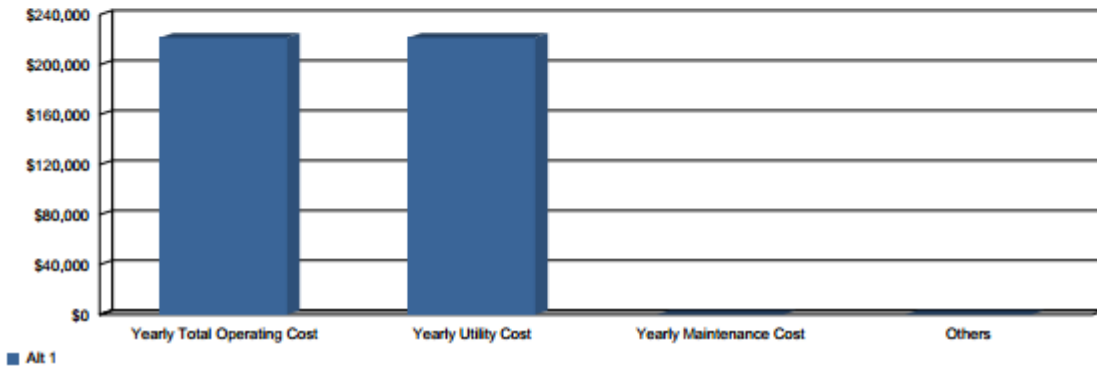
Project Information

Location	Rootstown, Ohio	Study Life:	20 years
Project Name	Neomed Research and Graduate Education	Cost of Capital:	10 %
User	Samuel T Bridwell	Alternative 1:	
Company	The Pennsylvania State University		
Comments			

Economic Comparison of Alternatives

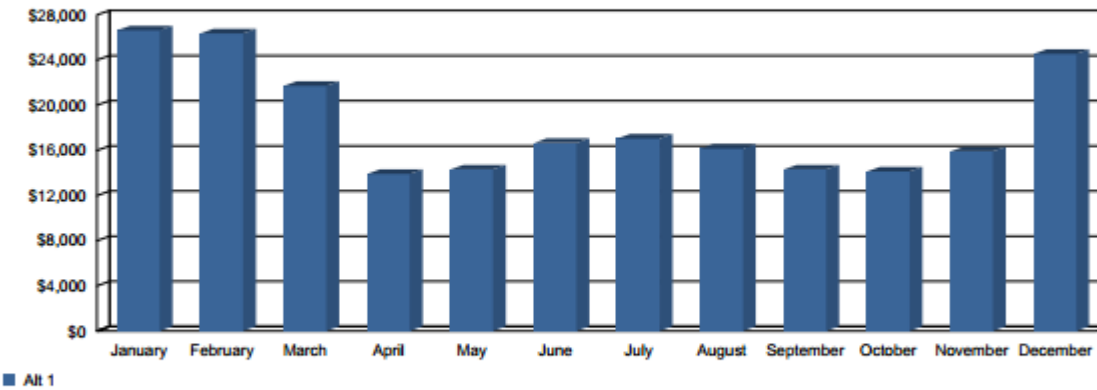
Yearly Savings (\$)	First Cost Difference (\$)	Cumulative Cash Flow Difference (\$)	Simple Payback (yrs.)	Net Present Value (\$)	Life Cycle Payback (yrs.)	Internal Rate of Return (%)	Life Cycle Cost
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Annual Operating Costs



Yearly Total Operating Cost (\$)	Yearly Utility Cost (\$)	Yearly Maintenance Cost (\$)	Plant kWh/ton-hr
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Monthly Utility Costs



Project Name: Neomed Research and Graduate Education
 Dataset Name: TECH 2.trc

TRACE 700 6.3
 calculated at 03:46 AM on 10/06/2014

ENERGY CONSUMPTION SUMMARY

By ACADEMIC

	Elect Cons. (kWh)	Gas Cons. (kBtu)	Water Cons. (1000 gals)	% of Total Building Energy	Total Building Energy (kBtu/yr)	Total Source Energy* (kBtu/yr)
Alternative 1						
Primary heating						
Primary heating		19,913,922		57.9 %	19,913,922	20,962,024
Other Htg Accessories	43,022			0.4 %	146,834	440,546
Heating Subtotal	43,022	19,913,922		58.3 %	20,060,756	21,402,570
Primary cooling						
Cooling Compressor	950,519			9.4 %	3,244,121	9,733,337
Tower/Cond Fans	272,359		7,413	2.7 %	929,562	2,786,966
Condenser Pump				0.0 %	0	0
Other Clg Accessories	10,814			0.1 %	36,908	110,736
Cooling Subtotal....	1,233,692		7,413	12.2 %	4,210,592	12,633,038
Auxiliary						
Supply Fans	1,512,810			15.0 %	5,163,221	15,491,213
Pumps	90,001			0.9 %	307,174	921,613
Stand-alone Base Utilities				0.0 %	0	0
Aux Subtotal....	1,602,811			15.9 %	5,470,395	16,412,826
Lighting						
Lighting	1,355,949			13.5 %	4,627,855	13,884,954
Receptacle						
Receptacles	6,078			0.1 %	20,743	62,235
Cogeneration						
Cogeneration				0.0 %	0	0
Totals						
Totals**	4,241,553	19,913,922	7,413	100.0 %	34,390,341	64,395,620

* Note: Resource Utilization factors are included in the Total Source Energy value.

** Note: This report can display a maximum of 7 utilities. If additional utilities are used, they will be included in the total.

Project Name: Neomed Research and Graduate Education
 Dataset Name: TECH 2.tnc

TRACE® 700 v6.3 calculated at 03:46 AM on 10/05/2014
 Alternative - 1 Energy Consumption Summary report page 1

Energy Cost Budget / PRM Summary

By ACADEMIC

Project Name: Neomed Research and Graduate Education	Date: October 06, 2014
City: Rootstown, Ohio	Weather Data: Akron, Ohio

Note: The percentage displayed for the "Proposed/ Base %" column of the base case is actually the percentage of the total energy consumption.

* Denotes the base alternative for the ECB study.

		* Alt-1		
		Energy 10 ⁶ Btu/yr	Proposed / Base %	Peak kBTuh
Lighting - Conditioned	Electricity	4,627.9	13	528
Space Heating	Electricity	146.8	0	36
	Gas	19,913.9	58	6,994
Space Cooling	Electricity	3,281.0	10	1,666
Pumps	Electricity	307.2	1	111
Heat Rejection	Electricity	929.6	3	224
Fans - Conditioned	Electricity	5,163.2	15	1,620
Receptacles - Conditioned	Electricity	20.7	0	2
Total Building Consumption		34,390.3		

		* Alt-1	
Total		Number of hours heating load not met	Number of hours cooling load not met
		0	0

		* Alt-1	
		Energy 10 ⁶ Btu/yr	Cost/yr \$/yr
Electricity		14,476.4	122,229
Gas		19,913.9	99,570
Total		34,390	221,799

Project Name: Neomed Research and Graduate Education
Dataset Name: TECH 2.lrc

TRACE® 700 v6.3 calculated at 03:46 AM on 10/06/2014
Energy Cost Budget Report Page 1 of 1

MONTHLY ENERGY CONSUMPTION

By ACADEMIC

----- Monthly Energy Consumption -----

Utility	Jan	Feb	Mar	Apr	May	June	July	Aug	Sept	Oct	Nov	Dec	Total
Alternative: 1													
Electric													
On-Pk Cons. (kWh)	232,362	209,454	241,360	266,840	382,432	542,511	673,198	562,125	391,157	263,034	241,512	235,466	4,241,551
On-Pk Demand (kW)	384	392	431	558	968	1,134	1,148	1,094	958	510	452	398	1,148
Off-Pk Demand (kW)	350	392	412	474	735	1,018	1,103	988	818	466	423	395	1,103
Mid-Pk Demand (kW)	404	405	424	475	777	1,122	1,174	1,072	818	455	427	409	1,174
Gas													
On-Pk Cons. (therms)	41,507	40,987	31,096	11,945	1,924	486	118	581	1,294	13,422	18,570	37,209	199,139
On-Pk Demand (therms/hr)	65	70	57	37	9	3	1	3	5	40	45	60	70
Water													
Cons. (1000gal)	57	51	59	179	741	1,525	2,043	1,640	802	190	67	58	7,413
Energy Consumption				Environmental Impact Analysis									
Building Source	349,705 Btu/(ft ² -year)			CO2			7,666,942 lbm/year						
	654,819 Btu/(ft ² -year)			SO2			53,207 gm/year						
				NOX			13,296 gm/year						
Floor Area	98,341 ft ²												

ONLY

Project Name: Neomed Research and Graduate Education
 Dataset Name: TECH 2.3rc

TRACE® 700 v6.3 calculated at 03:46 AM on 10/06/2014
 Alternative - 1 Monthly Energy Consumption report Page 1 of 1

Appendix B: Designer Elite CHVAC 7 Reports

Chvac - Full Commercial HVAC Loads Calculation Program SBM, Inc. Uniontown, OH 44685-8797				Elite Software Development, Inc. Neucom RGE Offices Page 3			
Building Summary Loads							
Building peaks in August at 1pm.							
Bldg Load Descriptions	Area Quan	Sen Loss	%Tot Loss	Lat Gain	Sen Gain	Net Gain	%Net Gain
Roof	5,638	23,257	9.69	0	11,900	11,900	2.29
Wall	8,148	67,219	28.00	0	11,747	11,747	2.26
Glass	6,252	149,585	62.31	0	166,211	166,211	31.97
Floor Slab	0	0	0.00	0	0	0	0.00
Skin Loads		240,061	100.00	0	189,858	189,858	36.52
Lighting	20,043	0	0.00	0	75,229	75,229	14.47
Equipment	30,283	0	0.00	0	113,661	113,661	21.86
People	246	0	0.00	67,650	67,650	135,300	26.03
Partition	0	0	0.00	0	0	0	0.00
Cool. Pret.	0	0	0.00	0	0	0	0.00
Heat. Pret.	0	0	0.00	0	0	0	0.00
Cool. Vent.	0	0	0.00	0	0	0	0.00
Heat. Vent.	0	0	0.00	0	0	0	0.00
Cool. Infil.	0	0	0.00	0	0	0	0.00
Heat. Infil.	0	0	0.00	0	0	0	0.00
Draw-Thru Fan	0	0	0.00	0	5,793	5,793	1.11
Blow-Thru Fan	0	0	0.00	0	0	0	0.00
Reserve Cap.	0	0	0.00	0	0	0	0.00
Reheat Cap.	0	0	0.00	0	0	0	0.00
Supply Duct	0	0	0.00	0	0	0	0.00
Return Duct	0	0	0.00	0	0	0	0.00
Misc. Supply	0	0	0.00	0	0	0	0.00
Misc. Return	0	0	0.00	0	0	0	0.00
Building Totals		240,061	100.00	67,650	452,191	519,841	100.00
Building Summary	Sen Loss	%Tot Loss	Lat Gain	Sen Gain	Net Gain	%Net Gain	
Ventilation	0	0.00	0	0	0	0.00	
Infiltration	0	0.00	0	0	0	0.00	
Pretreated Air	0	0.00	0	0	0	0.00	
Zone Loads	240,061	100.00	67,650	446,398	514,048	98.89	
Plenum Loads	0	0.00	0	0	0	0.00	
Fan & Duct Loads	0	0.00	0	5,793	5,793	1.11	
Building Totals	240,061	100.00	67,650	452,191	519,841	100.00	
Check Figures							
Total Building Supply Air (based on a 17° TD):				25,265	CFM		
Total Building Vent. Air (0.00% of Supply):				0	CFM		
Total Conditioned Air Space:				20,043	Sq.ft		
Supply Air Per Unit Area:				1.2605	CFM/Sq.ft		
Area Per Cooling Capacity:				462.7	Sq.ft/Ton		
Cooling Capacity Per Area:				0.0022	Tons/Sq.ft		
Heating Capacity Per Area:				11.98	Btuh/Sq.ft		
Total Heating Required With Outside Air:				240,061	Btuh		
Total Cooling Required With Outside Air:				43.32	Tons		

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Monday, February 06, 2012, 11:30 AM

Chvac - Full Commercial HVAC Loads Calculation Program SBM, Inc. Uniontown, OH 44685-8797				Elite Software Development, Inc. Neucom RGE Labs Page 3			
Building Summary Loads							
Building peaks in August at 3pm.							
Bldg Load Descriptions	Area Quan	Sen Loss	%Tot Loss	Lat Gain	Sen Gain	Net Gain	%Net Gain
Roof	0	0	0.00	0	0	0	0.00
Wall	9,558	75,269	36.29	0	14,191	14,191	1.06
Glass	5,787	132,161	63.71	0	121,290	121,290	9.05
Floor Slab	0	0	0.00	0	0	0	0.00
Skin Loads		207,430	100.00	0	135,480	135,480	10.11
Lighting	59,835	0	0.00	0	214,374	214,374	16.00
Equipment	212,480	0	0.00	0	761,262	761,262	56.80
People	411	0	0.00	107,888	107,888	215,775	16.10
Partition	0	0	0.00	0	0	0	0.00
Cool. Pret.	0	0	0.00	0	0	0	0.00
Heat. Pret.	0	0	0.00	0	0	0	0.00
Cool. Vent.	0	0	0.00	0	0	0	0.00
Heat. Vent.	0	0	0.00	0	0	0	0.00
Cool. Infil.	0	0	0.00	0	0	0	0.00
Heat. Infil.	0	0	0.00	0	0	0	0.00
Draw-Thru Fan	0	0	0.00	0	0	0	0.00
Blow-Thru Fan	0	0	0.00	0	13,275	13,275	0.99
Reserve Cap.	0	0	0.00	0	0	0	0.00
Reheat Cap.	0	0	0.00	0	0	0	0.00
Supply Duct	0	0	0.00	0	0	0	0.00
Return Duct	0	0	0.00	0	0	0	0.00
Misc. Supply	0	0	0.00	0	0	0	0.00
Misc. Return	0	0	0.00	0	0	0	0.00
Building Totals		207,430	100.00	107,888	1,232,279	1,340,167	100.00
Building Summary		Sen Loss	%Tot Loss	Lat Gain	Sen Gain	Net Gain	%Net Gain
Ventilation		0	0.00	0	0	0	0.00
Infiltration		0	0.00	0	0	0	0.00
Pretreated Air		0	0.00	0	0	0	0.00
Zone Loads	207,430	100.00	107,888	1,219,004	1,326,891	99.01	
Plenum Loads		0	0.00	0	0	0	0.00
Fan & Duct Loads		0	0.00	0	13,275	13,275	0.99
Building Totals		207,430	100.00	107,888	1,232,279	1,340,166	100.00
Check Figures							
Total Building Supply Air (based on a 20° TD):				57,892	CFM		
Total Building Vent. Air (0.00% of Supply):				0	CFM		
Total Conditioned Air Space:				33,050	Sq.ft		
Supply Air Per Unit Area:				1.7516	CFM/Sq.ft		
Area Per Cooling Capacity:				295.9	Sq.ft/Ton		
Cooling Capacity Per Area:				0.0034	Tons/Sq.ft		
Heating Capacity Per Area:				6.28	Btuh/Sq.ft		
Total Heating Required With Outside Air:				207,430	Btuh		
Total Cooling Required With Outside Air:				111.68	Tons		

Chvac - Full Commercial HVAC Loads Calculation Program SBM, Inc. Uniontown, OH 44685-8797				Elite Software Development, Inc. NEOMED CMU Page 3			
Building Summary Loads							
Building peaks in June at 4pm.							
Bldg Load Descriptions	Area Quan	Sen Loss	%Tot Loss	Lat Gain	Sen Gain	Net Gain	%Net Gain
Roof	14,704	68,146	7.83	0	52,478	52,478	5.63
Wall	8,414	34,199	3.93	0	8,255	8,255	0.89
Glass	280	8,487	0.98	0	15,496	15,496	1.66
Floor Slab	0	0	0.00	0	0	0	0.00
Skin Loads		110,832	12.73	0	76,229	76,229	8.17
Lighting	22,056	0	0.00	0	82,784	82,784	8.88
Equipment	21,584	0	0.00	9,680	81,011	90,691	9.73
People	78	0	0.00	21,513	21,513	43,027	4.61
Partition	0	0	0.00	0	0	0	0.00
Cool. Pret.	0	0	0.00	0	0	0	0.00
Heat. Pret.	0	0	0.00	0	0	0	0.00
Cool. Vent.	14,781	0	0.00	372,252	264,166	636,418	68.25
Heat. Vent.	9,948	759,475	87.27	0	0	0	0.00
Cool. Infil.	0	0	0.00	0	0	0	0.00
Heat. Infil.	0	0	0.00	0	0	0	0.00
Draw-Thru Fan	0	0	0.00	0	3,389	3,389	0.36
Blow-Thru Fan	0	0	0.00	0	0	0	0.00
Reserve Cap.	0	0	0.00	0	0	0	0.00
Reheat Cap.	0	0	0.00	0	0	0	0.00
Supply Duct	0	0	0.00	0	0	0	0.00
Return Duct	0	0	0.00	0	0	0	0.00
Misc. Supply	0	0	0.00	0	0	0	0.00
Misc. Return	0	0	0.00	0	0	0	0.00
Building Totals		870,307	100.00	403,445	529,093	932,538	100.00
Building Summary		Sen Loss	%Tot Loss	Lat Gain	Sen Gain	Net Gain	%Net Gain
Ventilation		759,475	87.27	372,252	264,166	636,418	68.25
Infiltration		0	0.00	0	0	0	0.00
Pretreated Air		0	0.00	0	0	0	0.00
Zone Loads		110,832	12.73	31,193	261,537	292,730	31.39
Plenum Loads		0	0.00	0	0	0	0.00
Fan & Duct Loads		0	0.00	0	3,389	3,389	0.36
Building Totals		870,307	100.00	403,445	529,093	932,538	100.00
Check Figures							
Total Building Supply Air (based on a 17* TD):				14,781	CFM		
Total Building Vent. Air (100.00% of Supply):				14,781	CFM		
Total Conditioned Air Space:				14,704	Sq.ft		
Supply Air Per Unit Area:				1.0052	CFM/Sq.ft		
Area Per Cooling Capacity:				189.2	Sq.ft/Ton		
Cooling Capacity Per Area:				0.0053	Tons/Sq.ft		
Heating Capacity Per Area:				59.19	Btuh/Sq.ft		
Total Heating Required With Outside Air:				870,307	Btuh		
Total Cooling Required With Outside Air:				77.71	Tons		

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Monday, February 06, 2012, 11:28 AM

Appendix C: Utility Data and Trends

Electrical Usage and Cost Yearly Comparison													
	FY 03	FY 04	FY 05	FY 06	FY 07	FY 08	FY 09	FY 10	FY 11	FY 12	FY 13	FY 14	Monthly Average
July	Kilowatt Hrs	1,090,800	894,451	864,648	823,121	803,831	801,182	802,301	873,802	742,648	849,188	1,216,025	867,397
	Dollars	\$76,356.00	\$67,205.77	\$68,984.20	\$62,575.46	\$63,667.81	\$68,700.57	\$72,389.56	\$66,113.17	\$55,883.68	\$62,790.24	\$89,539.28	\$67,636.90
	\$/kwh	\$0.070	\$0.075	\$0.072	\$0.076	\$0.079	\$0.086	\$0.090	\$0.082	\$0.076	\$0.075	\$0.074	\$0.074
August	Temperature												
	Kilowatt Hrs	1,039,200	970,422	928,187	918,745	886,110	808,037	790,258	881,642	869,299	932,194	1,171,771	901,393
	Dollars	\$73,246.12	\$67,155.69	\$68,692.77	\$67,713.83	\$69,254.89	\$72,086.86	\$72,350.75	\$72,350.75	\$65,413.83	\$67,165.08	\$70,420.88	\$86,984.41
September	Temperature												
	Kilowatt Hrs	975,600	1,045,788	923,692	793,210	848,130	763,456	826,345	821,581	776,852	864,756	1,221,542	871,827
	Dollars	\$68,278.54	\$73,666.56	\$66,987.11	\$59,813.76	\$68,888.25	\$65,895.67	\$64,755.35	\$61,569.34	\$60,432.26	\$65,455.19	\$91,314.41	\$66,639.60
October	Temperature												
	Kilowatt Hrs	942,000	867,898	830,910	758,171	895,846	793,020	749,675	707,548	733,208	775,208	1,070,569	803,949
	Dollars	\$64,867.04	\$65,309.91	\$62,178.27	\$56,046.41	\$49,896.64	\$68,339.73	\$64,477.73	\$59,299.41	\$54,968.49	\$55,617.58	\$59,044.17	\$73,620.25
November	Temperature												
	Kilowatt Hrs	801,600	814,199	792,234	746,735	783,910	718,951	821,495	709,884	769,813	753,095	1,106,962	781,990
	Dollars	\$65,129.20	\$69,074.02	\$64,833.03	\$53,574.35	\$54,788.41	\$58,782.86	\$59,540.80	\$63,119.86	\$53,737.50	\$56,624.77	\$57,188.91	\$73,920.47
December	Temperature												
	Kilowatt Hrs	789,600	792,906	822,665	753,764	771,334	694,931	737,906	732,248	755,099	754,084	1,032,840	783,484
	Dollars	\$62,255.12	\$64,452.99	\$64,942.47	\$60,201.89	\$64,248.00	\$66,852.25	\$64,703.88	\$66,977.70	\$65,440.83	\$65,424.54	\$67,593.06	\$88,031.99
January	Temperature												
	Kilowatt Hrs	841,200	815,210	759,144	473,077	681,397	703,052	708,704	657,776	650,462	835,841	1,123,259	748,346
	Dollars	\$52,835.99	\$54,003.48	\$52,765.28	\$42,868.36	\$50,664.29	\$53,047.76	\$54,766.11	\$49,798.95	\$48,452.78	\$61,077.50	\$73,960.73	\$55,018.74
February	Temperature												
	Kilowatt Hrs	790,800	810,055	754,786	678,228	777,793	734,842	680,824	675,017	700,753	763,616	1,084,702	763,608
	Dollars	\$63,627.92	\$63,763.63	\$62,550.45	\$60,749.17	\$63,126.01	\$64,161.90	\$55,201.99	\$52,770.13	\$50,632.89	\$60,760.05	\$55,800.98	\$71,054.58
March	Temperature												
	Kilowatt Hrs	794,400	777,011	785,594	669,115	705,942	716,921	720,252	683,767	704,306	748,176	1,148,868	758,537
	Dollars	\$54,355.16	\$53,372.08	\$53,474.80	\$62,252.72	\$51,468.49	\$53,999.39	\$56,455.53	\$53,025.49	\$49,196.09	\$50,887.48	\$54,129.49	\$77,028.99
April	Temperature												
	Kilowatt Hrs	896,400	837,648	757,345	677,027	702,451	752,149	779,435	682,739	828,228	824,821	1,108,614	804,047
	Dollars	\$63,962.46	\$54,934.24	\$56,255.17	\$62,286.25	\$51,362.71	\$56,402.35	\$60,491.36	\$60,456.99	\$51,574.41	\$60,125.30	\$60,277.34	\$73,339.86
May	Temperature												
	Kilowatt Hrs	831,600	769,220	783,602	642,935	730,711	740,803	721,657	772,074	742,967	821,612	1,084,702	755,338
	Dollars	\$58,456.38	\$62,713.62	\$56,140.70	\$59,916.55	\$54,977.62	\$59,716.57	\$61,966.41	\$56,398.65	\$58,508.47	\$57,030.38	\$59,918.87	\$68,704.20
June	Temperature												
	Kilowatt Hrs	963,396	928,351	838,655	625,672	769,400	785,900	779,017	762,090	740,270	873,359	946,424	819,903
	Dollars	\$65,435.81	\$67,224.67	\$65,200.60	\$67,891.83	\$62,101.49	\$67,897.80	\$66,399.81	\$59,368.47	\$53,985.30	\$61,788.08	\$70,790.68	\$63,440.41
Totals	Temperature												
	Kilowatt Hrs	10,756,596	10,323,159	9,941,462	8,560,000	8,007,481	9,412,336	9,084,271	9,064,457	8,902,678	9,146,994	9,869,015	9,369,859
	Dollars	\$738,805.74	\$732,876.66	\$713,104.85	\$715,892.58	\$651,934.32	\$731,842.75	\$741,876.29	\$725,678.47	\$670,939.27	\$680,201.98	\$734,447.11	\$712,509.093
	\$/kwh	\$0.069	\$0.071	\$0.072	\$0.084	\$0.078	\$0.082	\$0.080	\$0.075	\$0.074	\$0.074	\$0.076	\$0.076

Gas Usage and Cost Yearly Comparison		FY 03	FY 04	FY 05	FY 06	FY 07	FY 08	FY 09	FY 10	FY 11	FY 12	FY 13	FY 14	Average per month:
July	MCF's	2,505.30	2,667.61	2,647.06	2,139.01	2,002.50	1,957.90	2,013.40	2,339.90	2,207.60	1,964.50	2,373.90	4,102.00	2,409
	Dollars	\$13,929.47	\$18,895.61	\$18,820.53	\$16,962.35	\$17,101.35	\$15,584.88	\$28,811.75	\$20,331.39	\$18,005.19	\$13,008.92	\$13,664.17	\$19,468.10	\$17,881.98
	\$/MMBTU	\$5.56	\$7.11	\$7.11	\$7.93	\$8.54	\$7.96	\$14.31	\$8.69	\$8.16	\$6.62	\$5.76	\$4.75	\$7.71
August	Temperature													
	MCF's	3,333.58	2,649.95	3,057.88	2,314.00	2,314.00	1,812.60	2,339.70	2,339.70	2,522.00	1,677.10	2,075.30	3,791.50	2,469
	Dollars	\$17,634.65	\$18,841.14	\$21,741.53	\$13,293.18	\$19,692.14	\$13,458.56	\$23,435.66	\$19,534.16	\$20,980.52	\$12,393.77	\$13,292.30	\$16,481.66	\$17,564.94
September	Temperature													
	MCF's	2,568.12	2,910.18	2,984.29	2,075.10	2,079.60	2,251.80	2,471.40	2,854.00	2,819.00	1,983.20	2,251.40	3,466.80	2,563
	Dollars	\$13,585.34	\$20,681.38	\$21,218.30	\$20,460.49	\$17,562.22	\$16,348.07	\$26,023.84	\$24,730.61	\$23,093.25	\$15,355.92	\$15,185.69	\$16,363.29	\$19,218.20
October	Temperature													
	MCF's	2,959.20	4,231.89	3,735.98	2,862.80	3,334.90	2,054.20	3,481.60	4,143.20	3,251.10	2,506.60	3,452.70	3,862.20	3,323
	Dollars	\$15,664.17	\$30,088.74	\$26,562.82	\$26,967.58	\$24,881.69	\$15,433.20	\$36,686.06	\$33,133.17	\$28,687.71	\$20,183.14	\$23,837.44	\$16,893.88	\$25,084.97
November	Temperature													
	MCF's	6,267.30	4,959.15	4,460.92	3,935.50	4,861.00	4,598.70	6,067.60	4,418.80	4,453.50	4,234.80	4,007.90	5,754.50	4,834
	Dollars	\$33,154.02	\$35,259.56	\$31,646.04	\$44,538.11	\$45,780.90	\$38,822.23	\$68,624.56	\$39,716.17	\$39,230.88	\$34,293.41	\$31,013.13	\$26,539.76	\$39,051.56
December	Temperature													
	MCF's	6,834.50	5,873.66	6,253.44	7,094.50	4,928.40	6,196.80	6,537.20	6,503.90	7,764.80	5,282.60	5,051.20	8,572.00	6,408
	Dollars	\$36,154.51	\$41,761.72	\$44,461.96	\$80,948.25	\$51,546.14	\$42,671.16	\$75,439.29	\$49,858.90	\$51,402.98	\$39,397.63	\$37,111.17	\$34,348.00	\$48,758.48
January	Temperature													
	MCF's	6,945.90	8,047.26	1,559.48	4,777.80	5,106.30	5,754.20	8,909.10	7,521.10	7,956.30	6,293.50	6,452.60	9,545.50	6,572
	Dollars	\$36,743.81	\$57,216.02	\$11,087.90	\$38,365.73	\$35,943.25	\$44,433.93	\$100,940.10	\$55,204.87	\$52,511.58	\$42,745.45	\$43,851.87	\$37,332.45	\$46,364.75
February	Temperature													
	MCF's	9,194.60	8,696.89	6,791.38	6,731.50	8,629.70	9,120.30	7,686.50	8,181.20	6,711.60	5,673.20	9,070.60	9,392.70	7,990
	Dollars	\$52,448.23	\$61,834.89	\$48,286.71	\$44,851.98	\$61,857.69	\$73,692.02	\$79,716.69	\$60,393.62	\$45,826.80	\$39,326.62	\$60,909.08	\$45,592.17	\$56,228.04
March	Temperature													
	MCF's	6,042.80	5,915.89	6,144.96	5,604.00	1,723.60	6,958.10	6,201.00	6,120.40	4,994.70	4,501.10	7,630.70	5,622	5,622
	Dollars	\$31,986.41	\$42,061.98	\$43,690.87	\$54,599.77	\$14,492.03	\$68,759.94	\$66,747.56	\$47,310.69	\$37,135.59	\$32,353.91	\$61,900.24	\$45,547.16	\$6,547.16
April	Temperature													
	MCF's	4,865.21	5,000.45	4,192.98	4,334.00	8,560.10	4,264.30	4,710.20	3,865.80	3,592.40	3,815.30	5,735.80	4,812	4,812
	Dollars	\$25,736.96	\$35,553.20	\$29,812.09	\$40,977.97	\$76,253.37	\$41,005.51	\$43,776.60	\$30,636.47	\$26,137.19	\$28,977.20	\$42,106.50	\$38,270.28	\$7,907.28
May	Temperature													
	MCF's	2,988.90	3,490.04	4,115.48	2,896.00	2,420.20	3,712.60	3,101.30	3,581.80	2,127.50	3,059.20	3,524.60	3,183	3,183
	Dollars	\$15,811.28	\$24,814.18	\$29,261.07	\$26,139.30	\$22,144.83	\$38,462.54	\$28,789.37	\$28,382.18	\$15,637.13	\$21,334.86	\$25,190.32	\$25,087.91	\$25,087.91
June	Temperature													
	MCF's	3,253.69	3,163.57	2,535.81	2,575.30	2,669.50	2,663.60	2,645.50	2,546.10	2,398.10	2,504.60	3,868.50	2,820	2,820
	Dollars	\$17,212.02	\$22,492.98	\$18,029.61	\$21,233.35	\$24,563.43	\$32,364.41	\$25,481.46	\$20,068.73	\$16,949.77	\$14,431.51	\$25,829.97	\$21,699.75	\$21,699.75
Totals	Temperature													
	MCF's	\$7,759.10	\$7,596.54	\$8,469.65	\$8,879.51	\$8,629.80	\$11,545.10	\$6,027.40	\$4,456.40	\$5,788.60	\$4,495.70	\$5,495.20	\$5,922	\$5,922
	Dollars	\$310,030.87	\$409,511.40	\$344,619.23	\$429,338.06	\$411,839.04	\$441,036.45	\$604,482.94	\$429,320.96	\$313,802.34	\$375,598.59	\$313,802.34	\$393,891.88	\$405,770.16
Ave. Temp.	\$5.37	\$7.11	\$7.11	\$9.16	\$8.47	\$8.56	\$10.79	\$7.88	\$7.40	\$6.72	\$7.10	\$7.83	\$7.83	

CHP Analysis

		FY 03	FY 04	FY 05	FY 06	FY 07	FY 08	FY 09
July	\$/kwh	\$0.070	\$0.075	\$0.072	\$0.076	\$0.105	\$0.079	\$0.086
	\$/MMBTU	\$5.56	\$7.11	\$7.11	\$7.93	\$8.54	\$7.96	\$14.31
	Spark Gap	\$14.95	\$14.90	\$13.84	\$14.34	\$22.10	\$15.25	\$10.81
	kW	1515	1242	1340	1143	763	1116	1113
	MBH	3480	3691	3676	2971	2781	2719	2796
	ΔD	0.67	0.87	0.80	0.76	1.07	0.71	0.74
	Temperature	0	0	0	74°	74°	69°	69°
August	\$/kwh	\$0.070	\$0.069	\$0.074	\$0.074	\$0.095	\$0.079	\$0.089
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$7.17	\$8.51	\$7.43	\$10.64
	Spark Gap	\$15.36	\$13.17	\$14.57	\$14.42	\$19.45	\$15.82	\$15.50
	kW	1443	1348	1289	1276	862	1231	1122
	MBH	4630	3680	4247	2575	3214	2518	3059
	ΔD	0.94	0.80	0.97	0.59	1.09	0.60	0.80
	Temperature	0	0	0	73°	72°	73°	71°
September	\$/kwh	\$0.070	\$0.070	\$0.073	\$0.075	\$0.088	\$0.081	\$0.086
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$9.86	\$8.44	\$7.26	\$10.53
	Spark Gap	\$15.22	\$13.53	\$14.14	\$12.23	\$17.36	\$16.54	\$14.76
	kW	1355	1452	1283	1102	830	1178	1060
	MBH	3567	4042	4145	2882	2888	3128	3433
	ΔD	0.77	0.82	0.95	0.77	1.02	0.78	0.95
	Temperature	0	0	0	68°	62°	67°	68°
October	\$/kwh	\$0.069	\$0.075	\$0.075	\$0.074	\$0.096	\$0.076	\$0.081
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$9.42	\$7.46	\$7.51	\$10.54
	Spark Gap	\$14.89	\$14.94	\$14.82	\$12.24	\$20.54	\$14.84	\$13.28
	kW	1308	1205	1154	1053	725	1244	1101
	MBH	4110	5878	5189	3976	4632	2853	4836
	ΔD	0.92	1.43	1.32	1.11	1.87	0.67	1.29
	Temperature	0	0	0	54°	50°	59°	60°
November	\$/kwh	\$0.069	\$0.073	\$0.069	\$0.072	\$0.097	\$0.075	\$0.083
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$11.32	\$9.42	\$8.44	\$11.31
	Spark Gap	\$14.86	\$14.15	\$13.21	\$9.70	\$18.99	\$13.53	\$12.96
	kW	1113	1131	1100	1037	785	1089	999
	MBH	8705	6888	6182	5466	6751	6387	8427
	ΔD	2.29	1.78	1.65	1.54	2.52	1.72	2.47
	Temperature	0	0	44°	44°	45°	41°	46°

CHP Analysis

		FY 03	FY 04	FY 05	FY 06	FY 07	FY 08	FY 09
December	\$/kwh	\$0.066	\$0.069	\$0.067	\$0.080	\$0.071	\$0.074	\$0.079
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$11.41	\$10.46	\$6.89	\$11.54
	Spark Gap	\$14.10	\$13.01	\$12.46	\$11.99	\$10.33	\$14.71	\$11.52
	kW	1097	1101	1143	1047	1062	1071	965
	MBH	9492	8158	8685	9853	6845	8607	9079
	ΔD	2.54	2.17	2.23	2.76	1.89	2.35	2.76
	Temperature	0	0	31°	28°	38°	32°	31°
January	\$/kwh	\$0.063	\$0.066	\$0.070	\$0.112	\$0.074	\$0.075	\$0.077
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$8.03	\$7.04	\$7.72	\$11.33
	Spark Gap	\$13.11	\$12.30	\$13.26	\$24.71	\$14.75	\$14.39	\$11.10
	kW	1168	1132	1054	657	946	976	1015
	MBH	9647	11177	2166	6636	7092	7992	12374
	ΔD	2.42	2.89	0.60	2.96	2.20	2.40	3.57
	Temperature	0	0	27°	37°	32°	30°	28°
February	\$/kwh	\$0.068	\$0.066	\$0.070	\$0.090	\$0.068	\$0.074	\$0.075
	\$/MMBTU	\$5.70	\$7.11	\$7.11	\$6.66	\$7.17	\$8.08	\$10.37
	Spark Gap	\$14.17	\$12.34	\$13.29	\$19.58	\$12.84	\$13.52	\$11.73
	kW	1098	1125	1048	942	1080	1021	1017
	MBH	12770	12079	9432	9349	11986	12667	10676
	ΔD	3.41	3.15	2.64	2.91	3.25	3.64	3.08
	Temperature	0	0	31°	30°	20°	26°	20°
March	\$/kwh	\$0.068	\$0.069	\$0.068	\$0.093	\$0.073	\$0.075	\$0.078
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$9.74	\$8.41	\$9.88	\$10.76
	Spark Gap	\$14.76	\$13.02	\$12.83	\$17.52	\$12.95	\$12.19	\$12.20
	kW	1103	1079	1091	929	980	996	1000
	MBH	8393	8217	8535	7783	2394	9664	8613
	ΔD	2.23	2.23	2.29	2.45	0.72	2.84	2.52
	Temperature	0	0	34°	36°	42°	34°	32°
April	\$/kwh	\$0.071	\$0.066	\$0.074	\$0.092	\$0.073	\$0.075	\$0.075
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$9.46	\$8.91	\$9.62	\$9.29
	Spark Gap	\$15.62	\$12.11	\$14.65	\$17.50	\$12.52	\$12.36	\$12.81
	kW	1245	1163	1052	940	976	1045	1113
	MBH	6757	6945	5824	6019	11889	5923	6542
	ΔD	1.59	1.75	1.62	1.88	3.57	1.66	1.72
	Temperature	0	0	52°	53°	47°	53°	42°

CHP Analysis

		FY 03	FY 04	FY 05	FY 06	FY 07	FY 08	FY 09
May	\$/kwh	\$0.070	\$0.082	\$0.072	\$0.093	\$0.073	\$0.082	\$0.084
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$9.03	\$9.15	\$10.36	\$9.28
	Spark Gap	\$15.31	\$16.78	\$13.88	\$18.28	\$12.28	\$13.59	\$15.23
	kW	1155	1068	1088	893	1044	1015	1029
	MBH	4151	4847	5716	4022	3361	5156	4307
	ΔD	1.05	1.33	1.54	1.32	0.94	1.49	1.23
	Temperature	0	0	57°	59°	64°	56°	55°
June	\$/kwh	\$0.068	\$0.072	\$0.078	\$0.092	\$0.081	\$0.086	\$0.085
	\$/MMBTU	\$5.29	\$7.11	\$7.11	\$8.25	\$9.21	\$11.30	\$9.63
	Spark Gap	\$14.61	\$14.11	\$15.67	\$18.86	\$14.44	\$13.95	\$15.34
	kW	1338	1289	1165	869	1069	1091	1082
	MBH	4519	4394	3522	3577	3708	3977	3674
	ΔD	0.99	1.00	0.89	1.21	1.02	1.07	1.00
	Temperature	0	0	73°	67°	70°	69°	63°
Yearly Average	\$/kwh	\$0.069	\$0.071	\$0.072	\$0.085	\$0.083	\$0.078	\$0.082
	\$/MMBTU	\$5.35	\$7.11	\$7.11	\$9.02	\$8.56	\$8.54	\$10.80
	Spark Gap	\$14.75	\$13.70	\$13.89	\$15.95	\$15.71	\$14.22	\$13.10
	kW	1245	1195	1151	991	927	1089	1051
	MBH	6685	6666	5610	5426	5628	5966	6485
	ΔD	1.57	1.63	1.43	1.60	1.78	1.60	1.81
	Temperature	0	0	0	52	51	51	49

CHP Analysis

		FY 10	FY 11	FY 12	FY 13	FY 14	Monthly Average
July	\$/kwh	\$0.090	\$0.076	\$0.075	\$0.074	\$0.074	\$0.080
	\$/MMBTU	\$8.69	\$8.16	\$6.62	\$5.76	\$4.75	\$7.98
	Spark Gap	\$17.75	\$14.01	\$15.43	\$15.91	\$16.83	\$15.39
	kW	1114	1214	1031	1179	1689	1161
	MBH	3250	3066	2728	3297	5697	3132
	ΔD	0.85	0.74	0.78	0.82	0.99	0.80
	Temperature	68°	73°	70°	75	72	
August	\$/kwh	\$0.092	\$0.074	\$0.077	\$0.076	\$0.074	\$0.079
	\$/MMBTU	\$8.35	\$8.32	\$7.39	\$6.41	\$4.35	\$7.61
	Spark Gap	\$18.48	\$13.42	\$15.25	\$15.73	\$17.30	\$15.56
	kW	1098	1225	1207	1295	1627	1218
	MBH	3250	3503	2329	2882	5266	3262
	ΔD	0.87	0.84	0.57	0.65	0.95	0.79
	Temperature	71°	72°	77°	76	71	
September	\$/kwh	\$0.078	\$0.075	\$0.078	\$0.076	\$0.075	\$0.077
	\$/MMBTU	\$8.54	\$8.19	\$7.74	\$6.74	\$4.72	\$7.89
	Spark Gap	\$14.42	\$13.77	\$15.05	\$15.43	\$17.18	\$14.77
	kW	1148	1141	1079	1201	1697	1166
	MBH	4020	3915	2754	3127	4815	3446
	ΔD	1.03	1.01	0.75	0.76	0.83	0.87
	Temperature	64°	63°	70°	70	70	
October	\$/kwh	\$0.079	\$0.078	\$0.076	\$0.076	\$0.069	\$0.078
	\$/MMBTU	\$8.00	\$8.82	\$8.05	\$6.90	\$4.89	\$7.84
	Spark Gap	\$15.18	\$13.94	\$14.17	\$15.41	\$15.26	\$14.93
	kW	1041	983	1018	1077	1487	1083
	MBH	5754	4515	3481	4795	5364	4547
	ΔD	1.62	1.35	1.00	1.30	1.06	1.26
	Temperature	49°	52°	60°	56	61	
November	\$/kwh	\$0.077	\$0.076	\$0.074	\$0.076	\$0.067	\$0.076
	\$/MMBTU	\$8.99	\$8.81	\$8.10	\$7.74	\$4.61	\$8.51
	Spark Gap	\$13.52	\$13.37	\$13.45	\$14.51	\$14.95	\$13.84
	kW	1141	986	1069	1046	1537	1045
	MBH	6137	6185	5882	5567	7992	6598
	ΔD	1.58	1.84	1.61	1.56	1.52	1.87
	Temperature	45°	41°	51°	48	49	

CHP Analysis

		FY 10	FY 11	FY 12	FY 13	FY 14	Monthly Average
December	\$/kwh	\$0.077	\$0.076	\$0.073	\$0.076	\$0.066	\$0.073
	\$/MMBTU	\$7.67	\$6.62	\$7.46	\$7.35	\$4.01	\$8.08
	Spark Gap	\$14.96	\$15.56	\$14.05	\$15.03	\$15.29	\$13.43
	kW	1025	1017	1049	1047	1435	1057
	MBH	9033	10784	7337	7016	11906	8626
	ΔD	2.58	3.11	2.05	1.96	2.43	2.40
	Temperature	29°	24°	39°	40	34	
January	\$/kwh	\$0.077	\$0.076	\$0.074	\$0.073	\$0.066	\$0.076
	\$/MMBTU	\$7.34	\$6.60	\$6.79	\$6.80	\$3.91	\$7.38
	Spark Gap	\$15.30	\$15.58	\$15.03	\$14.61	\$15.39	\$14.92
	kW	984	914	903	1161	1560	992
	MBH	10446	11050	8741	8962	13258	8753
	ΔD	3.11	3.54	2.83	2.26	2.49	2.62
	Temperature	24°	22°	34°	33	28	
February	\$/kwh	\$0.078	\$0.075	\$0.072	\$0.073	\$0.067	\$0.074
	\$/MMBTU	\$7.38	\$6.83	\$6.93	\$6.72	\$4.85	\$7.28
	Spark Gap	\$15.33	\$15.15	\$14.29	\$14.70	\$14.70	\$14.27
	kW	946	938	973	1061	1479	1023
	MBH	11363	9322	7879	12598	13045	10920
	ΔD	3.52	2.91	2.37	3.48	2.58	3.12
	Temperature	25°	23°	33°	27	19	
March	\$/kwh	\$0.078	\$0.076	\$0.072	\$0.072	\$0.067	\$0.075
	\$/MMBTU	\$7.73	\$7.43	\$7.19	\$8.11		\$8.07
	Spark Gap	\$14.99	\$14.81	\$13.98	\$13.09		\$13.85
	kW	950	900	978	1039	1596	1004
	MBH	8501	6937	6252	10598		7808
	ΔD	2.62	2.26	1.87	2.99		2.28
	Temperature	41°	34°	35°	31	26	
April	\$/kwh	\$0.078	\$0.076	\$0.073	\$0.073	\$0.066	\$0.075
	\$/MMBTU	\$7.93	\$7.30	\$7.59	\$7.34		\$7.90
	Spark Gap	\$14.80	\$14.84	\$13.68	\$14.07		\$14.09
	kW	1083	948	1150	1146	1540	1078
	MBH	5369	4976	5299	7966		6683
	ΔD	1.45	1.54	1.35	2.04		1.83
	Temperature	53°	42°	53°	39	42	

CHP Analysis

		FY 10	FY 11	FY 12	FY 13	FY 14	Monthly Average
May	\$/kwh	\$0.078	\$0.076	\$0.077	\$0.073		\$0.078
	\$/MMBTU	\$7.92	\$7.35	\$6.97	\$7.15		\$7.88
	Spark Gap	\$14.97	\$14.85	\$15.52	\$14.22		\$14.99
	kW	1002	1072	1032	1141		1049
	MBH	4975	2955	4249	4895		4421
	ΔD	1.45	0.81	1.21	1.26		1.24
	Temperature	60°	55°	55°	56		
June	\$/kwh	\$0.078	\$0.073	\$0.071	\$0.075		\$0.078
	\$/MMBTU	\$7.89	\$7.07	\$5.76	\$6.68		\$7.75
	Spark Gap	\$14.94	\$14.30	\$14.97	\$15.23		\$15.13
	kW	1058	1028	1213	1314		1138
	MBH	3536	3331	3479	5373		3917
	ΔD	0.98	0.95	0.84	1.20		1.01
	Temperature	69°	68°	66°	65		
Yearly Average	\$/kwh	\$0.080	\$0.075	\$0.074	\$0.074	\$0.069	\$0.077
	\$/MMBTU	\$8.04	\$7.62	\$7.22	\$6.97	\$4.51	\$7.85
	Spark Gap	\$15.39	\$14.47	\$14.57	\$14.83	\$15.69	\$14.60
	kW	1049	1030	1059	1142	1565	1084
	MBH	6303	5878	5034	6423	8418	6010
	ΔD	1.76	1.67	1.39	1.65	1.58	1.63
	Temperature	50	47	54	51	0	

Appendix D: Initial DOE CHP Screening

Note: used 10-year average utility data for screening

DOE TAP CHP Qualification Screen				
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas				
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment g</i>				
Facility Information				
Facility Name	NEOMED Campus			
Location (City, State)	Rootstown, Ohio			
Application	Laboratory/Higher Ed.			
Loads				
Annual Hours of Operation	8,760	Annual operating hours with loads conducive to CHP		
Average Power Demand, kW	1,084	Average power demand during operating hours		
Annual Electricity Consumption, kWh	9,495,840			
Average Thermal Demand, MMBtu/hr	6.01			
Annual Thermal Demand, MMBtu	52,648			
Energy Costs				
	Base Case	CHP Case		
Boiler/Thermal Fuel Costs, \$/MMBtu	\$7.85	\$7.85		
CHP Fuel Costs, \$MM/Btu		\$7.85		
Average Electricity Costs, \$/kWh	\$0.077		Annual electricity costs (demand :	
Percent Average per kWh Electric Cost Avoided		0%	Option 1 - Percent of average elec	
Standby Rate, \$/kW		\$0.05	Option 2 - Monthly \$/kW standby	
Existing System				
Displaced Thermal Efficiency, %	90.0%	Displaced onsite thermal (boiler, heater, etc) efficiency		
CHP System				
Net CHP Power, kW		1,084	CHP System Specs	C
CHP Electric Efficiency, % (HHV)		36.8%	CHP system specs	C
CHP Thermal Output, Btu/kWh		3,854	CHP system specs	C
CHP Thermal Output, MMBtu/hr		4.2	CHP system specs	C
CHP Power to Heat Ratio		0.89	Calculated based on CHP power o	
CHP Availability, %		98%	90 to 98%	
Incremental O&M Costs, \$/kWh		\$0.019	CHP system specs	C
Thermal Utilization, %		90%	Amount of available thermal capt	
Total Installed Costs, \$/kW		\$2,335	CHP system specs	C

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment grade analysis.</i>		
Facility Information		
Facility Name	NEOMED Campus	
Location (City, State)	Rootstown, Ohio	
Application	Laboratory/Higher Ed.	
Annual Energy Consumption	Base Case	CHP Case
Purchased Electricity, kWh	9,495,840	189,917
Generated Electricity, kWh	0	9,305,923
On-site Boiler/Heater Thermal, MMBtu	52,648	20,372
CHP Thermal, MMBtu	0	32,276
Boiler/Heater Fuel, MMBtu	58,497	22,635
CHP Fuel, MMBtu	0	86,210
Total Fuel, MMBtu	58,497	108,845
Annual Operating Costs		
Purchased Electricity, \$	\$731,180	\$14,624
Standby Charges (Option 2), \$	\$0	\$650
On-site Boiler/Heater Fuel, \$	\$459,204	\$177,685
CHP Fuel, \$	\$0	\$676,749
Incremental O&M, \$	\$0	\$176,813
Total Operating Costs, \$	\$1,190,384	\$1,046,521
Simple Payback		
Annual Operating Savings		\$143,863
Total Installed Costs		\$2,531,140
Incentives		\$200,000
Simple Payback, Years		16.2
Operating Costs to Generate		
Fuel Costs, \$/kWh		\$0.073
Thermal Credit, \$/kWh		(\$0.030)
Incremental O&M, \$/kWh		\$0.019
Total Operating Costs to Generate, \$/kWh		\$0.061

Appendix E: CHP Configurations Screening

Option A: 1 GE Jenbacher J420 with process steam load

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an</i>		
Facility Information		
Facility Name	NEOMED Campus	
Location (City, State)	Rootstown, Ohio	
Application	Laboratory/Higher Ed.	
Loads		
Annual Hours of Operation	8,760	Annual operating hours with
Average Power Demand, kW	1,565	Average power demand during
Annual Electricity Consumption, kWh	13,709,400	
Average Thermal Demand, MMBtu/hr	4.82	
Annual Thermal Demand, MMBtu	42,179	
Energy Costs		
	Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51	\$4.51
CHP Fuel Costs, \$MM/Btu		\$4.51
Average Electricity Costs, \$/kWh	\$0.069	
Percent Average per kWh Electric Cost Avoided		0%
Standby Rate, \$/kW		\$0.05
Existing System		
Displaced Thermal Efficiency, %	85.0%	Displaced onsite thermal (kWh)
CHP System		
Net CHP Power, kW		1,426
CHP Electric Efficiency, % (HHV)		40.8%
CHP Thermal Output, Btu/kWh		3,852
CHP Thermal Output, MMBtu/hr		5.5
CHP Power to Heat Ratio		0.89
CHP Availability, %		98%
Incremental O&M Costs, \$/kWh		\$0.019
Thermal Utilization, %		90%
Total Installed Costs, \$/kW		\$2,335

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an</i>		
Facility Information		
Facility Name	NEOMED Campus	
Location (City, State)	Rootstown, Ohio	
Application	Laboratory/Higher Ed.	
Annual Energy Consumption	Base Case	CHP Case
Purchased Electricity, kWh	13,709,400	1,467,475
Generated Electricity, kWh	0	12,241,925
On-site Boiler/Heater Thermal, MMBtu	42,179	0
CHP Thermal, MMBtu	0	42,441
Boiler/Heater Fuel, MMBtu	49,623	0
CHP Fuel, MMBtu	0	102,326
Total Fuel, MMBtu	49,623	102,326
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	\$101,256
Standby Charges (Option 2), \$	\$0	\$856
On-site Boiler/Heater Fuel, \$	\$223,799	\$0
CHP Fuel, \$	\$0	\$461,490
Incremental O&M, \$	\$0	\$232,597
Total Operating Costs, \$	\$1,169,748	\$796,198
Simple Payback		
Annual Operating Savings		\$373,550
Total Installed Costs		\$3,329,710
Incentives		\$200,000
Simple Payback, Years		8.4
Operating Costs to Generate		
Fuel Costs, \$/kWh		\$0.038
Thermal Credit, \$/kWh		(\$0.018)
Incremental O&M, \$/kWh		\$0.019
Total Operating Costs to Generate, \$/kWh		\$0.038

Option B: 2 GE Jenbacher J316 with process steam load

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		Annual operating hours with
Average Power Demand, kW	1,565		Average power demand during
Annual Electricity Consumption, kWh	13,709,400		
Average Thermal Demand, MMBtu/hr	4.82		
Annual Thermal Demand, MMBtu	42,179		
Energy Costs		Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	85.0%		Displaced onsite thermal (l
CHP System			
Net CHP Power, kW			1,696
CHP Electric Efficiency, % (HHV)			38.3%
CHP Thermal Output, Btu/kWh			4,382
CHP Thermal Output, MMBtu/hr			7.4
CHP Power to Heat Ratio			0.78
CHP Availability, %			98%
Incremental O&M Costs, \$/kWh			\$0.019
Thermal Utilization, %			90%
Total Installed Costs, \$/kW			\$2,335

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an</i>		
Annual Energy Consumption	Base Case	CHP Case
Purchased Electricity, kWh	13,709,400	0
Generated Electricity, kWh	0	13,709,400
On-site Boiler/Heater Thermal, MMBtu	42,179	0
CHP Thermal, MMBtu	0	54,068
Boiler/Heater Fuel, MMBtu	49,623	0
CHP Fuel, MMBtu	0	122,228
Total Fuel, MMBtu	49,623	122,228
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	\$0
Standby Charges (Option 2), \$	\$0	\$1,018
On-site Boiler/Heater Fuel, \$	\$223,799	\$0
CHP Fuel, \$	\$0	\$551,246
Incremental O&M, \$	\$0	\$260,479
Total Operating Costs, \$	\$1,169,748	\$812,742
Simple Payback		
Annual Operating Savings		\$357,005
Total Installed Costs		\$3,960,160
Incentives		\$200,000
Simple Payback, Years		10.5
Operating Costs to Generate		
Fuel Costs, \$/kWh		\$0.040
Thermal Credit, \$/kWh		(\$0.016)
Incremental O&M, \$/kWh		\$0.019
Total Operating Costs to Generate, \$/kWh		\$0.043

Option C: 3 GE Jenbacher J312 with process steam load

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		Annual operating hours with
Average Power Demand, kW	1,565		Average power demand during
Annual Electricity Consumption, kWh	13,709,400		
Average Thermal Demand, MMBtu/hr	4.82		
Annual Thermal Demand, MMBtu	42,179		
Energy Costs			
	Base Case		CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	85.0%		Displaced onsite thermal (l
CHP System			
Net CHP Power, kW			1,899
CHP Electric Efficiency, % (HHV)			38.1%
CHP Thermal Output, Btu/kWh			4,387
CHP Thermal Output, MMBtu/hr			8.3
CHP Power to Heat Ratio			0.78
CHP Availability, %			98%
Incremental O&M Costs, \$/kWh			\$0.021
Thermal Utilization, %			90%
Total Installed Costs, \$/kW			\$2,737

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an</i>		
Annual Energy Consumption	Base Case	CHP Case
Purchased Electricity, kWh	13,709,400	-2,593,135
Generated Electricity, kWh	0	16,302,535
On-site Boiler/Heater Thermal, MMBtu	42,179	0
CHP Thermal, MMBtu	0	64,368
Boiler/Heater Fuel, MMBtu	49,623	0
CHP Fuel, MMBtu	0	145,957
Total Fuel, MMBtu	49,623	145,957
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	-\$178,926
Standby Charges (Option 2), \$	\$0	\$1,139
On-site Boiler/Heater Fuel, \$	\$223,799	\$0
CHP Fuel, \$	\$0	\$658,267
Incremental O&M, \$	\$0	\$342,353
Total Operating Costs, \$	\$1,169,748	\$822,833
Simple Payback		
Annual Operating Savings		\$346,915
Total Installed Costs		\$5,197,563
Incentives		\$200,000
Simple Payback, Years		14.4
Operating Costs to Generate		
Fuel Costs, \$/kWh		\$0.040
Thermal Credit, \$/kWh		(\$0.014)
Incremental O&M, \$/kWh		\$0.021
Total Operating Costs to Generate, \$/kWh		\$0.048

Option B: 1 GE Jenbacher J420 with trigeneration, absorption cooling sized to thermal output

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		
Average Power Demand, kW	1,565	Average power demand	
Annual Hours of Cooling Demand	2,520	input	
Annual Hours of Heating Demand	6,240	determined by annual	
Annual Electricity Consumption, kWh	13,709,400		
Average Heating Demand, MMBtu/hr	8.42	CHP system sized to heat	
Annual Heating Demand, MMBtu	52,541		
Average Cooling Demand, Tons	394	2014 cooling	
Average Power Demand without Cooling, kW	1,329	CHP system sized not to	
Average Thermal Requirements for Cooling, MMBtu/hr	6.75	Thermal requirements for	
Average Thermal Requirements for Cooling, MMBtu/hr	#REF!	Thermal requirements for	
Annual Cooling Demand, Tons	992,880		
Energy Costs		Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	0.069		
Cooling Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	90.0%		
Existing Chiller Power Requirements, kWh/Ton	0.60		

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
CHP System		CHP Cooling Single Effect	
Net CHP Power, kW			1,426
CHP Electric Efficiency, % (HHV)			40.8%
CHP Thermal Output, Btu/kWh (Available Heating)			3,852
CHP Thermal Output, MMBtu/hr (Available Heating)			5.49
CHP Thermal Output, Btu/kWh (Available Cooling)			3,274
CHP Thermal Output, MMBtu/hr (Available Cooling)			4.67
CHP Power to Heat Ratio			0.89
CHP Availability, %			98%
Incremental O&M Costs for CHP, \$/kWh			\$0.019
Incremental O&M Costs for chiller, \$/Ton-Year			\$30.00
CHP Installed Costs, \$/kW (without chillers)			\$2,335
Thermal Utilization, %			90%
CHP Cooling			
Absorption Chiller COP			0.7
Absorption Chiller Capacity, Tons			245
Absorption Installed Costs, \$/Ton			\$1,720

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>		
Annual Energy Consumption	Base Case	CHP Cooling Single Effect
Purchased Electricity, kWh	13,709,400	1,104,259
Generated Electricity, kWh	0	12,241,925
Annual Cooling Demand, Tons	992,880	992,880
Electric Cooling, Tons	992,880	387,519
Cooling Electricity, kWh	595,728	232,511
CHP Cooling, Tons	0	605,361
On-site Boiler/Heater Thermal Demand, MMBtu	52,541	22,309
Boiler/Heater Fuel, MMBtu	58,379	24,788
CHP Heating, MMBtu	0	30,232
CHP Fuel, MMBtu	0	102,326
Total Fuel, MMBtu	58,379	127,114
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	\$76,194
Standby Charges (Option 2), \$	\$0	\$856
On-site Boiler/Heater Fuel, \$	\$263,288	\$111,793
CHP Fuel, \$	\$0	\$461,490
Incremental O&M, \$	\$0	\$239,950
Total Operating Costs, \$	\$1,209,236	\$890,283
Simple Payback		
Annual Operating Savings, \$		\$318,953
Chiller Installed Costs, \$/kW		\$296
Total CHP System Costs, \$/kW (including chiller)		\$2,631
Total Installed Costs		\$3,751,325
Incentives		\$200,000
Simple Payback, Years		11.1
Operating Costs to Generate, \$/kWh		
Fuel Costs, \$/kWh		\$0.038
Cooling Credit, \$/kWh		\$0.000
Heating Credit, \$/kWh		(\$0.012)
Incremental O&M, \$/kWh		\$0.020
Total Operating Costs to Generate, \$/kWh		\$0.045

Option E: 2 GE Jenbacher J316 with trigeneration, absorption cooling sized to thermal output

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		
Average Power Demand, kW	1,565	Average power demand	
Annual Hours of Cooling Demand	2,520	input	
Annual Hours of Heating Demand	6,240	determined by annual	
Annual Electricity Consumption, kWh	13,709,400		
Average Heating Demand, MMBtu/hr	8.42	CHP system sized to heat	
Annual Heating Demand, MMBtu	52,541		
Average Cooling Demand, Tons	394		
Average Power Demand without Cooling, kW	1,329	CHP system sized not to	
Average Thermal Requirements for Cooling, MMBtu/hr	6.75	Thermal requirements for	
Average Thermal Requirements for Cooling, MMBtu/hr	#REF!	Thermal requirements for	
Annual Cooling Demand, Tons	992,880		
Energy Costs		Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	0.069		
Cooling Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	90.0%		
Existing Chiller Power Requirements, kWh/Ton	0.60		

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
CHP System		CHP Cooling Single Effect	
Net CHP Power, kW			1,696
CHP Electric Efficiency, % (HHV)			38.3%
CHP Thermal Output, Btu/kWh (Available Heating)			4,382
CHP Thermal Output, MMBtu/hr (Available Heating)			7.43
CHP Thermal Output, Btu/kWh (Available Cooling)			3,725
CHP Thermal Output, MMBtu/hr (Available Cooling)			6.32
CHP Power to Heat Ratio			0.78
CHP Availability, %			98%
Incremental O&M Costs for CHP, \$/kWh			\$0.019
Incremental O&M Costs for chiller, \$/Ton-Year			\$30.00
CHP Installed Costs, \$/kW (without chillers)			\$2,335
Thermal Utilization, %			90%
CHP Cooling			
Absorption Chiller COP			0.7
Absorption Chiller Capacity, Tons			332
Absorption Installed Costs, \$/Ton			\$1,350

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>		
Annual Energy Consumption	Base Case	CHP Cooling Single Effect
Purchased Electricity, kWh	13,709,400	-1,341,851
Generated Electricity, kWh	0	14,559,821
Annual Cooling Demand, Tons	992,880	992,880
Electric Cooling, Tons	992,880	173,830
Cooling Electricity, kWh	595,728	104,298
CHP Cooling, Tons	0	819,050
On-site Boiler/Heater Thermal Demand, MMBtu	52,541	11,637
Boiler/Heater Fuel, MMBtu	58,379	12,931
CHP Heating, MMBtu	0	40,903
CHP Fuel, MMBtu	0	129,810
Total Fuel, MMBtu	58,379	142,740
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	-\$92,588
Standby Charges (Option 2), \$	\$0	\$1,018
On-site Boiler/Heater Fuel, \$	\$263,288	\$58,317
CHP Fuel, \$	\$0	\$585,441
Incremental O&M, \$	\$0	\$286,586
Total Operating Costs, \$	\$1,209,236	\$838,774
Simple Payback		
Annual Operating Savings, \$		\$370,463
Chiller Installed Costs, \$/kW		\$264
Total CHP System Costs, \$/kW (including chiller)		\$2,599
Total Installed Costs		\$4,407,892
Incentives		\$200,000
Simple Payback, Years		11.4
Operating Costs to Generate, \$/kWh		
Fuel Costs, \$/kWh		\$0.040
Cooling Credit, \$/kWh		\$0.000
Heating Credit, \$/kWh		(\$0.014)
Incremental O&M, \$/kWh		\$0.020
Total Operating Costs to Generate, \$/kWh		\$0.046

Option F: 3 GE Jenbacher J312 with trigeneration, absorption cooling sized to thermal output

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		
Average Power Demand, kW	1,565	Average power demand	
Annual Hours of Cooling Demand	2,520	input	
Annual Hours of Heating Demand	6,240	determined by annual	
Annual Electricity Consumption, kWh	13,709,400		
Average Heating Demand, MMBtu/hr	8.42	CHP system sized to heat	
Annual Heating Demand, MMBtu	52,541		
Average Cooling Demand, Tons	394		
Average Power Demand without Cooling, kW	1,329	CHP system sized not to	
Average Thermal Requirements for Cooling, MMBtu/hr	6.75	Thermal requirements for	
Average Thermal Requirements for Cooling, MMBtu/hr	#REF!	Thermal requirements for	
Annual Cooling Demand, Tons	992,880		
Energy Costs		Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	0.069		
Cooling Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	90.0%		
Existing Chiller Power Requirements, kWh/Ton	0.60		

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
CHP System		CHP Cooling Single Effect	
Net CHP Power, kW			1,899
CHP Electric Efficiency, % (HHV)			38.1%
CHP Thermal Output, Btu/kWh (Available Heating)			4,387
CHP Thermal Output, MMBtu/hr (Available Heating)			8.33
CHP Thermal Output, Btu/kWh (Available Cooling)			3,729
CHP Thermal Output, MMBtu/hr (Available Cooling)			7.08
CHP Power to Heat Ratio			0.78
CHP Availability, %			98%
Incremental O&M Costs for CHP, \$/kWh			\$0.021
Incremental O&M Costs for chiller, \$/Ton-Year			\$30.00
CHP Installed Costs, \$/kW (without chillers)			\$2,737
Thermal Utilization, %			90%
CHP Cooling			
Absorption Chiller COP			0.7
Absorption Chiller Capacity, Tons			372
Absorption Installed Costs, \$/Ton			\$1,350

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>		
Annual Energy Consumption	Base Case	CHP Cooling Single Effect
Purchased Electricity, kWh	13,709,400	-3,144,010
Generated Electricity, kWh	0	16,302,535
Annual Cooling Demand, Tons	992,880	992,880
Electric Cooling, Tons	992,880	74,755
Cooling Electricity, kWh	595,728	44,853
CHP Cooling, Tons	0	918,125
On-site Boiler/Heater Thermal Demand, MMBtu	52,541	6,690
Boiler/Heater Fuel, MMBtu	58,379	7,433
CHP Heating, MMBtu	0	45,851
CHP Fuel, MMBtu	0	145,957
Total Fuel, MMBtu	58,379	153,390
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	-\$216,937
Standby Charges (Option 2), \$	\$0	\$1,139
On-site Boiler/Heater Fuel, \$	\$263,288	\$33,523
CHP Fuel, \$	\$0	\$658,267
Incremental O&M, \$	\$0	\$353,506
Total Operating Costs, \$	\$1,209,236	\$829,498
Simple Payback		
Annual Operating Savings, \$		\$379,738
Chiller Installed Costs, \$/kW		\$264
Total CHP System Costs, \$/kW (including chiller)		\$3,001
Total Installed Costs		\$5,699,454
Incentives		\$200,000
Simple Payback, Years		14.5
Operating Costs to Generate, \$/kWh		
Fuel Costs, \$/kWh		\$0.040
Cooling Credit, \$/kWh		\$0.000
Heating Credit, \$/kWh		(\$0.014)
Incremental O&M, \$/kWh		\$0.022
Total Operating Costs to Generate, \$/kWh		\$0.048

Option G: 1 GE Jenbacher J420 with trigeneration, full load absorption cooling with boiler makeup

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		
Average Power Demand, kW	1,565	Average power demand	
Annual Hours of Cooling Demand	2,520	input	
Annual Hours of Heating Demand	6,240	determined by annual	
Annual Electricity Consumption, kWh	13,709,400		
Average Heating Demand, MMBtu/hr	8.42	CHP system sized to heat	
Annual Heating Demand, MMBtu	52,541		
Average Cooling Demand, Tons	394	2014 cooling	
Average Power Demand without Cooling, kW	1,329	CHP system sized not to	
Average Thermal Requirements for Cooling, MMBtu/hr	6.75	Thermal requirements for	
Average Thermal Requirements for Cooling, MMBtu/hr	#REF!	Thermal requirements for	
Annual Cooling Demand, Tons	992,880		
Energy Costs		Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	0.069		
Cooling Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	90.0%		
Existing Chiller Power Requirements, kWh/Ton	0.60		

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
CHP System		CHP Cooling Single Effect	
Net CHP Power, kW			1,426
CHP Electric Efficiency, % (HHV)			40.8%
CHP Thermal Output, Btu/kWh (Available Heating)			3,852
CHP Thermal Output, MMBtu/hr (Available Heating)			5.49
CHP Thermal Output, Btu/kWh (Available Cooling)			3,274
CHP Thermal Output, MMBtu/hr (Available Cooling)			4.67
CHP Power to Heat Ratio			0.89
CHP Availability, %			98%
Incremental O&M Costs for CHP, \$/kWh			\$0.019
Incremental O&M Costs for chiller, \$/Ton-Year			\$30.00
CHP Installed Costs, \$/kW (without chillers)			\$2,335
Thermal Utilization, %			90%
CHP Cooling			
Absorption Chiller COP			0.7
Absorption Chiller Capacity, Tons			245
Absorption Installed Costs, \$/Ton			\$1,720
tons made up by boiler			154
MMBTU/hr			1.85

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>		
Annual Energy Consumption	Base Case	CHP Cooling Single Effect
Purchased Electricity, kWh	13,709,400	871,747
Generated Electricity, kWh	0	12,241,925
Annual Cooling Demand, Tons	992,880	992,880
Electric Cooling, Tons	992,880	0
Cooling Electricity, kWh	595,728	0
CHP Cooling, Tons	0	992,880
On-site Boiler/Heater Thermal Demand, MMBtu	52,541	26,959
Boiler/Heater Fuel, MMBtu	58,379	29,955
CHP Heating, MMBtu	0	30,232
CHP Fuel, MMBtu	0	102,326
Total Fuel, MMBtu	58,379	132,281
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	\$60,151
Standby Charges (Option 2), \$	\$0	\$856
On-site Boiler/Heater Fuel, \$	\$263,288	\$135,096
CHP Fuel, \$	\$0	\$461,490
Incremental O&M, \$	\$0	\$239,950
Total Operating Costs, \$	\$1,209,236	\$897,543
Simple Payback		
Annual Operating Savings, \$		\$311,694
Chiller Installed Costs, \$/kW		\$296
Total CHP System Costs, \$/kW (including chiller)		\$2,631
Total Installed Costs		\$3,751,325
Incentives		\$200,000
Simple Payback, Years		11.4
Operating Costs to Generate, \$/kWh		
Fuel Costs, \$/kWh		\$0.038
Cooling Credit, \$/kWh		\$0.000
Heating Credit, \$/kWh		(\$0.010)
Incremental O&M, \$/kWh		\$0.020
Total Operating Costs to Generate, \$/kWh		\$0.047

Option H: 2 GE Jenbacher J316 with trigeneration, full load absorption cooling with boiler makeup

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment decision.</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		
Average Power Demand, kW	1,565	Average power demand	
Annual Hours of Cooling Demand	2,520	input	
Annual Hours of Heating Demand	6,240	determined by annual	
Annual Electricity Consumption, kWh	13,709,400		
Average Heating Demand, MMBtu/hr	8.42	CHP system sized to heat	
Annual Heating Demand, MMBtu	52,541		
Average Cooling Demand, Tons	394		
Average Power Demand without Cooling, kW	1,329	CHP system sized not to	
Average Thermal Requirements for Cooling, MMBtu/hr	6.75	Thermal requirements for	
Average Thermal Requirements for Cooling, MMBtu/hr	#REF!	Thermal requirements for	
Annual Cooling Demand, Tons	992,880		
Energy Costs		Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	0.069		
Cooling Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	90.0%		
Existing Chiller Power Requirements, kWh/Ton	0.60		

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
CHP System		CHP Cooling Single Effect	
Net CHP Power, kW			1,696
CHP Electric Efficiency, % (HHV)			38.3%
CHP Thermal Output, Btu/kWh (Available Heating)			4,382
CHP Thermal Output, MMBtu/hr (Available Heating)			7.43
CHP Thermal Output, Btu/kWh (Available Cooling)			3,725
CHP Thermal Output, MMBtu/hr (Available Cooling)			6.32
CHP Power to Heat Ratio			0.78
CHP Availability, %			98%
Incremental O&M Costs for CHP, \$/kWh			\$0.019
Incremental O&M Costs for chiller, \$/Ton-Year			\$30.00
CHP Installed Costs, \$/kW (without chillers)			\$2,335
Thermal Utilization, %			90%
CHP Cooling			
Absorption Chiller COP			0.7
Absorption Chiller Capacity, Tons			332
Absorption Installed Costs, \$/Ton			\$1,350
tons made up by boiler			69
MMBTU/hr			0.83

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>		
Annual Energy Consumption	Base Case	CHP Cooling Single Effect
Purchased Electricity, kWh	13,709,400	-1,446,149
Generated Electricity, kWh	0	14,559,821
Annual Cooling Demand, Tons	992,880	992,880
Electric Cooling, Tons	992,880	0
Cooling Electricity, kWh	595,728	0
CHP Cooling, Tons	0	992,880
On-site Boiler/Heater Thermal Demand, MMBtu	52,541	13,723
Boiler/Heater Fuel, MMBtu	58,379	15,248
CHP Heating, MMBtu	0	40,903
CHP Fuel, MMBtu	0	129,810
Total Fuel, MMBtu	58,379	145,058
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	-\$99,784
Standby Charges (Option 2), \$	\$0	\$1,018
On-site Boiler/Heater Fuel, \$	\$263,288	\$68,770
CHP Fuel, \$	\$0	\$585,441
Incremental O&M, \$	\$0	\$286,586
Total Operating Costs, \$	\$1,209,236	\$842,030
Simple Payback		
Annual Operating Savings, \$		\$367,206
Chiller Installed Costs, \$/kW		\$264
Total CHP System Costs, \$/kW (including chiller)		\$2,599
Total Installed Costs		\$4,407,892
Incentives		\$200,000
Simple Payback, Years		11.5
Operating Costs to Generate, \$/kWh		
Fuel Costs, \$/kWh		\$0.040
Cooling Credit, \$/kWh		\$0.000
Heating Credit, \$/kWh		(\$0.013)
Incremental O&M, \$/kWh		\$0.020
Total Operating Costs to Generate, \$/kWh		\$0.047

Option I: 3 GE Jenbacher J312 with trigeneration, full load absorption cooling with boiler makeup

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
Loads			
Annual Hours of Operation	8,760		
Average Power Demand, kW	1,565	Average power demand	
Annual Hours of Cooling Demand	2,520	input	
Annual Hours of Heating Demand	6,240	determined by annual	
Annual Electricity Consumption, kWh	13,709,400		
Average Heating Demand, MMBtu/hr	8.42	CHP system sized to heat	
Annual Heating Demand, MMBtu	52,541		
Average Cooling Demand, Tons	394		
Average Power Demand without Cooling, kW	1,329	CHP system sized not to	
Average Thermal Requirements for Cooling, MMBtu/hr	6.75	Thermal requirements for	
Average Thermal Requirements for Cooling, MMBtu/hr	#REF!	Thermal requirements for	
Annual Cooling Demand, Tons	992,880		
Energy Costs		Base Case	CHP Case
Boiler/Thermal Fuel Costs, \$/MMBtu	\$4.51		\$4.51
CHP Fuel Costs, \$MM/Btu			\$4.51
Average Electricity Costs, \$/kWh	0.069		
Cooling Electricity Costs, \$/kWh	\$0.069		
Percent Average per kWh Electric Cost Avoided			0%
Standby Rate, \$/kW			\$0.05
Existing System			
Displaced Thermal Efficiency, %	90.0%		
Existing Chiller Power Requirements, kWh/Ton	0.60		

DOE TAP CHP Qualification Screen			
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating			
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>			
Facility Information			
Facility Name	NEOMED Campus		
Location (City, State)	Rootstown, Ohio		
Application	Laboratory/Higher Ed.		
CHP System		CHP Cooling Single Effect	
Net CHP Power, kW			1,899
CHP Electric Efficiency, % (HHV)			38.1%
CHP Thermal Output, Btu/kWh (Available Heating)			4,387
CHP Thermal Output, MMBtu/hr (Available Heating)			8.33
CHP Thermal Output, Btu/kWh (Available Cooling)			3,729
CHP Thermal Output, MMBtu/hr (Available Cooling)			7.08
CHP Power to Heat Ratio			0.78
CHP Availability, %			98%
Incremental O&M Costs for CHP, \$/kWh			\$0.021
Incremental O&M Costs for chiller, \$/Ton-Year			\$30.00
CHP Installed Costs, \$/kW (without chillers)			\$2,737
Thermal Utilization, %			90%
CHP Cooling			
Absorption Chiller COP			0.7
Absorption Chiller Capacity, Tons			372
Absorption Installed Costs, \$/Ton			\$1,350
tons made up by boiler			30
MMBTU/hr			0.36

DOE TAP CHP Qualification Screen		
Gas Fueled CHP - Recip Engine, Microturbine, Fuel Cell or Gas Turbine Systems / natural gas, LFG, biogas with Heating		
<i>Note: The results of this screening analysis use average values and assumptions and should not be utilized as an investment</i>		
Annual Energy Consumption	Base Case	CHP Cooling Single Effect
Purchased Electricity, kWh	13,709,400	-3,188,863
Generated Electricity, kWh	0	16,302,535
Annual Cooling Demand, Tons	992,880	992,880
Electric Cooling, Tons	992,880	0
Cooling Electricity, kWh	595,728	0
CHP Cooling, Tons	0	992,880
On-site Boiler/Heater Thermal Demand, MMBtu	52,541	7,587
Boiler/Heater Fuel, MMBtu	58,379	8,430
CHP Heating, MMBtu	0	45,851
CHP Fuel, MMBtu	0	145,957
Total Fuel, MMBtu	58,379	154,387
Annual Operating Costs		
Purchased Electricity, \$	\$945,949	-\$220,032
Standby Charges (Option 2), \$	\$0	\$1,139
On-site Boiler/Heater Fuel, \$	\$263,288	\$38,018
CHP Fuel, \$	\$0	\$658,267
Incremental O&M, \$	\$0	\$353,506
Total Operating Costs, \$	\$1,209,236	\$830,899
Simple Payback		
Annual Operating Savings, \$		\$378,338
Chiller Installed Costs, \$/kW		\$264
Total CHP System Costs, \$/kW (including chiller)		\$3,001
Total Installed Costs		\$5,699,454
Incentives		\$200,000
Simple Payback, Years		14.5
Operating Costs to Generate, \$/kWh		
Fuel Costs, \$/kWh		\$0.040
Cooling Credit, \$/kWh		\$0.000
Heating Credit, \$/kWh		(\$0.014)
Incremental O&M, \$/kWh		\$0.022
Total Operating Costs to Generate, \$/kWh		\$0.048



Appendix F: Sensitivity Study


Option A		Electric Price	Payback Period
		Current .069\$/kWH	8.4
		\$0.074	7.3
		\$0.077	6.6
		\$0.081	6.1
		\$0.084	5.6
		\$0.088	5.2
		\$0.091	4.9
		\$0.095	4.6
		\$0.098	4.3
		Gas Price	Payback Period
		Current \$4.51/MMBtu	8.4
		\$4.28	8.1
		\$4.05	7.9
		\$3.83	7.6
		\$3.60	7.4
		\$3.38	7.2
		\$3.15	7.0
		\$2.93	6.9
		\$2.70	6.7
electric increase/gas decrease	Electric Price	Gas Price	Payback Period
0	Current .069\$/kWH	Current \$4.51/MMBtu	8.4
5%	\$0.074	\$4.28	7.0
10%	\$0.077	\$4.05	6.3
15%	\$0.081	\$3.83	5.6
20%	\$0.084	\$3.60	5.2
25%	\$0.088	\$3.38	4.7
30%	\$0.091	\$3.15	4.4
35%	\$0.095	\$2.93	4.0
40%	\$0.098	\$2.70	3.8

Option B		Electric Price	Payback Period
		Current .069\$/kWH	10.5
		\$0.074	8.6
		\$0.077	7.8
		\$0.081	7.0
		\$0.084	6.4
		\$0.088	5.9
		\$0.091	5.5
		\$0.095	5.1
		\$0.098	4.8
		Gas Price	Payback Period
		Current \$4.51/MMBtu	10.5
		\$4.28	9.8
		\$4.05	9.3
		\$3.83	9.0
		\$3.60	8.6
		\$3.38	8.2
		\$3.15	7.9
		\$2.93	7.6
		\$2.70	7.4
electric increase/gas decrease	Electric Price	Gas Price	Payback Period
0	Current .069\$/kWH	Current \$4.51/MMBtu	10.5
5%	\$0.074	\$4.28	8.2
10%	\$0.077	\$4.05	7.2
15%	\$0.081	\$3.83	6.3
20%	\$0.084	\$3.60	5.7
25%	\$0.088	\$3.38	5.1
30%	\$0.091	\$3.15	4.7
35%	\$0.095	\$2.93	4.3
40%	\$0.098	\$2.70	4.0

Appendix G: Emissions Calculations

Option A

 Documentation

1. CHP: Type of System

Recip Engine - Lean Burn

2. CHP: Electricity Generating Capacity (per unit)

Normal size range for this technology is 500 to 5,000 kW

1,426 kW

3. CHP: How Many Identical Units (i.e., engines) Does This System Have?

1

4. CHP: How Many Hours per Year Does the CHP System Operate?

7 days per week, 24 hours per day, 8,760 hours

As a number of hours per year

OR As a percentage

5. CHP: Does the System Provide Heating or Cooling or Both?

Heating Only

If Heating and Cooling: How many of the 8,760 hours are in cooling mode?

As a number of hours per year

as a percentage of the 8,760 hours?

If Heating and Cooling: Does the System Provide Simultaneous Heating and Cooling?

No

6. CHP: Fuel

Fuel Type

View Biomass and Coal Fuel Characteristics

7. CHP: If Diesel, Distillate, Coal or Other: What is the Sulfur Content?

If WHP, what is the sulfur content of the stack?

High sulfur oil: 0.15% or 1,500

Low sulfur oil: 0.05% or 500

Ultra low sulfur diesel: 15 ppm

I will enter a value in one of the following blocks or

Enter Sulfur Content of Fuel as a percent

OR ppm ppm

8. CHP: What is the CO₂ Emission Rate for this Fuel? (default completed for fuel in Item 6)

Enter alternative value: lb CO₂/MMBtu

9. CHP: What is the Heat Content of this Fuel? (Enter a value in only ONE of the boxes) Submit

	<input type="text" value="1,028"/>	Btu/cubic foot (HHV)
OR	<input type="text" value="-"/>	Btu/gallon (HHV)
OR	<input type="text" value="-"/>	Btu/lb (HHV)

10. CHP: Boiler Steam To Process (Steam Turbine CHP Only)

Boiler Steam to Process as lb Steam/hr	<input type="text" value="0"/>
Boiler Steam to Process as MMBtu Steam/hr	<input type="text" value="0"/>

Submit

11. CHP: Steam Turbine System Boiler Efficiency (Steam Turbine CHP Only)

Enter Boiler Efficiency as % Submit

12. CHP: Electric Efficiency

Submit

Enter Generating Efficiency as % (HHV)

OR Enter Generating Efficiency as Btu/kWh HHV Btu/kWh (HHV)

OR Enter Generating Efficiency as Btu/kWh LHV Btu/kWh (LHV)

13. CHP: Base Power to Heat Ratio

The Power to Heat Ratio should reflect ONLY the thermal production of the generating unit (i.e., combustion turbine). Thermal Output of the duct burners (if equipped) should not be included.

Submit

Power to Heat Ratio

If WHP: Useful Thermal Output (MMBtu/hr)

14. CHP: NOx Emission Rate

Note: Default emissions are without aftertreatment. Some areas may require add-on controls and you will need to enter an emission rate based on your local requirements. SCR can reduce emissions by up to 90%

Enter a NOx Rate as ppm (15% O ₂)	<input type="text" value="-"/>	ppm
OR Enter a NOx Rate as gm/hp-hr	<input type="text" value="1.100"/>	gm/hp-hr
OR Enter a NOx Rate as lb/MMBtu	<input type="text" value="-"/>	lb NOx/MMBtu
OR Enter a NOx Rate as lb/MWh	<input type="text" value="-"/>	lb NOx/MWh

Submit

15. Duct Burners: Does the System Incorporate Duct Burners? Submit

No

16. Duct Burners: What is the Total Fuel Input Capacity of the Burners for Each CHP Unit? Submit

For reference, the Recip Engine - Lean Burn has a heat input of 11.9 MMBtu/hr

MMBtu/hr

17. Duct Burners: The CHP system operates 8,760 hours per year. How much do the duct burners operate? Submit

As a number of hours per year

As a percentage of the 8,760 hours?

18. Duct Burners: NOx Emission Rate for the Duct Burners

Submit

OR

lb/MMBtu
 ppm NOx at 15% O2

19. Cooling: Does the CHP Provide Cooling? **No** Submit

You indicated No Cooling in Item 5

20. Cooling: Type of Absorption Chiller Used? Submit

Coefficient of Performance (COP)

21. Cooling: What is the Cooling Capacity of the System? Submit

Based on your other entries, the maximum cooling capacity is . tons or . MMBtu/hr of cooling

(Enter a value in only ONE of the boxes)

Cooling Tons
 OR MMBtu per Hour of Cooling

22. Displaced Cooling: What is the Efficiency of the Cooling System that is Being Displaced? Submit

(Enter a value in only ONE of the boxes)

Electricity Demand (kW per ton)
 OR Coefficient of Performance (COP)

23. Displaced Thermal: Type of System: Existing Gas Boiler

24. Displaced Thermal: If not a Natural Gas System: What is the Sulfur Content?

I will enter a or

Enter Sulfur Content as a percent OR ppm ppm

25. Displaced Thermal: What is the CO2 Emission Rate for this Fuel? (default completed for fuel in Item 23)

Enter alternative value: lb CO2/MMBtu

26. Displaced Thermal: What is the Heat Content of this Fuel? (Enter a value in only ONE of the boxes)

OR Btu/cubic foot (HHV)
OR Btu/gallon (HHV)
OR Btu/lb (HHV)

27. Displaced Thermal: Efficiency (usually a boiler)

I will enter an efficiency

Enter Generating Efficiency as %

28. Displaced Thermal Production: NOx Emission Rate

I will enter the NOx rate

NOx Rate lb NOx/MMBtu

29. Displaced Electricity: Generation Profile

[Link to EPA's Fuel and CO2 Emissions Savings Calculation Methodology for CHP](#)

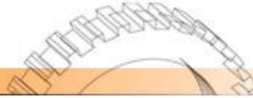
30. Displaced Electricity: Select U.S. Average, eGRID Subregion, NERC region, or State

[Link to eGRID Subregion Map](#)

31. Displaced Electricity: Select Electric Grid Region for Transmission and Distribution (T&D) Losses

[Link to NERC Interconnections Map](#)

CHP Results



The results generated by the CHP Emissions Calculator are intended for educational and outreach purposes only; it is not designed for use in developing emission inventories or preparing air permit applications.

The results of this analysis have not been reviewed or endorsed by the EPA CHP Partnership.

Table 1

Annual Emissions Analysis

	CHP System	Displaced Electricity Production	Displaced Thermal Production	Emissions/Fuel Reduction	Percent Reduction
NO _x (tons/year)	20.30	10.82	2.82	(6.66)	-49%
SO ₂ (tons/year)	0.03	30.93	0.02	30.92	100%
CO ₂ (tons/year)	6,105	14,337	3,293	11,525	65%
CH ₄ (tons/year)	0.12	0.163	0.06	0.110	49%
N ₂ O (tons/year)	0.01	0.231	0.01	0.225	95%
Total GHGs (CO ₂ e tons/year)	6,111	14,412	3,296	11,597	65%
Fuel Consumption (MMBtu/year)	104,445	139,368	56,341	91,264	47%
Equal to the annual GHG emissions from this many passenger vehicles:				2,201	
Equal to the annual GHG emissions from the generation of electricity for this many homes:				1,439	

This CHP project will avoid yearly emissions of greenhouse gases by 11,597 tons of carbon dioxide equivalent.



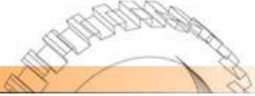
Equal to the annual greenhouse gas emissions from 2,201 passenger vehicles.




Equal to the annual greenhouse gas emissions from the generation of electricity used by 1,439 homes.



Option B



Documentation

1. CHP: Type of System

Recip Engine - Lean Burn

2. CHP: Electricity Generating Capacity (per unit)

Normal size range for this technology is 500 to 5,000 kW

848 kW

3. CHP: How Many Identical Units (i.e., engines) Does This System Have?

2

4. CHP: How Many Hours per Year Does the CHP System Operate?

7 days per week, 24 hours per day, 8,760 hours

As a number of hours per year

OR As a percentage

5. CHP: Does the System Provide Heating or Cooling or Both?

Heating Only

If Heating and Cooling: How many of the 8,760 hours are in cooling mode?

As a number of hours per year

as a percentage of the 8,760 hours?

If Heating and Cooling: Does the System Provide Simultaneous Heating and Cooling?

No

6. CHP: Fuel

Fuel Type: Natural Gas

View Biomass and Coal Fuel Characteristics

7. CHP: If Diesel, Distillate, Coal or Other: What is the Sulfur Content?

If WHP, what is the sulfur content of the stack?

I will enter a value in one of the following blocks

or

High sulfur oil: 0.15% or 1,500

Low sulfur oil: 0.05% or 500

Ultra low sulfur diesel: 15 ppm

Enter Sulfur Content of Fuel as a percent

OR ppm ppm

8. CHP: What is the CO₂ Emission Rate for this Fuel? (default completed for fuel in Item 6)

Enter alternative value: lb CO₂/MMBtu

9. CHP: What is the Heat Content of this Fuel? (Enter a value in only ONE of the boxes) Submit

	1,028	Btu/cubic foot (HHV)
OR	-	Btu/gallon (HHV)
OR	-	Btu/lb (HHV)

10. CHP: Boiler Steam To Process (Steam Turbine CHP Only)

Boiler Steam to Process as lb Steam/hr	0	Submit
Boiler Steam to Process as MMBtu Steam/hr	0	

11. CHP: Steam Turbine System Boiler Efficiency (Steam Turbine CHP Only)

I will enter an efficiency
Use default for this technology

Enter Boiler Efficiency as % Submit

12. CHP: Electric Efficiency

I will enter an efficiency in **one** of the following blocks
Use default for this technology

Enter Generating Efficiency as % (HHV) Submit

OR Enter Generating Efficiency as Btu/kWh HHV Btu/kWh (HHV)

OR Enter Generating Efficiency as Btu/kWh LHV Btu/kWh (LHV)

13. CHP: Base Power to Heat Ratio

The Power to Heat Ratio should reflect ONLY the thermal production of the generating unit (i.e., combustion turbine). Thermal Output of the duct burners (if equipped) should not be included.

I will enter a Power to Heat
Use default for this technology

Power to Heat Ratio Submit

If WHP: Useful Thermal Output (MMBtu/hr)

14. CHP: NOx Emission Rate

I will enter a NOx rate in **one** of the following blocks

Use default emissions for this technology.
Note: Default emissions are without aftertreatment. Some areas may require add-on controls and you will need to enter an emission rate based on your local requirements. SCR can reduce emissions by up to 90%

	-	ppm
OR	1.100	gm/hp-hr
OR	-	lb NOx/MMBtu
OR	-	lb NOx/MWh

Submit

15. Duct Burners: Does the System Incorporate Duct Burners? Submit
 ▼

16. Duct Burners: What is the Total Fuel Input Capacity of the Burners for Each CHP Unit? Submit
 For reference, the Recip Engine - Lean Burn has a heat input of 7.6 MMBtu/hr
 MMBtu/hr

17. Duct Burners: The CHP system operates 8,760 hours per year. How much do the duct burners operate? Submit
 As a number of hours per year
 As a percentage of the 8,760 hours?

18. Duct Burners: NOx Emission Rate for the Duct Burners Submit

lb/MMBtu
 OR ppm NOx at 15% O2

19. Cooling: Does the CHP Provide Cooling? No Submit
 You indicated No Cooling in Item 5

20. Cooling: Type of Absorption Chiller Used? Submit
 ▼
 Coefficient of Performance (COP)

21. Cooling: What is the Cooling Capacity of the System? Submit
 Based on your other entries, the maximum cooling capacity is . tons or . MMBtu/hr of cooling

(Enter a value in only ONE of the boxes) Cooling Tons
 OR MMBtu per Hour of Cooling

22. Displaced Cooling: What is the Efficiency of the Cooling System that is Being Displaced? Submit
 ▼

(Enter a value in only ONE of the boxes)
 Electricity Demand (kW per ton)
 OR Coefficient of Performance (COP)

23. Displaced Thermal: Type of System: Existing Gas Boiler

24. Displaced Thermal: If not a Natural Gas System: What is the Sulfur Content?

I will enter a or

Enter Sulfur Content as a percent ppm ppm

25. Displaced Thermal: What is the CO2 Emission Rate for this Fuel? (default completed for fuel in Item 23)

Enter alternative value: lb CO2/MMBtu

26. Displaced Thermal: What is the Heat Content of this Fuel? (Enter a value in only ONE of the boxes)

Btu/cubic foot (HHV)
 OR Btu/gallon (HHV)
 OR Btu/lb (HHV)

27. Displaced Thermal: Efficiency (usually a boiler)

I will enter an efficiency

Enter Generating Efficiency as %

28. Displaced Thermal Production: NOx Emission Rate

I will enter the NOx rate

NOx Rate lb NOx/MMBtu

29. Displaced Electricity: Generation Profile

[Link to EPA's Fuel and CO2 Emissions Savings Calculation Methodology for CHP](#)

30. Displaced Electricity: Select U.S. Average, eGRID Subregion, NERC region, or State

31. Displaced Electricity: Select Electric Grid Region for Transmission and Distribution (T&D) Losses

CHP Results



The results generated by the CHP Emissions Calculator are intended for educational and outreach purposes only; it is not designed for use in developing emission inventories or preparing air permit applications.

The results of this analysis have not been reviewed or endorsed by the EPA CHP Partnership.

Table 1

Annual Emissions Analysis

	CHP System	Displaced Electricity Production	Displaced Thermal Production	Emissions/Fuel Reduction	Percent Reduction
NO _x (tons/year)	24.14	12.87	3.82	(7.45)	-45%
SO ₂ (tons/year)	0.04	36.79	0.02	36.77	100%
CO ₂ (tons/year)	7,744	17,051	4,469	13,776	64%
CH ₄ (tons/year)	0.15	0.194	0.08	0.132	48%
N ₂ O (tons/year)	0.01	0.274	0.01	0.268	95%
Total GHGs (CO ₂ e tons/year)	7,752	17,141	4,473	13,862	64%
Fuel Consumption (MMBtu/year)	132,498	165,756	76,458	109,717	45%
Equal to the annual GHG emissions from this many passenger vehicles:				2,630	
Equal to the annual GHG emissions from the generation of electricity for this many homes:				1,720	

This CHP project will avoid yearly emissions of greenhouse gases by 13,862 tons of carbon dioxide equivalent.

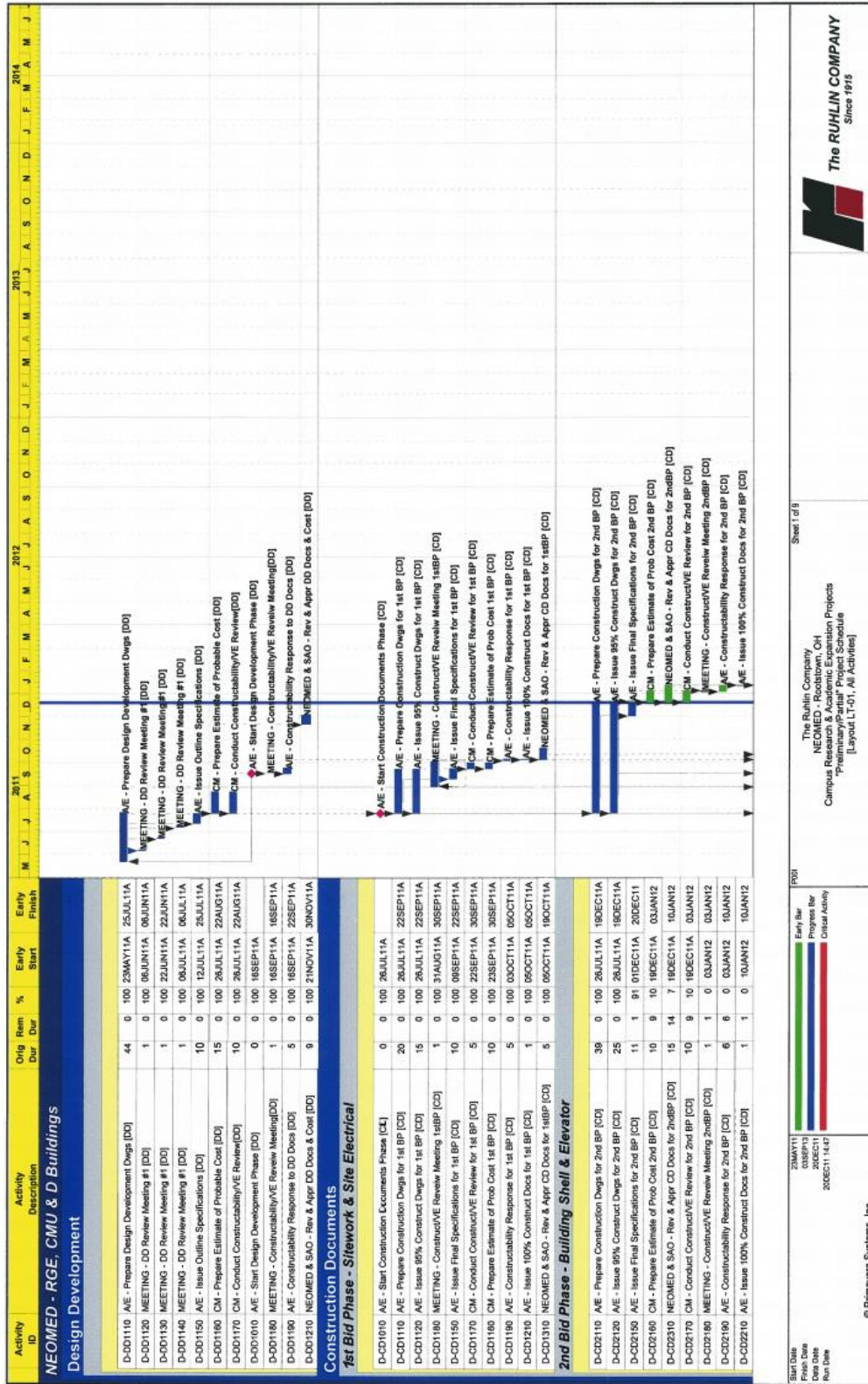
Equal to the annual greenhouse gas emissions from 2,630 passenger vehicles.

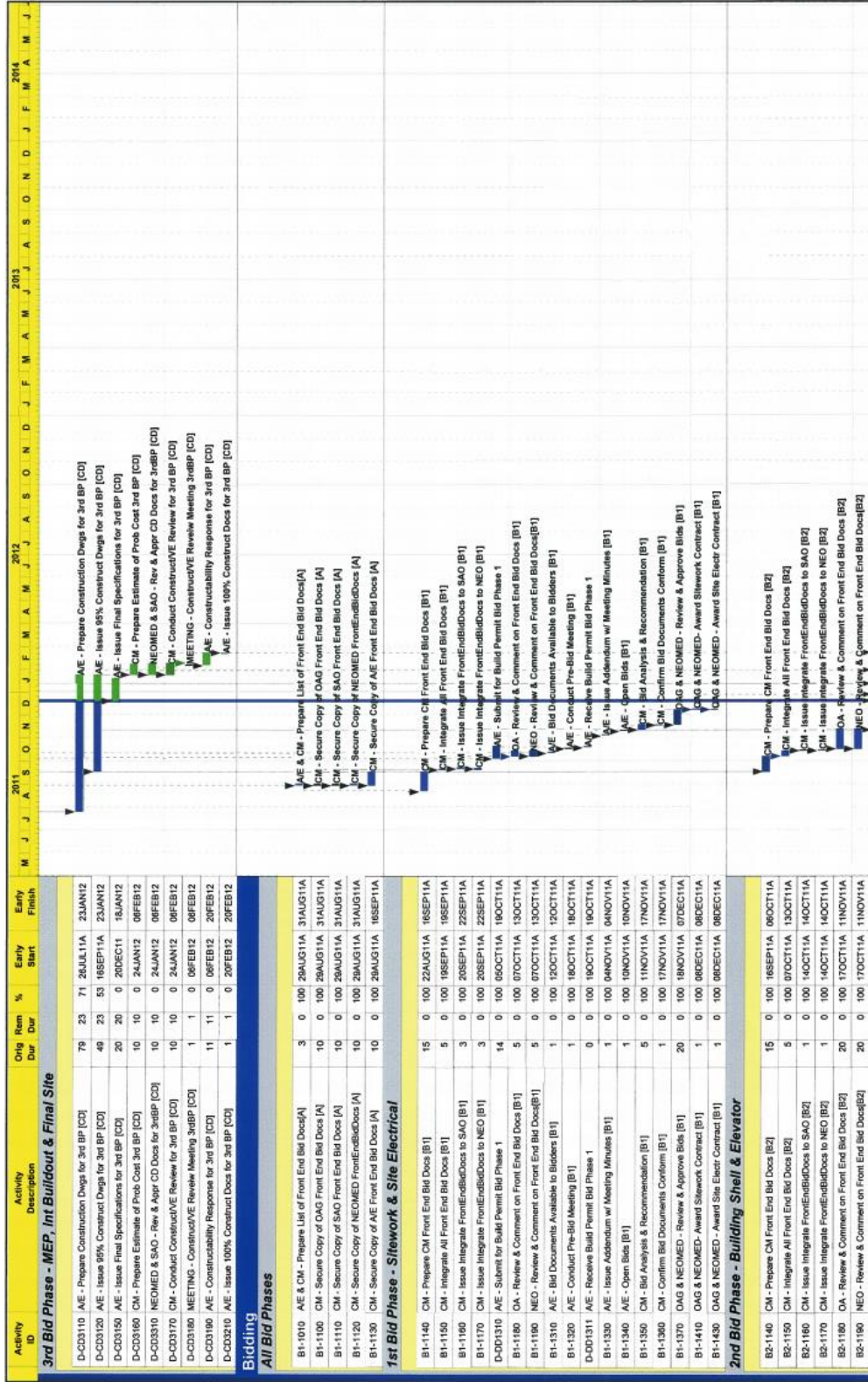


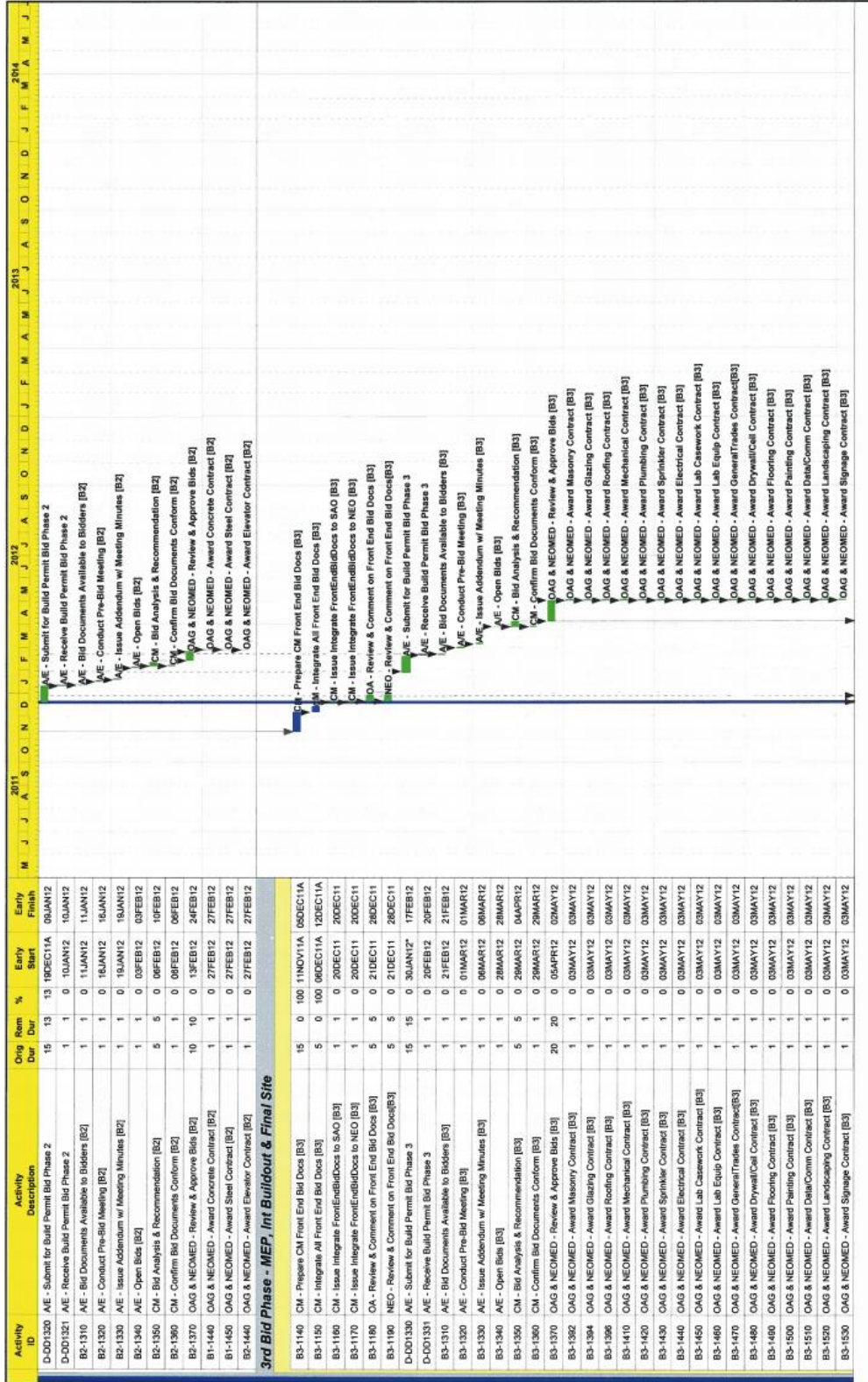
Equal to the annual greenhouse gas emissions from the generation of electricity used by 1,720 homes.

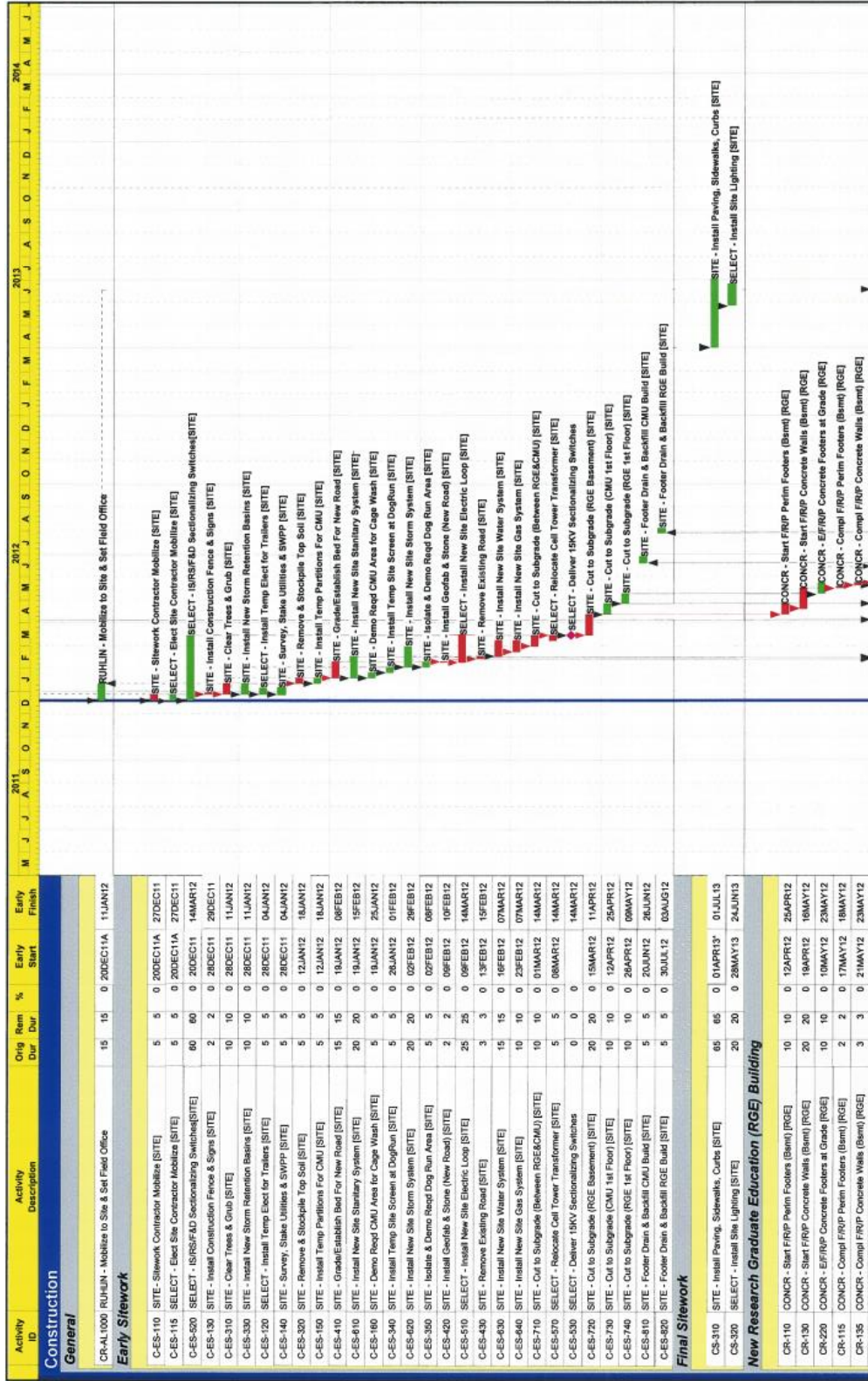


Appendix H: Project Schedules
Original Schedule

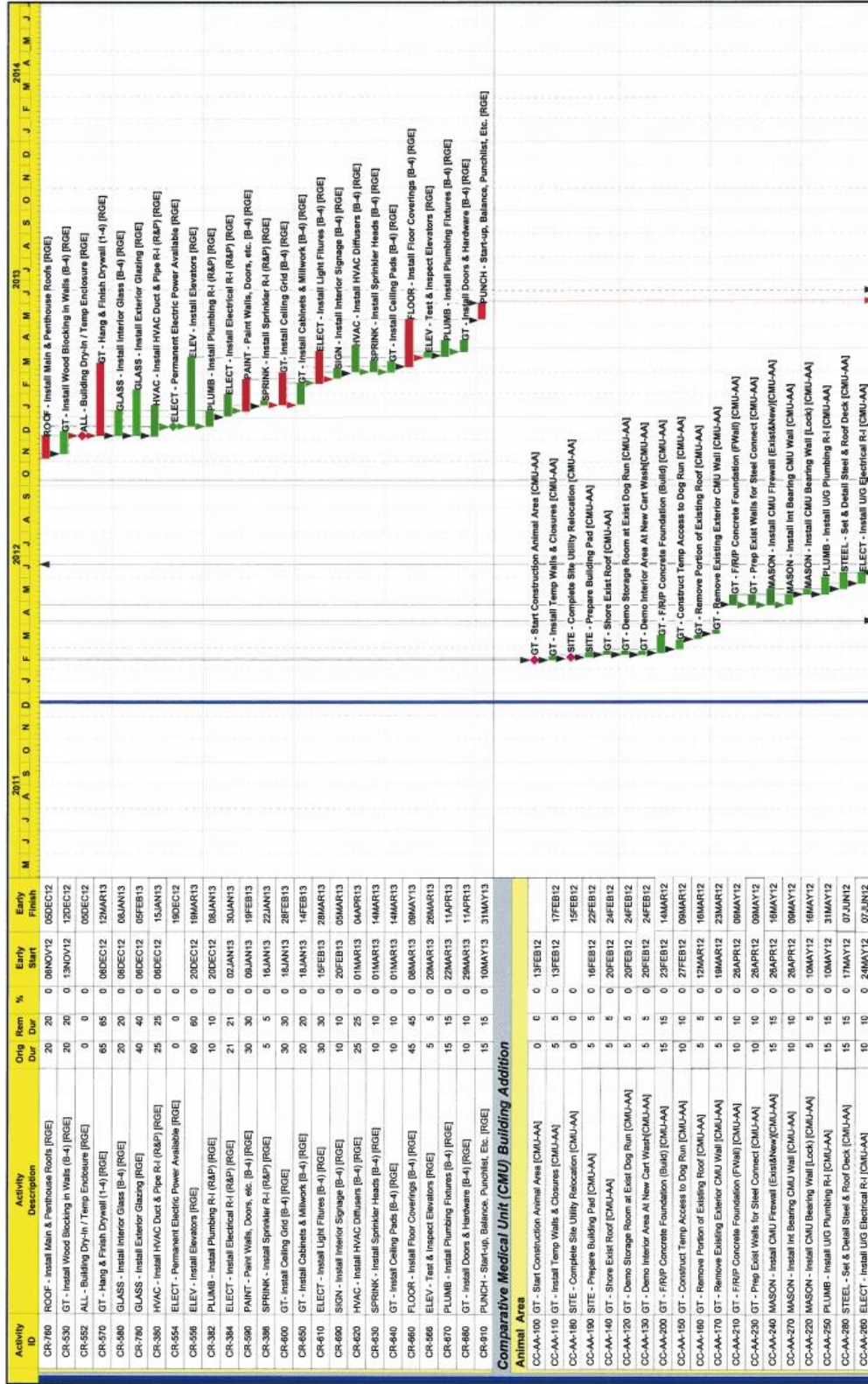


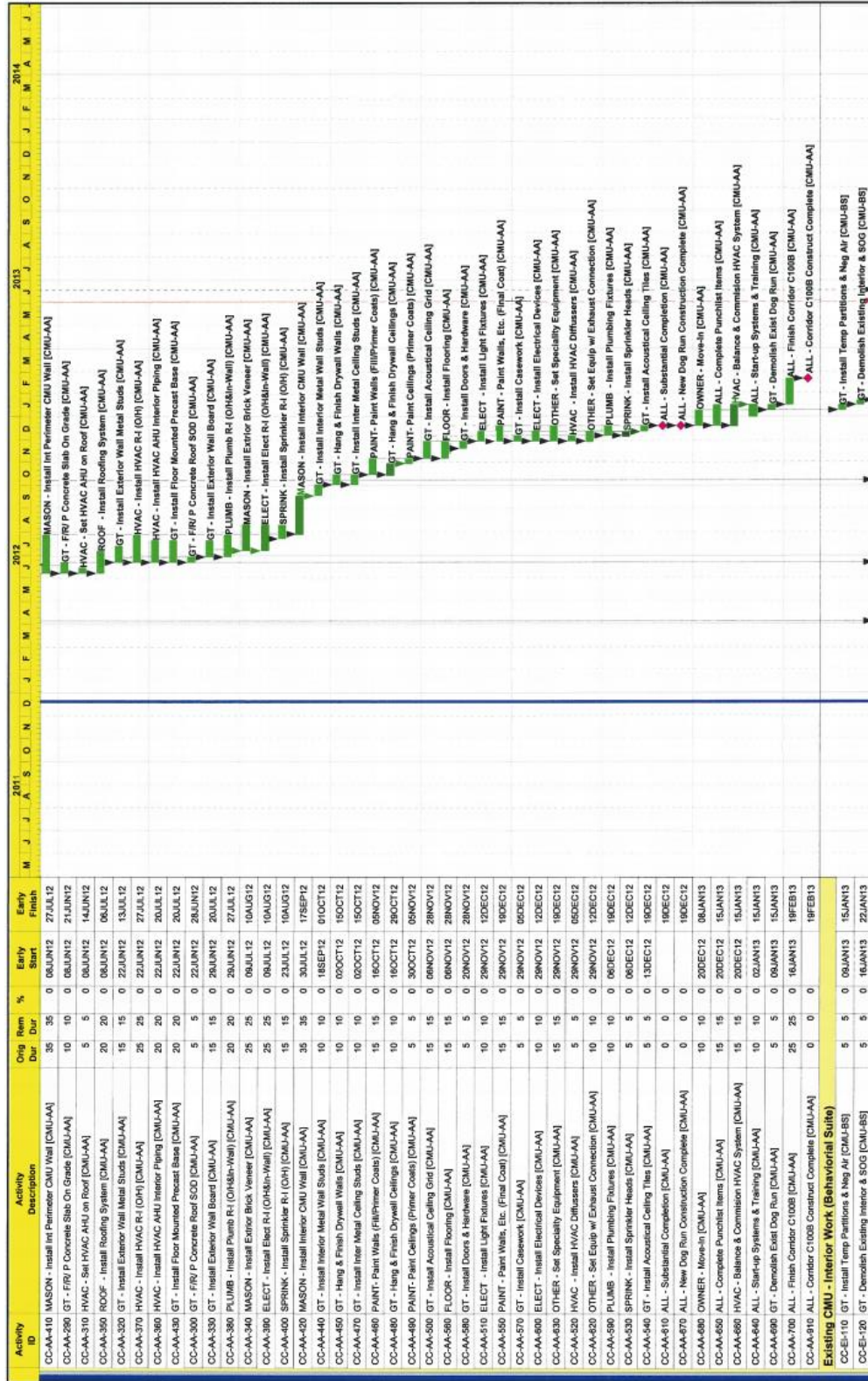






Activity ID	Activity Description	Orig Dur	Risk %	Early Start	Early Finish
CR-120	CONCR - FRIP Int Concrete Footers (Bent) [RGE]	5	5	0 21MAY12	25MAY12
CR-140	CONCR - Cure Time Concrete Wall (Basement) [RGE]	5	5	0 24MAY12	31MAY12
CR-145	CONCR - Cure Time Concrete Int Foot (Bent) [RGE]	5	5	0 29MAY12	04JUN12
CR-150	STEEL - Erect/Detail Steel Deck (Basement)[RGE]	10	10	0 01JUN12	14JUN12
CR-160	PLUMB - Install U/G Plumbing (Basement) [RGE]	10	10	0 15JUN12	28JUN12
CR-180	STEEL - Erect/Detail Steel & Deck (2&3F) [RGE]	10	10	0 15JUN12	28JUN12
CR-190	ELECT - Install U/G Electrical (Basement) [RGE]	5	5	0 29JUN12	06JUL12
CR-250	STEEL - Erect/Detail Steel & Deck (4F&5F) [RGE]	10	10	0 29JUN12	13JUL12
CR-260	MEP - Install MEP Box-outs in FloorDeck (2)[RGE]	5	5	0 29JUN12	06JUL12
CR-200	CONCR - FRIP Concrete SOG (Basement) [RGE]	10	10	0 06JUL12	20JUL12
CR-301	MEP - Install MEP Box-outs in FloorDeck (3)[RGE]	5	5	0 06JUL12	13JUL12
CR-303	MEP - Install MEP Box-outs in FloorDeck (4)[RGE]	5	5	0 16JUL12	20JUL12
CR-270	PLUMB - Install U/G Plumbing (1) [RGE]	10	10	0 16JUL12	27JUL12
CR-254	STEEL - Erect/Detail S/S ScreenWall(Floor) [RGE]	5	5	0 18JUL12	20JUL12
CR-210	CONCR - FRIP Concrete SOG (Over Basement) [RGE]	5	5	0 23JUL12	27JUL12
CR-305	MEP - Install MEP Box-outs in FloorDeck (R)[RGE]	5	5	0 23JUL12	27JUL12
CR-300	CONCR - FRIP Concrete SOG (2nd Floor) [RGE]	5	5	0 30JUL12	03AUG12
CR-510	MASON - Install Interior CMU Walls (B-4) [RGE]	60	60	0 30JUL12	22OCT12
CR-272	ELECT - Install U/G Electrical (1) [RGE]	5	5	0 30JUL12	03AUG12
CR-360	HVAC - Install HVAC Duct & Pipe R-4 (B) [RGE]	40	40	0 30JUL12	24SEP12
CR-212	WATERP - Install Waterproof & Drain Tile [RGE]	5	5	0 30JUL12	03AUG12
CR-302	CONCR - FRIP Concrete SOG (3rd Floor) [RGE]	5	5	0 06AUG12	10AUG12
CR-274	CONCR - FRIP Concrete SOG (1) [RGE]	5	5	0 06AUG12	10AUG12
CR-214	CONCR - Backfill Basement Walls [RGE]	5	5	0 06AUG12	10AUG12
CR-304	CONCR - FRIP Concrete SOG (4th Floor) [RGE]	5	5	0 13AUG12	17AUG12
CR-370	HVAC - Install HVAC Duct & Pipe R-4 (1-4) [RGE]	80	80	0 13AUG12	05DEC12
CR-362	PLUMB - Install Plumbing R-4 (B) [RGE]	40	40	0 13AUG12	09OCT12
CR-330	STEEL - Install Steel Stairs [RGE]	20	20	0 13AUG12	10SEP12
CR-710	GT - Install Exterior Metal Studs [RGE]	50	50	0 20AUG12	29OCT12
CR-306	CONCR - FRIP Concrete SOG (Roof) [RGE]	5	5	0 20AUG12	24AUG12
CR-372	PLUMB - Install Plumbing R-4 (1-4) [RGE]	75	75	0 27AUG12	12DEC12
CR-364	ELECT - Install Electrical R-4 (B) [RGE]	75	75	0 27AUG12	12DEC12
CR-308	HVAC - FRIP Concrete AHU Maint Pads (Roof)[RGE]	5	5	0 04SEP12	10SEP12
CR-720	GT - Install Ext Insulat/Moisture Barrier [RGE]	50	50	0 04SEP12	12NOV12
CR-310	HVAC - Lit, Set & Install AHUs (Roof) [RGE]	10	10	0 11SEP12	24SEP12
CR-374	ELECT - Install Electrical R-4 (1-4) [RGE]	50	50	0 11SEP12	19NOV12
CR-335	CONCR - Pour Concrete Stair Pans [RGE]	10	10	0 11SEP12	24SEP12
CR-320	GT - Install Metal Stud Walls (B-4) [RGE]	50	50	0 25SEP12	05DEC12
CR-336	HVAC - Lit & Set Exhaust Stacks (Roof) [RGE]	10	10	0 25SEP12	09OCT12
CR-4750	MASON - Install Ext Masonry Walls & Brick [RGE]	80	80	0 25SEP12	22JAN13
CR-740	MASON - Install Ext Brick Linels [RGE]	60	60	0 25SEP12	19DEC12
CR-376	SPRINK - Install Sprinkler R-4 (1-4) [RGE]	30	30	0 25SEP12	09NOV12
CR-366	SPRINK - Install Sprinkler R-4 (B) [RGE]	10	10	0 25SEP12	09OCT12
CR-790	GT - Install Ext Plywood & Roof Wood Block [RGE]	20	20	0 09OCT12	09NOV12
CR-540	PLUMB - Install In-Wall Plumbing R-4 (B-4) [RGE]	50	50	0 09OCT12	19DEC12
CR-500	ELECT - Install In-Wall Electric R-4 (1-4) [RGE]	50	50	0 09OCT12	19DEC12





Activity ID	Activity Description	Orig Dur	Rem %	Early Start	Early Finish
CC-EI-130	PLUMB - Install UG Plumbing R-1 [CMU-BS]	4	0	23JAN13	28JAN13
CC-EI-140	ELECT - Install UG Electrical R-1 [CMU-BS]	3	0	25JAN13	29JAN13
CC-EI-150	GT - FRP Concrete Slab on Grade [CMU-BS]	5	0	30JAN13	09FEB13
CC-EI-160	HVAC - Install HVAC R-1 (OH) [CMU-BS]	3	0	06FEB13	09FEB13
CC-EI-170	PLUMB - Install Plumbing R-1 (OH) [CMU-BS]	3	0	08FEB13	12FEB13
CC-EI-180	ELECT - Install Electrical R-1 (OH) [CMU-BS]	3	0	11FEB13	13FEB13
CC-EI-190	SPRINK - Install Sprinkler R-1 (OH) [CMU-BS]	1	0	12FEB13	12FEB13
CC-EI-200	GT - Install Interior Metal Wall Studs [CMU-BS]	5	0	14FEB13	20FEB13
CC-EI-210	PLUMB - Install Plumbing R-1 (In-Wall) [CMU-BS]	5	0	21FEB13	27FEB13
CC-EI-220	ELECT - Install Electric R-1 (In-Wall) [CMU-BS]	5	0	21FEB13	27FEB13
CC-EI-230	GT - Hang & Finish Drywall Walls [CMU-BS]	5	0	28FEB13	06MAR13
CC-EI-240	PAINT - Paint Walls (Primer Coat) [CMU-BS]	5	0	07MAR13	13MAR13
CC-EI-250	GT - Install Acoustical Ceiling Grid [CMU-BS]	5	0	14MAR13	20MAR13
CC-EI-260	ELECT - Install Light Fixtures [CMU-AA]	2	0	21MAR13	22MAR13
CC-EI-270	HVAC - Install HVAC Diffusers [CMU-AA]	2	0	25MAR13	26MAR13
CC-EI-280	SPRINK - Install Sprinkler Heads [CMU-AA]	1	0	27MAR13	27MAR13
CC-EI-290	GT - Install Acoustical Ceiling Tiles [CMU-BS]	5	0	28MAR13	03APR13
CC-EI-300	PAINT - Paint Walls, Etc. (Final Coat) [CMU-BS]	5	0	04APR13	10APR13
CC-EI-310	FLOOR - Install Flooring [CMU-BS]	5	0	11APR13	17APR13
CC-EI-320	GT - Install Casework [CMU-BS]	5	0	18APR13	24APR13
CC-EI-330	GT - Install Doors & Hardware [CMU-BS]	5	0	18APR13	24APR13
CC-EI-340	PLUMB - Install Plumbing Fixtures [CMU-BS]	2	0	25APR13	26APR13
CC-EI-350	ELECT - Install Electrical Devices [CMU-BS]	2	0	25APR13	26APR13
CC-EI-360	ALL - Substantial Completion [CMU-BS]	0	0	0	26APR13
CC-EI-370	ALL - Start-up Systems & Training [CMU-BS]	5	0	29APR13	03MAY13
CC-EI-380	ALL - Complete Punchlist Items [CMU-BS]	5	0	05MAY13	10MAY13
CC-EI-390	HVAC - Balance & Commission HVAC System [CMU-BS]	5	0	13MAY13	17MAY13
CC-EI-400	ALL - Construction Complete [CMU-BS]	0	0	0	17MAY13
CC-EI-410	OWNER - Move-In [CMU-BS]	5	0	20MAY13	24MAY13
Existing CMU - Inter Work (Electrical Upgrades)					
CC-EI-710	ELECT - Install Electric Feeders & Panels [CMU-EU]	15	15	30JAN13	18FEB13
CC-EI-720	ELECT - Rerouted Existing Electric Panels [CMU-EU]	15	15	20FEB13	12MAR13
New CMU Mechanical Building					
CC-NE-900	ALL - Construct New CMU Mechanical Building	40	40	22JUN12	17AUG12
Existing CMU MEP & Boiler House Upgrades					
CU-BH-900	PLUMB - Install Existing CMU Boiler House Upgrades	40	40	22JUN12	17AUG12
Central Mechanical Room					
CU-MR-300	ALL - Construct Central Mechanical Room	40	40	22JUN12	17AUG12
Existing Building D Renovation					
CD-010	SAO & NEOMED - Authorization of Funds Building D	0	0	0	04APR12
CD-020	NEOMED - Move Staff to New RGE Building	10	10	05JUN13	14JUN13
CD-100	ALL - Renovate Existing Building D [D]	55	55	17JUN13	03SEP13
Alternate Bridge (RGE Building to CMU Building)					
CB-100	ALL - Construct Alternate Bridge [BRIDGE]	100	100	06OCT12	05MAR13

RS07-8 FOR RUHLIN / OWNER / OFCC REVIEW		NEOMED		Revised Baseline for July 15, 2013 Owner Move-In		RS07-8 Printed 27-May-13 09:08											
Activity ID	Task Description	Orig Dur	Rem Dur	Start	Finish	Total Float	May	June	July	August	September	October	November	December			
Alternate Bridge (RGE Building to CMU Building)																	
CB-190	CONC - Pour Edge Foundation (All Bridge)	5	5	02-Jun-13	02-Sep-13	-5											
CB-191	STEEL - Install Structural Steel (All Bridge)	5	5	02-Jun-13	07-Sep-13	-5											
CB-200	CONC - Install Concrete Slab on Deck (All Bridge)	5	5	16-Jun-13	14-Jun-13	-5											
CB-100	GLASS - Install Window Framing & Glazing	17	17	24-Jun-13	21-Jun-13	-5											
CB-110	GLASS - Exterior Metal Studs (All Bridge)	5	5	16-Jul-13	24-Jul-13	-5											
CB-120	GLASS - Install Exterior Metal Studs (All Bridge)	12	12	16-Jul-13	02-Aug-13	-2											
CB-130	WLSGLG - Install 1st Floor Slabs (All Bridge)	3	3	25-Jul-13	26-Jul-13	-3											
CB-202	ROOF - Install Rubber Roofing (All Bridge)	5	5	25-Jul-13	31-Jul-13	-3											
CB-108	ELEC - Electrical Rough-in, ALL (All Bridge)	5	5	26-Jul-13	05-Aug-13	-3											
CB-108	MECH - HVAC Rough-in, ALL (All Bridge)	5	5	26-Jul-13	05-Aug-13	-3											
CB-109	WLSGLG - Hang / Finish Drywall (All Bridge)	5	5	07-Aug-13	07-Aug-13	-5											
CB-140	WLSGLG - Hanging / Finish Drywall (All Bridge)	8	8	08-Aug-13	19-Aug-13	-5											
CB-141	WLSGLG - Hanging (All Bridge)	2	2	20-Aug-13	21-Aug-13	-5											
CB-115	ELEC - Install Light Fixtures (All Bridge)	4	4	22-Aug-13	04-Sep-13	-5											
CB-115	ELEC - Install Light Fixtures (All Bridge)	5	5	22-Aug-13	04-Sep-13	-5											
CB-128	FLOOR - Install Rubber Flooring Mem	3	3	05-Sep-13	05-Sep-13	-5											
CB-128	WLSGLG - Install Ceiling Par (All Bridge)	3	3	05-Sep-13	05-Sep-13	-5											
Site Electrical Loop - East																	
LOO-100	"1 DELAY" ELEC - Electric Loop Relocation, East Campus	99	9	14-Jan-13 A	31-May-13	64											
LOO-100	"1 DELAY" ELEC - Electric Loop Relocation, East Campus	99	9	14-Jan-13 A	31-May-13	64											
LOO-240	ELEC - Excavate / Install Conduit 18x11 to road	2	2	20-May-13	20-May-13	-16											
LOO-280	ELEC - Pull Wire New 20x7 to 18x7, Call	2	2	20-May-13	21-May-13	-24											
LOO-300	ELEC - Pull Wire 18x4 to 18x4	2	2	20-May-13	24-May-13	-24											
LOO-300	ELEC - Pull Wire 18x4 to 18x2	1	1	20-May-13	22-May-13	-24											
LOO-310	ELEC - Pull Wire 18x2 to 18x11, SMA	1	1	20-May-13	24-May-13	-24											
LOO-320	ELEC - New Wire at 20x7, SMA	1	1	24-May-13	24-May-13	-24											
LOO-330	ELEC - Excavate / Install Conduit New, Mainroom	5	5	24-May-13	31-May-13	-24											
LOO-300	ELEC - Terminate 20x7, SMA, 20x10x2E	1	1	28-May-13	24-May-13	-21											
Cooling Tower Replacement																	
CTWR-100	BP22 - Cooling Tower Replacement Work	99	24	14-Jan-13 A	21-Jan-13	-15											
CTWR-100	BP22 - Start-Up New Tower #2 [CTWR]	99	24	14-Jan-13 A	21-Jan-13	-15											
CTWR-200	BP22 - Start-Up New Tower #1 [CTWR]	5	4	28-May-13 A	23-May-13	0											
CTWR-200	BP22 - Punch List / Close-Out [CTWR]	5	5	24-May-13	31-May-13	0											

Actual Work Remaining Work Milestone

Task filters: NEO Not Complete, NEO Omit